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REQUIREMENTS FOR EXPLOSION-PROOF ELECTRICAL EQUIPMENT IN AIR FORCE HANGARS

Lester A. Eggleston, et al

Southwest Research Institute

Prepared for:

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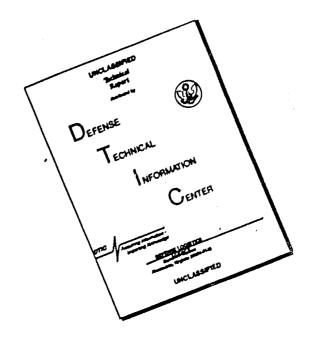
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Lester A. Eggleston Michael D. Pish

Southwest Research Institute
San Antonio, Texas

TECHNICAL REPORT NO. AFWL-TR-72-135

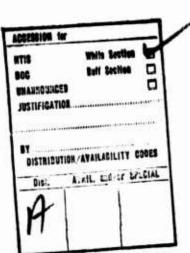
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13 ABSTRACT			

(Distribution Limitation Statement A)

The objective of this research effort was to determine if current requirements for explosion-proof equipment in USAF hangars are more stringent than necessary, and thereby result in unnecessary expense in meeting such requirements. Experiments and tests conducted, both in actual USAF hangars and in the laboratory, indicated that the vapor explosibility hazard from leaks and fuel spills is lower than generally believed. The results of this study indicate that hazardous zone definitions in existing codes could be relaxed without compromising safety. Vertical profile measurements of fuel spills and fuel leak vapors showed that under normal conditions of ventilation, the atmosphere in the 2-in. level was well below the lower explosive limit (LEL). Even with the extreme condition of volatile fuel spills in quiescent, confined spaces, the LEL level did not rise above 7 inches. It was concluded, therefore, that all portions of hangar spaces more than 12 in. above the floor could be considered as nonhazardous with respect to vapors from aircraft fuel spills and leaks relating to explosion-proof equipment requirements. In view of this. it further concluded that the 18-inch upper boundary in existing National Electric Code (NEC) and the Occupational Safety and Health Act (OSHA) requirements are more than adequate to ensure safety.

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Lester A. Eggleston Michael D. Pish Southwest Research Institute San Antonio, Texas

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FOREWORD

This report was prepared by the Southwest Research Institute, San Antonio, Texas, under Contract F29601-71-C-0116. The research was performed under Program Element 63723F, Project 683M. Task 2.

Inclusive dates of research were June 1971 through July 1972. The report was submitted 15 June 1973 by the Air Force Weapons Laboratory Project Officer, Mr. Frederick H. Peterson (DEZ).

This technical report has been reviewed and is approved.

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ABBREVIATIONS

AC alternating current

ASTM American Society for Testing Materials

atm atmosphere(s)

avgas aviation gasoline

Div Division

LEL lower explosive limit

1/min liters per minute

MSA Mine Safety Appliances

NA nonapplicable

NEC National Electrical Code

NFPA National Fire Protection Association

0.D. outside diameter

Ref(s) reference(s)

R.H. relative humidity

sec second

UDMH unsymmetrical dimethyl hydrazine

UEL upper explosive limit

V volt

Vol% percent by volume

ALMF-1K-17-122

SECTION I

INTRODUCTION

Many informed persons have been concerned about existing codes pertaining to the explosivity of aircraft fuel vapors in aircraft hangars and resultant requirements for explosion-proof electrical equipment. No data were available with which engineering judgments could be made of criteria now in force. Accordingly, the Civil Engineering Division of the Air Force Weapons Laboratory was directed early in 1971 to carry out an appropriate investigation of the basic problem. On 16 June 1971, the Air Force Weapons Laboratory negotiated a contract with the Southwest Research Institute to accomplish the required research. The Statement of Work for this specifically required the contractor to prepare and submit recommended revisions of AFM 88-15, if such were deemed necessary.

The decided approach to the problem consisted of both laboratory and field Initially, spill and leakage tests would be conducted on a small scale in a simulated hangar environment. These would provide information on the effects of varying fuels, exposed surface areas, temperature, humidity, barometric pressure, and various typical building design features (such as pressurizing to block vapor flow). Laboratory work was carried out in three phases. In Phase 1, sampling was carried out in a single geometric plane for points 18 inches apart between the vapor source and the wall of the room. Vertical increments were taken at points 4 inches to 16 inches above the floor. In Phase 2. sampling was carried out at the center of the room and at points 2 feet from the walls of each corner at heights of 2, 12, 18, and 48 inches. In addition, three points were monitored at the 96-inch ceiling level. Phase 3 studied vertical profiles of vapor concentration at 2-inch intervals up to 24 inches and at 1/2-inch intervals up to 12 inches. Field work was carried out in USAF hangars at Kelly AFB, Randolph AFB, and Bergstrom AFB. The objective of this work was to secure maximum parking and maximum maintenance occupancy for worstcase conditions with fully fueled aircraft and extended closed door operations. A large-scale JP-4 spill test also was included. Sampling was generally at 2 inches above the floor.

To secure quantitative information on actual vapor concentrations arising from flammable liquid spills or leaks under various conditions, a total of 32 tests was carried out under simulated hangar conditions, together with five tests in operating USAF hangars. A total of 124,122 data points was recorded during 591 hours and 10 minutes of testing. The instrumentation consisted of a Beckman Model 400 Total Hydrocarbon Analyzer and a Honeywell 24-Point Recorder which controlled a bank of three-way solenoid valves in a continually purged and synchronized sampling system. The instrumentation was regularly calibrated against a standard methane-air mixture which had been analyzed using a Perkin-Elmer Gas Chromatrograph. Eased on data compiled by the US Bureau of Mines, the average lower explosive limit (LEL) of JP-4 and 115/145 avgas was taken at 1.25 percent by volume (12,500 ppm). This figure was then used in calculating the fuel vapor equivalent of the methane-air standard calibration gas.

SECTION II

DISCUSSION OF THE PROBLEM

An unwritten principle of industrial safety states that if a hazard is known to exist, adequate measures must be taken to avoid loss of life or property because of it. Sound economic practice requires that any protective measures taken must be suited both to the severity of the exposure and to the likelihood of adverse consequences. Whenever data on severity and probability are not available, it is not unusual to assume the worst situation and devise countermeasures accordingly.

This practice can be justified only on the grounds that any and all expenditures for safety are worthwhile a premise which is difficult to defend. Frequently, the costs of protection can far exceed the benefits to be realized, and unless safety requirements are based on sound information, the expense may quickly reach the point of diminishing returns on the investments involved and defeat its own purpose. Appreciable savings can be realized when the costs of the safety measures provided are equated against the hazard probabilities.

The use, handling, and storage of flammable liquids involves an unavoidable hazard potential. Hangars used for parking and maintenance of partially or fully fueled aircraft can regularly contain areas where concentrations of tuel vapors could conceivably build up to the lower explosive limit (LEL). Some aircraft fuel systems have no allowance for thermal expansion. A fueled aircraft moved into a warm hangar will drip fuel at the tank outlets. In such areas, any source of ignition might produce serious consequences. One obvious protective measure is to minimize the ignition probability by using explosion-proof electrical fixtures in zones where vapor concentrations could present a hazard. These are specified in both the National Fire Protection Association (NFPA) Standards for civil aircraft which include the National Electrical Code (NEC) and AFM 88-15 for military hangars. The question thus arises as to which standard is most appropriate. If one is just adequate, the other would appear to be either deficient or excessive, depending on which is used as the reference. For both, the fuel volatilities involved are essentially the same.

The NFPA began formulating its aviation standards about 1950 when piston aircraft dominated the scene and gasoline was the principal fuel used. Efforts to ascertain the basis used by the NFPA committee in defining the limits of the hazardous areas have been unsuccessful. As far as could be determined, however, no quantitative data on hangar conditions were then available. Harvey Hansberry (Ref. 1), current Vice Chairman of the Aviation Committee, states that he is unaware of any published hangar work. Three reports (Refs. 2, 3, 4) were found which dealt with the vapor envelope at tank vents during outdoor refueling. But since refueling in hangars is presently prohibited by NFPA Standard. No. 407, they were mapplicable except for general information. It can only be assumed that the standards represent subjective judgements on the part of those involved.

High-volatility fuels (gasoline, JP-4, and Jet B) are still in sufficient use to warrant the application of appropriate standards. With low-volatility fuels (Jet A, JP-5, and JP-8), the hazard would be almost nonexistent.

Piston engines require a tailored gasoline fuel, while turbine engine fuel requirements are much less critical. JP-4 and Jet B are kerosene-gasoline blends, while Jet A, JP-5, and JP-8 are straight kerosenes. Since the problem is to determine what constitutes an appropriate standard in terms of the more hazardous fuels, the standard should be based on objective judgements resulting from quantitative measurements.

Both aviation gasoline (avgas) and military turbine fuel (JP-4) have flash points below 0°F. By definition, this is the lowest temperature at which, under controlled conditions, the vapor layer over the fuel reaches the LEL. The flash point is commonly determined by the closed cup method. ASTM D-56. Since normal hangar ambient conditions are invariably well above 0°F, it can be assumed safely that at the immediate liquid surface of any fuel spill or leak and at some finite distance above it, an explosive concentration can exist. Whether or not this would constitute a hazard depends upon many interrelated variables such as

- (1) the partial pressure of the volatile fuel components;
- (') the volume and surface area of the exposed fuel;

- (3) air currents in the vicinity of the spill which may dilute the released fuel vapor; and
- (4) the time required for cleanup of spills or effective dissipation of volatile fractions.

From an engineering standpoint, any fuel spill involves a diffusion/evaporation process, and, if all the factors were known, equations could conceivably be written to characterize the phenomena. In actual practice, spills are not predictable in size and nature. Temperatures, irregular surface areas, rates of fuel release, and ventilation conditions vary so widely that about the only practical approach to hazard assessment is measurement of vapor concentrations in some worst-case situations.

All of the fuel vapors involved with the fuels mentioned are essentially butane-pentane-hexane mixtures that are several times heavier than air. It would be normal to expect the highest concentrations of flammable gases to build up at floor level or below it, with gradually decreasing concentrations at higher levels as the fuel vapors diffuse upwards or are diluted by air currents. This philosophy is the basis of the several electrical standards in use today which set various distances above the floor as zones in which explosion-proof equipment is mandatory. Such standards can be evaluated only from data on the horizontal and vertical distributions of fuel vapor and the concentrations reached at various times as the fuel evaporates and as vapors are dissipated by convection and diffusion.

There are a number of possible sources of tuel vapors in hangars. These are evaporation from the exposed surfaces of containers, accidentally spilled fuels, inadvertent losses during maintenance operations, leaks dripping onto the floor, and the displacement of vapors from aircraft tanks during thermal expansion or refueling. Once generated, the vapors could move by gravity flow or wind pressure differentials anywhere within the area of concern. Therefore, the overall protective scheme should be based on actually measured concentrations of vapors under representative conditions and should consider the costs of providing adequate protection against adverse situations. By simulation of drips and spills in a small-scale facility under controlled conditions and tests in actual operating hangars, it should be possible to secure useful data on the magnitude of the hazard exposure.

Protection may take a number of forms, and all may supplement each other. In aircraft hangars, an obvious approach is to establish operating practices which minimize the release of vapors. NFPA Standard No. 407 on aircraft fueling, which requires this to be done out-of-doors, is a step in this direction. This eliminates large-scale indoor vapor venting. The cited references 2, 3, and 4 deal with vapor venting.

The requirements of the two codes of interest are shown for an assumed hangar situation in Figure 1. Article 500 of the NEC, which governs hazardous areas in general, classifies them in three ways:

- Class I flammable vapors in sufficient quantities to produce an explosible mixture
- Class II combustible dusts
- Class III easily ignitable fibers.

It should be noted that while the mere presence of flammable vapors could categorize aircraft hangars as Class 1, the vapors must be produced in sufficient quantities to present a preciable hazard. That is, the degree of exposure factor must be represented. If the hazard is continuous, intermittent, or periodic under normal operating conditions, it is described as Class 1, Division 1. On the other hand, if the flammables are normally confined and the presence of vapors is the exception rather than the rule, the area is described as Class 1, Division 2, and the electrical requirements are less rigorous.

When explosion-proof equipment is necessary, it must be suited to the specific vapors (or dusts) with respect to the maximum explosion pressures the fixture must be able to withstand and the allowable clearances which control flame stopping effectiveness. This requires a further classification by vapor properties as may be seen from reference to Table 500-2(c) of the NEC, included as Appendix 1 on page 32. Almost all flammable liquids, including petroleum fuels, fall into Class 1, Group D (Div. 1 or 2). A few compounds used in aerospace work, especially UDMH, are in Class 1, Group C. The presence of Group C liquids in hangars, however, is unlikely, and spills of such liquids in hangars are even less likely.

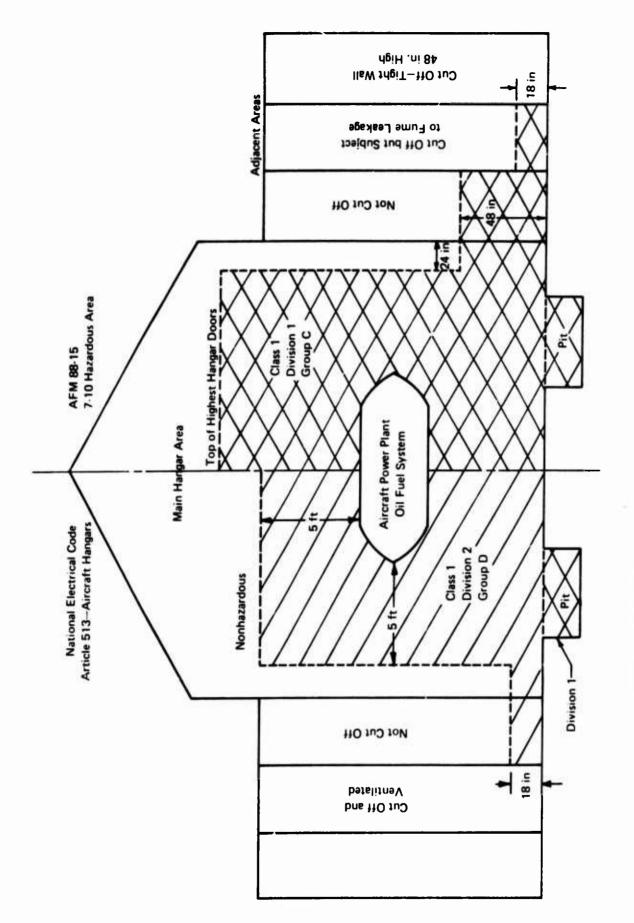


FIGURE 1. COMPARISON OF HAZARDOUS AREA DILI INTIONS BY ARTICLE 513 OF NATIONAL ELECTRICAL CODE AND ALM 88-15

It is very important that any heat-generating equipment selected for use in a hangar not produce a surface temperature high enough to cause auto-ignition of the particular fuel vapor under consideration. The revised National Electric Code states:

(a) Approval for Class and Properties. Equipment shall be approved not only for the class of location but also for the explosion properties of the specific gas, vapor, or dust that will be present. In addition, equipment shall not have exposed any surface that operates at a temperature in excess of the ignition temperature of the specific gas vapor or dust.

The characteristics of various atmospheric mixtures of hazardous gases, vapors, and dusts depend on the specific hazardous material involved.

(b) Marking. Approved equipment shall be marked to show the Class, Group and operating temperature, or temperature range, based on operation in a 40°C ambient for which it is approved.

The temperature range, if provided, shall be indicated in identification numbers, as shown in Table 500-2(b).

Identification numbers marked on equipment nameplates shall be in accordance with Table 500-2(b).

Exception: Equipment of the nonheat-producing type, such as junction buxes, conduit and fittings, are not required to have a marked operating temperature.

For purposes of testing and approval, various atmospheric mixtures (not oxygen enriched) have been grouped on the basis of their hazardous characteristics, and facilities have been made available for testing and approval of equipment for use in the atmospheric groups listed in Table 500-2(c). Since there is no consistent relationship between explosion properties and ignition temperature, the two must be regarded as independent requirements.*

There are appreciable cost differences between the various Group and Division ratings, and between explosion-proof and nonexplosion-proof equipment.

Explosion-proof equipment is more expensive than nonexplosive-proof equipment. For any particular installation wherein operations are well established (in this case, aircraft hangars), it is logical to gather quantitative data on the actual hazard exposure under the most adverse exposure conditions, allow a reasonable margin for any unknowns, and then determine the adequacy of existing safety measures. Accordingly, this research program was designed to provide firm data which could be used by USAF engineers to evaluate the requirements for explosion-proof electrical outlets in USAF aircraft hangars. Pertinent portions of Air Force Manual (AFM) 88-15 and the National Electric Code (NEC) are presented in Appendix I for convenient reference.

^{*1971-72} Revised National Electric Code, paragraphs 500-2(a) and (b).

SECTION III

TEST PROGRAM INSTRUMENTATION

1. INSTRUMENT PACKAGE DESIGN

The magnitude of any flammable vapor hazard can be exposed as a percentage of the LEL. If it is below the LEL, the mixture cannot be ignited. A mixture above the LEL must be considered dangerous. Even if the mixture is above the upper explosive limit (UEL), it may become diluted enough to fall within the explosible range.

There are two basic techniques for measuring vapor concentrations. One uses catalytic oxidation of the sample gas by a hot platinum filament to unbalance an electrical bridge circuit and produce a direct readout calibrated in percent of LEL. A portable instrument is available with a hand operated sample pump for quick checking of areas for hazardous gases. Multipoint devices of this design are available with built-in sampling pumps for permanent installation. If desired, special explosion-proof diffusion heads can make the measurement directly at the immediate sampling point. Without special calibration, the latter instruments cannot measure concentrations above the LEL. Common ranges available are 0 to 10 percent and 0 to 100 percent of LEL. Thus, these oxidation type devices were considered to have too limited a range for this program (except for checking purposes) since the range to be investigated was on the order of 0 to 200,000 ppm.

The most versatile instrument for measuring hydrocarbon vapor concentrations is the hydrogen flame ionization meter. This instrument has been available for many years, and its accuracy and stability are well established. Since it was recognized that the vapor concentrations in the test program could vary from extremely low values to well above the LEL and since quantitative results were needed, the ion = on type meter was selected.

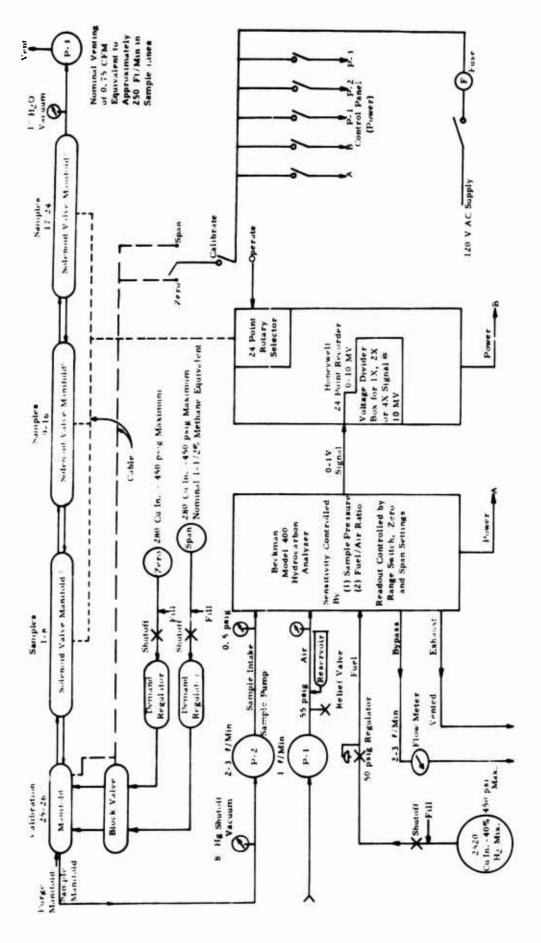
The instrument used had a stated useful range from 1 ppm full-scale to 100,000 ppm full-scale (based upon methane). These values were indicative but not limiting. The lowest range used during the program was 0 to 10 ppm of fuel vapor. The highest was 0 to 20,000 ppm of fuel vapor. Calibration to higher ranges would have been possible, but this was not necessary.

The original plan was to use two instruments. One was to be used to monitor ten fixed points, while the other was to monitor a scanner probe moving horizontally and vertically across selected planes in the simulated hangar space. This, however, would have greatly complicated data reduction and would have been poorly suited to the required full-scale hangar tests. After further study, it was decided to use a single instrument to monitor twenty-four fixed points placed in accordance with the needs of the experiment.

A 24-point Honeywell recording thermometer also was made available to the program. This was modified by the manufacturer to:

- (1) isolate the 24-point thermocouple selector switch from the measuring circuit and convert it to a 120-VAC rotary selector switch to control the sampling solenoids:
- (2) change the chart drive gear trains to print 12 points/in., regardless of time. This prevented overprinting of closely grouped data points:
- (3) provide readily changeable drive motors to enable sampling speeds between 5 and 30 sec/point as desired; and
- (4) calibrate the measuring circuits for 0 to 10 mV DC. To print out the signals from the fuel vapor measurements at each sample point.

An operational schematic of the instrument package is shown as Figure 2. The rotary switch on the Honeywell drive motor controls a bank of twenty-four 3-way solenoid valves. Normally each sample line (about 50 to 100 ft of 1/4-in, O.D. polyethylene tubing) was connected to a purge manifold, which exhausted a total of about 21 g/min from the system, keeping a continually fresh sample at the manifold. As each sample solenoid was activated in turn, the stream was switched to the sample manifold. The sample pump sent 2 to 3 g/min to a Beckman Model 400 Total Hydrocarbon Analyzer where it indicated the vapor content. The signal was then fed to the 24-point recorder through a small voltage divider box which enabled any reading to be multiplied by 2 or 4 for convenience in readout. At the conclusion of the sample period, the recorder printed an identified data point.



Three-way valves. Sample line normally connected to purge manifold (P-3) energizing solenoid transfers stream to sample manifold (P-2),

The instruments, pumps, and sampling system were assembled into a standard 6-ft rack cabinet. The lower portion contained nine pressure tanks rated at 500 psig which could contain enough of the 40-percent hydrogen/60-percent nitrogen fuel gas mix for the Beckman Analyzer to support operation for over a week. It also contained a switch selectable tank of calibration gas and a tank of nitrogen for a zero gas. The instrument package is illustrated in Figure 3.

It was constructed for complete portability and ready movement to any selected test site. Allowing time for warmup of the instrument and running sample lines, a test could be started approximately 4 hr after arrival at the point of intended use.

2. CALIBRATION

Calibration of any instrument, such as the Beckman Model 400 Analyzer to read total volume of a mixture of hydro-carbon vapors, requires the determination of a typical analysis so that a reference gas can be prepared. Since the desired end product of the study was related to the LEL of aviation fuel vapors, advantage was taken of Zabetakis' (Ref. 5) work in this area. He points out that there is some disagreement on the flammability limit of fuel blends, but suggests these values:

<u>Fuel</u>	LEL (Vol %)
Avgas 100/130	1.3
Avgas 115/145	1.2
Jet Fuel JP-4	1.3

The LEL of a fuel vapor blend is related to the LEL of its various components, and the same reference cites these figures:

Compound	LEL (Vol %)
Methane	5.0
Ethane	3.0
Propane	2.1
Butane	1.8
Pentane	1.4
Hexane	1.2
Heptane	1.05
Octane	0.95

Cross plotting vapor LEL's with the number of carbon atoms involved (as shown in Figure 4), it may be seen that a typical aviation fuel spill would have an averaged LEL of approximately 1...5 percent, corresponding to a pentane/hexane mix with a median of 5.75 carbon atoms per molecule. The value r would also contain relatively small amounts of butane and heavy ends. Some slight differences could be expected between the heavy ends from avgas and those from JP-4 by reason of the higher final boiling point of JP-4.

For the same volume percentage, an aviation fuel vapor would read 5.75 times higher on the analyzer than methane vapor. This fact was used in preparing the calibration gas. Methane was selected as the basic component gas since it would remain in the vapor state when stored and mixed at high pressures.

The calibration sample was prepared by charging 1-1/2 atm of methane to an evacuated pressure cylinder which was then pressurized by adding 100 atm of compressed air. This was equilibrated for 4 days with a steam coil and water coil on opposite sides of the cylinder to set up convection miling currents. The contents were then analyzed on a Perkin-Elmer Gas Chromotograph against a reference sample prepared by injecting 10 ml of pure methane into a 1000-ml flask. Three runs on each gas, with run-to-run errors under 5 percent, showed the calibration gas contained 1.34 percent of methane.

In use, the gas was equivalent to 1.34 percent/5.75 percent or 0.233 percent of typical fuel vapor. As may be seen from Figure 2, a calibration gas cylinder was readily available at the input manifold. Before, during, and after each run; the instrument was set either to 10,000-ppm full-scale (2330 ppm) in calibration, or 20,000-ppm full-scale (1165 ppm) as required by the experiment.

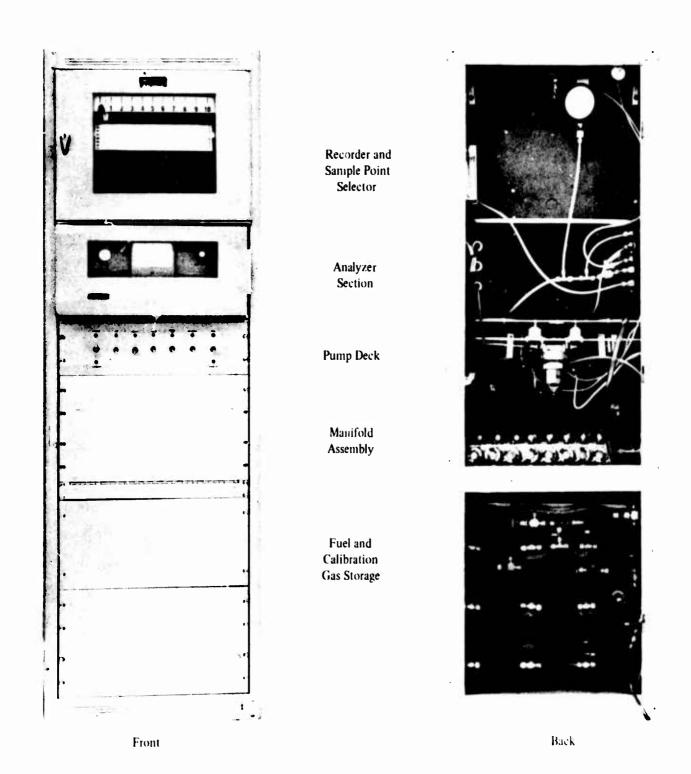


FIGURE 3. PHOTOGRAPH OF INSTRUMENT PACKAGE

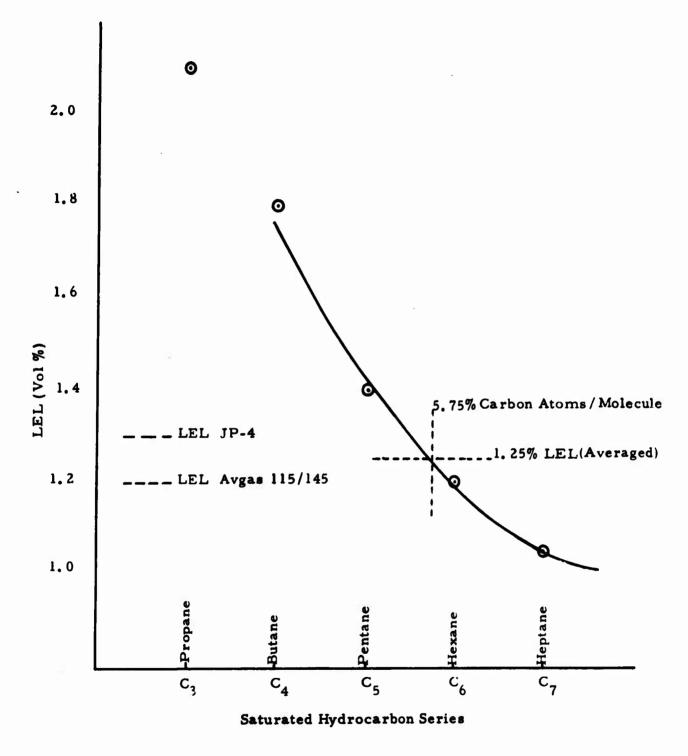


FIGURE 4. LOWER EXPLOSIVE LIMITS FOR FUELS AND VARIOUS SATURATED HYDROCARBONS

3. SAMPLING CONSIDERATIONS

For acceptable results, the sampling process must not affect the conditions being observed. The sample must be promptly analyzed, and, in a multipoint system, proper separations must be maintained. These criteria received continual attention during the program.

At no times were significant volumes being used for analysis. The sample and purge pumps continually removed approximately 1 cfm, and this was less than the air leakage in-and-out expectable in the 1600-cu ft enclosure involved. The samples were drawn parallel to the floor to avoid any effects on the vapor layer. No approach velocity could be noted above or below the sample point, and, even in the same plane, it was difficult to detect with a hot wire anemometer. Nevertheless, in the final vertical profile series when sampling at 1/2-in. intervals above the floor, a special stack was constructed to insure horizontal low-velocity laminar sampling.

The purge pump maintained a fresh sample at the manifold at all times. Calculations indicated that the typical lags between sample entry and arrival at the manifold were between 10 and 25 seconds.

For adequate separation between samples, the volume of the sample system must be minimized, and the flow must be made high enough to completely flush out the preceding sample before a new measurement is made. The initial shakedown runs showed obvious sample overlap when running at 5 sec/point. A speed of 7.5 sec/point was marginal if appreciable changes in vapor concentration occurred. Most of the work was carried out at 10 or 15 sec/point, except for the long duration runs in USAF hangars where 30 sec/point was deemed adequate. In addition, each sampling plan was based on graduated cycling from areas of high-vapor concentration to areas of low-vapor concentration and back again, avoiding abrupt changes in vapor values.

Sampling was under continual study during the program. During the latter phases, the instrument package was modified to reduce the original sample manifold volume from 9 cu in. to 1.5 cu in. and to meter the sample flow rate. With these improvements, an instrument response time of 5 sec/point was anticipated. The sample system performed as expected, but the recorder bridge balance circuit could not respond fast enough to make the 5-sec cycle feasible without further modifications. Excellent response was secured at 10 sec/point.

SECTION IV

TEST FACILITIES

The program required extensive testing in a simulated hangar space, a term which was not defined in the Statement of Work but was left to the interpretation of the contractor. It also specified field tests in USAF hangars selected as suitable to the purpose.

1. SIMULATED HANGAR SPACE

An aircraft hangar is essentially little more than a sizeable building designed for the storage and maintenance of aircraft. Large end doors are provided to permit passage in and out. Hangars are reasonably draft free, and, in temperate or cold climates, heaters are installed for working comfort. Aircraft shelters and nose docks meet this general description, also.

For the purposes of these tests, it was felt that as long as a semiquiescent environment could be secured, size (within reason) was not especially important. An unused concrete structure with a builtup joist roof was available which would supply a 14 × 14-ft working space and an adjoining 10 × 10-ft instrument room. This was rehabilitated for the purpose, and a floor plan is shown in Figure 5. An inside view of the experimental space is shown in Figure 6.

In order to investigate the effect of drafts coming from under a hangar door, a 4-in. plenum space was constructed across the inside east wall. This extended to within 2 in. of the floor and connected to two 18-in., low-capacity, tangential blowers set into the wall. Only one was used in testing. The second was utilized to expedite ventilation between tests. Typical velocities produced during tests are indicated in Figure II-1 of Appendix II.

A 4-in. low-power, shaded-pole fan was placed in one corner to produce floor drafts from ventilation inside the building. The velocities are noted in Figure II-3 of Appendix II.

For the first part of tests all sample lines were supported on ringstands. A plastic-covered, wire-grid system was then installed for mounting the polyethylene sample lines and securing better spatial distribution. Diagrams of the sample locations (Figs. II-1 through II-9) are included in Appendix II. Portable electric unit heaters were used prior to all runs at high-ambient temperatures to achieve the desired conditions.

2. SELECTED USAF HANGARS

A survey of the San Antonio area showed numerous hangars which could be made available to the program. The requirement essentially was for one or more large hangars which, on occasion, were filled with fueled aircraft and where vapor concentration measurements could be made over a 2- or 3-day period under closed door conditions. Three hangars were considered at Kelly AFB, four at Randolph AFB, and three at Bergstrom AFB. The final choices were Hangar 935 at Kelly AFB (Texas Air National Guard, F-100's); Hangar 5 at Randolph AFB (Air Training Command, T-38's); and Hangar 4337 at Bergstrom AFB (Tactical Air Command, RF-4's). The respective commands afforded excellent cooperation in making these hangars available and in aiding project personnel in setting up the instrument package. Randolph AFB officials were especially helpful in authorizing the desired large-scale spill test at the conclusion of the monitoring runs. Sketches showing sample points of the hangars and their aircraft occupancy are included in Appendix II. Figure 7 is a photograph of the aircraft in Hangar 5 at Randolph AFB during Test 26. The aircraft shown represented maximum hangar parking occupancy. The tests at Kelly AFB and Bergstrom AFB were conducted with maximum maintenance occupancy. The spill test at Randolph AFB is illustrated in Figure 8, while the Bergstrom tests are shown in Figure 9. The number and positions of aircraft in occupancy are shown as Figures II-6, II-7, and II-9 of Appendix II.

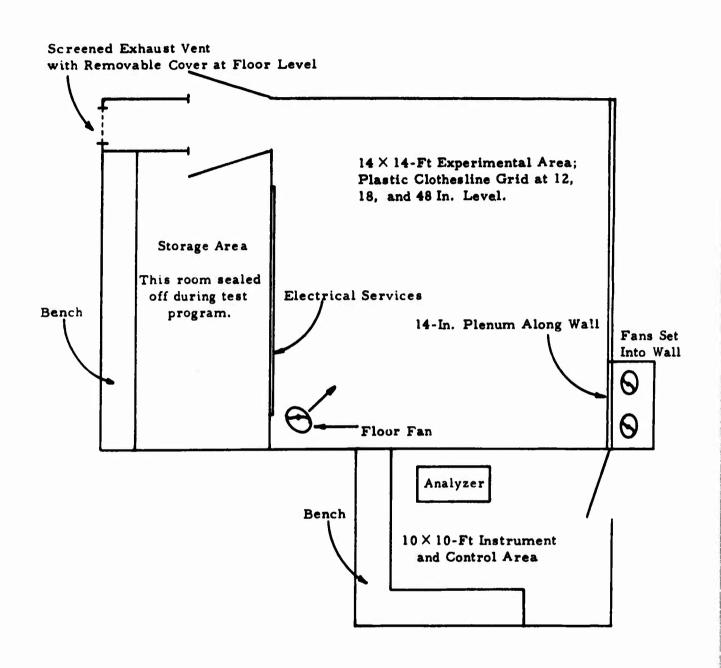


FIGURE 5. FLOOR PLAN-SIMULATED HANGAR SPACE

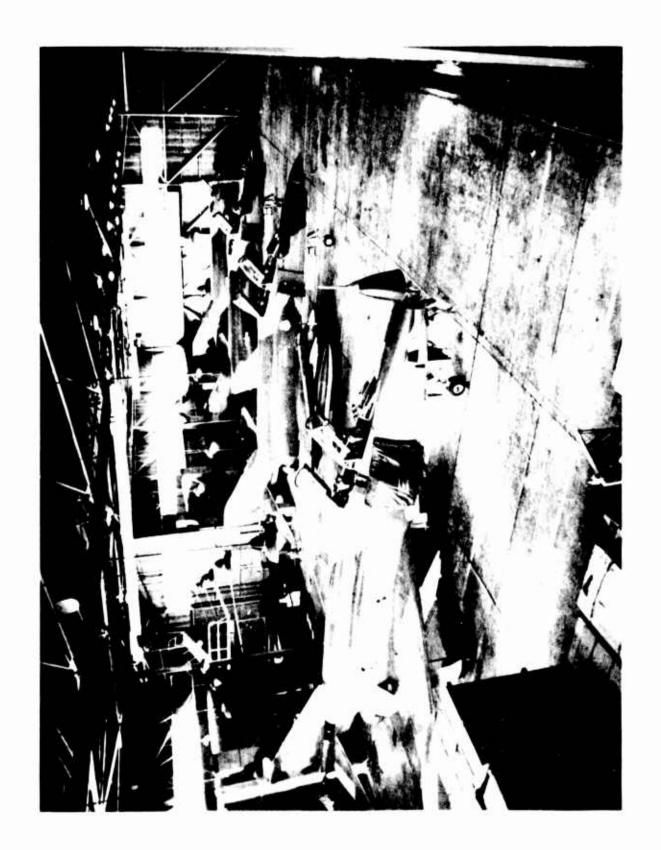


FIGURE 6. INTERIOR VIEW OF SIMULATED HANGAR SPACE





FIGURE 8. VIEW OF HANGAR 5, RANDOLPH AIR FORCE BASE SPILL TEST 27



SECTION V

TEST PROGRAM CHRONOLOGY AND TABULATED RESULTS

In the absence of any known information on the subject, the experimental approach was almost completely empirical. The test facility attempted to simulate actual conditions in actual buildings so as to determine what could be expected in USAF hangars under spill or leakage conditions. As the data from each run were collected, they were used to plan succeeding tests until the character of the vapor distribution pattern began to make itself evident and the relative importance of the variables could be discerned. This resulted in three separate but interrelated phases for the simulated hangars plus a fourth phase of field testing in actual hangars at USAF bases.

1. PHASE 1

Tests 1 through 5 were exploratory in nature, investigating the way in which vapor from an open pan would spread along a single vertical plane at 4 to 16 in. above the floor, starting above the pan in the center and extending toward the wall. It also measured the effect of dumping fuel on the floor and introducing floor drafts. The sampling plan appears in Appendix II as Figure II-1. The results are summarized in Table 1.

The Phase 1 data did not support previously held theories on vapor distribution and on the magnitude of the explosibility hazard. Accordingly, the recorded values were not considered acceptable until they had been checked and confirmed by an MSA Model 2A Explosibility Meter. Even though the facility provided an essentially draft-free, quiescent environment and no obvious air movements could be detected, it was concluded that some air currents did, in fact, exist which could dilute the vapor concentrations at the immediate liquid surface or divert rich mixtures away from the sample points.

2. PHASE 2

In the light of the Phase 1 results, the logical step was to increase the spatial coverage of the sampling and investigate vapor concentrations at significant levels between floor and ceiling. A support grid of plastic-coated wire simplified location of sample points at 2, 12, 18, and 48 in. above the floor and at the 96-in. ceiling level. Five locations were checked at each level. These were 2 ft from the walls at each corner, corresponding to the hazard area definition used in AFM 88-15, and in the center of the room.

Phase 2 work included a total of twenty-two tests with an ambient temperature range of 50°F to 98°F. Relative humidity was also recorded, but it was quickly apparent that humidity did not affect the results. Phase 2 results are summarized in Table 2.

While the Phase 2 work was in progress, it was learned (Ref. 6) that Eastman Kodak had been conducting a comparable program on various solvents, both in the laboratory and in a 20 × 40 × 15-ft plastic-covered, field facility. This work confirmed the importance of convection mixing currents in producing low vapor concentrations and the inapplicability of diffusion law theories. Accordingly, even though the quiescent air conditions in the facility appeared representative of typical installation, special efforts, including the use of smoke bombs to indicate air leakage, were made to secure a tight vapor seal. Test 19 and succeeding runs were made with the better sealed facility. These were essentially a repetition of Tests 10 through 14 and 17 to check the effect of possible air cross-currents and improve the validity of the earlier data. As may be seen by comparing the data of Table 2, higher maximum values were usually observed close to the floor in the sealed chamber, indicating that vapor leakage in an unsealed building can be appreciable. There were no significant differences at higher levels.

After consultation with the Project Monitor, the accumulated data were made available to Eastman Kodak for analysis and a conference arranged to compare the two programs. It was found (Ref. 7) that although the experimental approaches differed appreciably, the results were generally in good agreement. The Eastman Kodak work has not been completed, and no decision has yet been reached on publication.

3. PHASE 3

As the investigation proceeded, it became increasingly apparent that vertical profile information on vapor concentrations would be needed. While maximum values exceeding the LEL were occasionally noted at the 2-in. level, values were never

TABLE 1. MAXIMUM VAPOR CONCENTRATIONS IN A 200-SQ-FT CLOSED ROOM, QUIESCENT CONDITIONS, SAMPLING IN A SINGLE PLANE

(LEL = 12.500 ppm)

			Test	Test Number		
Test Parameters	1	2	3	4a*	4P*	5
Fuel	avgas	JP-4	avgas	avgas	avgas	JP-4
Vapor Source	pan	pan	pan	spill	spill with	pan
					exhaust	
Wetted Area (sq ft)	9	9	Š.	35	35	ĸ
Total Area (%)	3	3	2.5	17.5	17.5	2.5
Temperature (°F)	7.1	73	62	9	63	99
Vapor Concentration					})
(ppm) at:						
16 In. Above Floor	1400	1100	730	3950	920	355
12 In. Above Floor	1600	1250	715	4100	950	150
8 In. Above Floor	1800	1240	999	4850	950	220
4 In. Above Floor	3350	2300	1000+	9750	006	475
Time to Reach Maximum (min)	24	72	114	24	n/a	96

*Tests 4a and 4b continue Test 3. Pan was dumped on floor. After peak concentration had been reached, air inlet fan was started.

TABLE 2. MAXIMUM VAPOR CONCENTRATIONS IN 200-SQ-FT CLOSED ROOM. QUIESCENT CONDITIONS, SAMPLING IN THREE VERTICAL PLANES

Value Valu						Test Number	•			
Value Process	lest Parameters	ь	7	8	9	10	11	12	13	14
Value Valu	Final	ALVAS	JP-4	AVEAS	JP-4	JP-4	AVEAS	AVEAS	Avgas	JP-4
Netred Area (sp. 1) 5 5 10 10 30 30 30 98 96 Tota' Area (sp. 1) 25 25 5 5 5 15 15 49 48 Temperature (*F) 60 75 72 54 71 79 52 98 Vapor Concentration (5pm) at 1 Spm Str. 1 96 1, 100 1, 100 2, 500 2, 500 1, 100 2, 500 2, 100 1, 100 2, 500 2, 100 1, 10		•			2-gal drip	4-gal drip		••		4-gal spil
Total Area (%)										98
Temperature (*F)			-							48
Vapor Concentration										95
\$\frac{\psi}{\psi} Above Floor \$520 \$455 \$2,700 \$850 \$800 \$1,100 \$2,500 \$2,500 \$2,600 \$4810. Above Floor \$790 \$655 \$3,450 \$1,050 \$950 \$1,450 \$3,300 \$7,300 \$2,12 \$16. Above Floor \$790 \$655 \$3,450 \$1,050 \$1,050 \$1,850 \$5,200 \$9,200 \$3,12 \$16. Above Floor \$16,0000 \$2,850 \$10,0000 \$3,700 \$1,000 \$1,900 \$7,000 \$10,000 \$4,000 \$2.0000 \$1,000 \$1,000 \$1,900	The state of the s	617	, ,	••	,,	••	• • •	36	70	70
\$6 \ \text{lin.} \ \ \text{Acception} \text{520} \text{455} \text{2,700} \qq \qq \qq \qq \qq \qq \qq \qq \qq \qq \q										
48 In. Above Floor 840 620 2,800 1,050 950 1,450 3,300 7,300 2, 18 In. Above Floor 790 655 3,450 1,050 1,050 1,850 5,200 9,200 3, 12 In. Above Floor 920 750 3,700 1,000 1,050 1,050 1,950 7,000 10,000 4, 2 In. Above Floor 1C,000+ 2,850 10,000+ 3,700 5,100 9,450 20,000+ 19,800 20, Time to Reach Maximum (min) 10 4 34 282 60 258 3 3 3 Test Number Test Parameters 15 16 17 18 194 200 210 220 Fuel avgas avgas JP-4 JP-4 JP-4 JP-4 JP-4 JP-4 avg 4-gal spill 10-gal spill 4-gal		6.36	48.6	3 700	960	800	1 100	3 600		2 200
18 In. Above Fluor 790 665 3,450 1,050 1,050 1,850 5,200 9,200 3, 12 In. Above Floor 920 750 3,700 1,000 1,050 1,950 7,000 10,000 4, 2850 10,000+ 3,700 5,100 9,450 20,000+ 19,800 20, 20 2 In. Above Floor 10,000+ 2,850 10,000+ 3,700 5,100 9,450 20,000+ 19,800 20, 20 2 In. Above Floor 15 16 17 18 190 200 210 220 2 In. Above Floor 4,000 4,000 1,500 4,000 1,500 4,000 1,500 1, 48 In. Above Floor 3,600 1,800 1,800 2,300 6,700 5,800 7,400 2,500 5, 200 1,600 1, 1									2 100	2,700
12 In. Above Floor 920 750 3,700 1,000 1,050 1,900 7,000 10,000 4, 2 In. Above Floor 10,000+ 2,850 10,000+ 3,700 5,100 9,450 20,000+ 19,800 20, 20 21 22 22 22 23 23 23 24 24					•					2, 900
2 In. Above Floor 1C,000+ 2,850 10,000+ 3,700 5,100 9,450 20,000+ 19,800 20, 200 19,800 20, 200 20,000+ 20,0				•			•			3, 200
Time to Reach Maximum (min) 10 4 34 282 60 258 3 3 3		,								4, 400
Test Parameters 15 16 17 18 194 204 214 224 225	2 In. Above Floor	10,000+							19,800	20, 000+
Test Parameters 15	Time to Reach Maximum (min)	10	4	34	282	60	258	3	3	4
Fuel vapor Source A-gal spill 10-gal spill 4-gal spill 10-gal spill 10-gal spill 10-gal spill 10-gal spill 10-gal spill 4-gal spill 4-ga		- 101		-						
Vapor Source	Test Parameters	15	16		18	19*	20+	21+	22*	30*
Vapor Source	Fuel	AV#3.0	AV#38	1P-4	JP-4	JP-4	1P-4	1P-4	10.4	avgas
Wetted Area (sq (t) 98 156 98 176 98 98 98 98 98 98 78 70 70 70 70 88 49 40 1,500 1										4-gal spill
Total Area (%)	•									96
Temperature (*F) 52 60 50 64 67 67 61 77 Vapor Concentration (ppm lat:					100					48
Vapor Concentration (ppm) at:										
(ppm) at:		36	00	,,		• • •		01	• • • • • • • • • • • • • • • • • • • •	82
Section Sect	•									
48 In. Above Floor 2,600 1,600 1,500 2,800 2,700 1,200 4,300 1,000 1, 16 In. Above Floor 3,600 1,800 1,800 2,300 6,700 5,800 7,400 2,500 5, 12 In. Above Floor 4,600 3,500 1,550 3,900 10,100 7,800 10,200 4,300 8, 2 In. Above Floor 20,000+ 20,000+ 10,200 20,000+ 20,000+ 20,000+ 20,000+ 20,000+ 20, Time to Reach Maximum (min) 0 7 11 7 3 7 7 7 Test Number Test Number		2.400	1.700	1.600	1.800	2. 900	1.600	4, 400	1.500	1, 750
18 In. Above Floor 3,600 1,800 1,800 2,300 6,700 5,800 7,400 2,500 5, 12 In. Above Floor 4,600 3,500 1,550 3,900 10,100 7,800 10,200 4,300 8, 2 In. Above Floor 20,000+ 20,000				1.500	2.800	2, 700	1. 200			1, 900
12 In. Above Floor 4,600 3,500 1,550 3,900 10,100 7,800 10,200 4,300 8, 2 in. Above Floor 20,000+ 20,000+ 10,200 20,000+ 20,00										5, 650
2 fm, Above Floor 20,000+ 20,000+ 10,200 20,000+ 20,00										8, 700
Time to Reach Maximum (min) 0 7 11 7 3 7 7 7 Test Number Test Number		., .								20.000+
Fuel avgas JP-4 JP-4 avgas avgas JP-4 JP-4 Vapor Source floor fan 4-gal spill floor fan 4-gal drip floor fan 4-gal										3
Fuel avgas JP-4 JP-4 avgas avgas JP-4 JP-4 Vapor Source floor fan 4-gal spill floor fan 4-gal drip floor fan 4-gal					Test liumber					
Vapor Source floor fan 4-gal spill floor fan 4-gal drip floor fan 4-gal drip floor fan Wetted Area (%) 96 94 38 25 35 25 Total Area (%) 48 48 47 18 12.5 17.5 12.5 Temperature (*F) 82 89 90 90 85 85	Fr . atterte rs	30**	31*	31++			330	3300		
Vapor Source floor fan 4-gal spill floor fan 4-gal drip floor fan 4-gal drip floor fan Wetted Area (ag ft) 96 96 94 38 25 35 25 Total Area (%) 4n 48 47 18 12.5 17.5 12.5 Temperature (*F) 82 89 90 90 85 85	Fuel	BV636	1P-4	1P-4	24584	20025	JP-4	IP.4		
Wetted Area (%) 96 94 38 25 35 25 Total Area (%) 46 48 47 18 12.5 17.5 12.5 Temperature (*F) 82 89 90 90 85 85					**	-		•		
Total Area (%) 48 48 47 18 12.5 17.5 12.5 Temperature (*F) 82 89 89 90 90 85 85										
Temperature (°F') 82 89 90 90 85 85										
					1.7					
Vapor Concentration		82	77	07	70	90	67	87		
(ppm) at:		1 150	174	116			3 000	1 700		
16 In. Above Floor 1, 250 275 125 3,500 585 2,000 1,700								•		
4h In. Above Floor 1,900 350 350 5,900 640 3,300 2,300										
18 In. Above Floor 1,900 450 450 7,600 675 4,300 3,075					1115-000					
12 In. Above Floor 1,900 550 475 8,850 695 5,400 3,050							-	•		
2 In. Abrive Floor 2, 250 10, 150 2, 750 20, 000+ 930 20, 000+ 13, 000	2 In. Above Floor	2, 250		-		930				
Time to Reach Maximum (min) 33 55 68	Time to Reach Maximum (min)	*	33	• • •	55	• • •	68			

Note: Values shown as 10,000+ and 20,000+ were slightly over range of instrument but did not warrant a change in scale.

Values are short time maximums. Duration may be obtained from data plots or tables in Appendixes III and IV.

see onfigurations II-2 and II-3 for sampling details.

^{*}Extra care taken in sealing room.
**Small fan on floor in corner aimed at center to simulate floor drafts.

observed at the next level, 12 in. above the floor, nor at the 18-in. level used in NEC Par. 513, nor at the 48-in. level used in AFM 88-15 to define the hazard zone. Tests 23 and 29 measured the vertical profiles for JP-4 and avgas spills at 2-in. intervals up to 24 in. above the floor in a sealed environment. As may be seen from the data of Table 3, the LEL could exist at 4 and 6 in. above the floor. Additionally, Tests 34 through 37 were run to examine the profile in more detail, sampling at 1/2-in. increments. Since the lowest points were close enough to the liquid surface of the spill so that surface conditions could be affected by sampling, extra care was taken through the use of a laminar flow, low-velocity sampling deck. The results of the Phase 3 tests are plotted in Figure 10 which shows that even when plotting short time maximums in a nontypical sealed environment, the actual hazard zone for the most volatile fuel was less than 8 in. above the floor.

4. ALL-PHASE WORK

Repeated checks were made of the effects of movements at floor level. It had been noted in Phase 1 that if project personnel entered the test chamber and walked across the room, the vapor concentration temporarily dropped at the 4-in, level. Tests 4b and 5 documented the air movement effect when a draft was simulated under the hangar door. The cross floor velocity was approximately 75 ft/minute. Air movement was again investigated during Tests 30 through 33, when a 4-in, flow fan was operated for a short time during the test. The location of the fan and air velocities are shown in Figure II-3 of Appendix II. In every case, any disturbance of the air at floor level immediately reduced the vapor concentration until the movement was stopped, at which time it gradually returned to near its previous equilibrant value.

5. PHASE 4

The required field tests in USAF hangars were planned on the basis of information from Phases 1, 2, and 3. Since the observed vapor concentrations had been so low in the small sealed test facility, it appeared that meaningful results in large open area hangars could be secured only in worst-case situations such as with tightly closed doors, maximum fueled aircraft occupancy, and conditions when fuel leaks or drips could occur.

Hangar doors are normally open during operations. A survey was taken, however, which revealed weekend periods for some hangars at Kelly AFB, Randolph AFB, and Bergstrom AFB during which "worst-case" tests could be run. The aircraft involved were the F-100, T-38, and RF-4. With the complete cooperation of all three Air Force Commands, weekend monitoring tests were set up at the three bases. These were designated as Tests 24 through 28. The sampling plans are shown in Figures II-6, II-7, and II-9 of Appendix II, while the results are listed as Table 4.

The large-scale spill test, which was to be run if a suitable facility could be obtained, was carried out as Test 27 at Randolph AFB, after conclusion of the monitoring tests. Hangar 5 was cleared of aircraft, and the doors were closed. The floor area, including two adjacent shops, was covered with sample lines as shown in Figure II-8 of Appendix II. The floor drains were sealed. With the Base Fire Department standing by to observe and monitor, a drum of JP-4 fuel was dumped on the floor. The test ran approximately 2-1/2 hr, after which the doors were opened and the floor washed down. The data for this test appear in Appendix IV as Table IV-27. Fire Department checks with a MSA Model 2A Explosibility Meter showed values at or above the LEL only at the immediate liquid level in a single low spot of the floor at the drain.

6. DATA REDUCTION

A total of 124,122 data points were recorded during this study covering some 600 hr of test operation. The tabulated data for each run are included as Appendix IV. To visualize better the physical relationships, the runs in the test facility have been plotted against time for various heights above the floor and are included as Appendix III. From these curves, it may be seen that the maximum vapor concentration values are of relatively short duration. Except close to the floor, the vapor explosibility hazard is essentially nonexistent.

No effects could be noted that related to barometric pressure or humidity. Theoretically, pressure or humidity would be relevant only if diffusion theory had been shown to be controlling, which was not the case.

In the same manner, the hazard differences between avgas and JP-4 fuels for spill conditions with limited amounts were not significant, nor was the temperature. Avgas and JP-4 are both essentially high-volatility fuels as far as flash point is concerned. Their volatile fractions are almost the same. The primary difference between these fuels is the amount per gallon of each fuel that will readily evaporate in a given length of time. Differences in ambient temperature vary the thermal driving force which is measured from the below-zero (°F) flash point. At elevated temperatures, the volatile fractions of both fuels

TABLE 3. VERTICAL PROFILES OF MAXIMUM VAPUR CONCENTRATIONS IN SEALED ROOM

Test No.	23	29	7.	ž	72	r
Foel	1P.4				ŝ	
	4-10-1	TO THE TOTAL OF TH	m 1000	4-40 	37838	84848
Area (89 ft)	10d 10d	111de 1985	1-gal apill	4-gal spill	4-gal spill	4-gal drip
Area (%)	2+	64	75	09	2	0 0
Temp (F)	62	69	75	83	87	92
Height Above Floor						
(in.)	bbm	mdd	mdd	bbm	mdd	шdd
24	1200	1300		'	.	
22	1300	1500	,			•
20	1700	2900	1	• •	, (• =
18	1700	3300	•	•		
16	1300	3900	•	. 1	1	
14	1600	4100	•		•	•
12	1500	5200	8100	4300	5900	7400
11.5	•	•	8600	4400	5800	7400
11.0	•	•	8300	4400	2900	7400
10.5	•	1	0006	5400	9500	7600
10.0	1900	7100	8900	2900	6300	7800
9.5	•	•	10000	6200	6400	2900
9.0	•	1	9800	9029	9400	8100
8.5	•	•	10800	7100	6700	8300
8.0	3600	9200	10600	7300	0072	8500
7.5	•	1	11600	7600	7400	8800
7.0		ı	11700	7900	1900	0006
• • •	•	1	12400	6200	8100	9300
0.9	9200	12100	12700	8500	8800	9500
5.5		•	13300	8600	8900	9800
5.0	•	1	13400	8800	9500	10300
4.5	•	1	14100	0006	9500	10500
4.0	13300	16900	14100	9300	0066	10600
3.5	•	ı	14900	9500	10400	10900
3.0	•	i	14900	10100	10800	11200
2.5		1	15900	10100	11100	11300
2.0	16000	19800	00091	10500	11600	11600
1.5		•	16600	10600	12100	11930
1.0	•	•	16700	11000	12600	12300
0.5	•	,	18400	12200	13800	13900

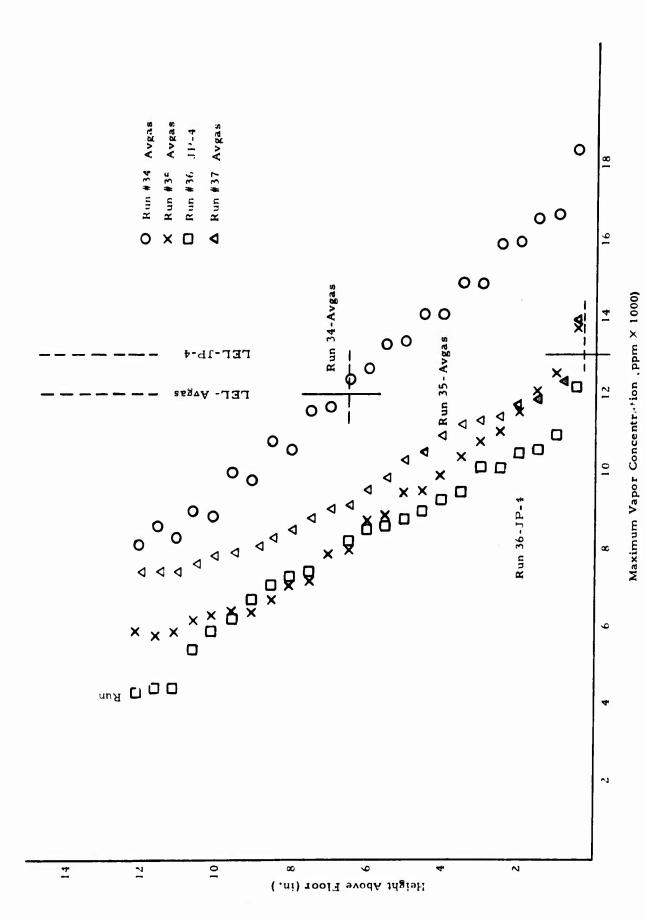


TABLE 4. MAXIMUM VAPOR CONCENTRATIONS IN SELECTED TYPICAL USAF HANGARS

(LEL 12,500 ppm)

28 JP-4 monitor Bergstrom AFB RF-4 46-66	NA NA 1000+** 61 hr 36 min
27 JP-4 55-gal spill Randolph AFB None 57	1175 1755 2660* 3 hr 48 min
26 JP-4 monitor 55-9 Randolph AFB Ran T-38	NA NA 24 63 hr 18 min
25 JP-4 monitor Kelly AFB F-100 65	NA NA 26 118 hr 30 min
24 JP-4 monitor Kelly AFB F-100 65	: NA NA 40 45 hr 30 min
Test No. Fuel Type Location Aircraft Temperature (°F)	Vapor Concentration (ppm) at: 18 In. Above Floor 10 In. Above Floor 2 In. Above Floor Length of Run

^{*}Maximum value in two adjoining rooms, door closed, was 340 ppm at 35 min.

from wing tank fuel expansion. Typical maximums in other areas were 50 ppm or less. **Maximum value was recorded 6 in. from 2×4 ft $\times 3$ -in. pan catching dripping JP-4

would evaporate more rapidly and be dissipated sooner. That is, the vapor concentrations reached would be strongly affected by temperature differences within the room. The temperature differences also act as the driving forces for the diluting convection currents within the room.

SECTION VI

ANALYSIS OF RESULTS AND CONCLUSIONS

1. DISCUSSION OF THE TEST RESULTS

At the outset of the program, it was expected that spills and leaks in aircraft hangars would follow a general pattern predictable from classical diffusion theory. If this were true, then for any given time after a spill, it would be possible to calculate the accumulated vapor build-up from the floor, up to any level.

An example of such a theoretical calculation for benzene is shown as Figure 11 (Ref 8). Zabetakis (Ref 5) gives 1.3 percent and 7.9 percent, respectively, for the LEL and UEL values of this material. These are about the same as for aviation fuel vapors so that the chart for such spills would be comparable.

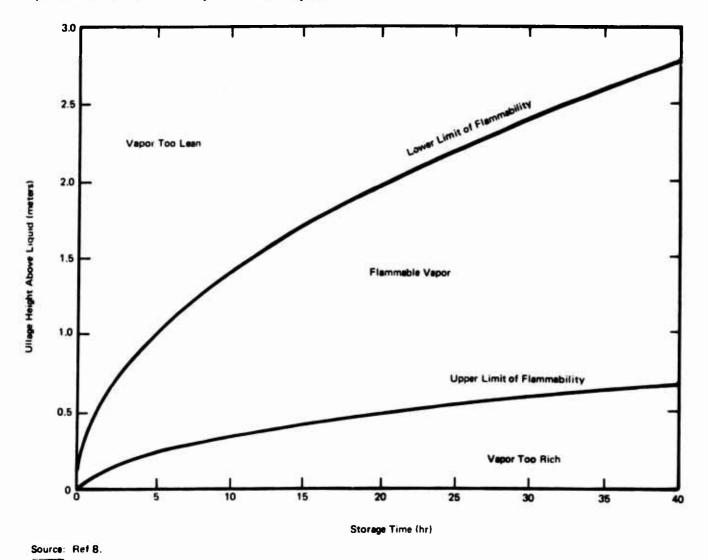


FIGURE 11. CALCULATED DIFFUSION OF BENZENE INTO AIR

These calculations assumed an unlimited supply of the pure compound, an isothermal environment, and only molecular diffusion forces to accomplish the liquid-vapor-air mixing process. Such assumptions are completely unrealistic for the spill of some definite quantity of an aviation fuel, consisting of a blended hydrocarbon mixture in a building where floor-to-wall-to

ceiling temperature differences set up small but appreciable convection currents. Also, it has been believed that after any spill, the rapid flashoff of volatiles would create a rich vapor which would drift or be moved by convection currents, essentially undiluted, toward potential ignition points. Obviously, such a condition could be hazardous and would justify establishment of appropriate safety standards.

None of the experimental work conducted in this program supported this rich cloud concept. They did show that under extreme spill conditions in a small confined area, the vapor concentration could gradually build up and approach the LEL in a layer as high as 7 in, above the floor. The general vertical profile of maximum observed values, irrespective of time reached, is illustrated in Figure 10. It was also noticed that for any spill in a quiescent environment where the fuel collected in small pools on a rough concrete floor, a value near the LEL at the 1/2-in, level could continue for several hours. In the laboratory facility, maximum values slightly over 20,000 ppm were recorded at the 2-in, level on numerous occasions, but these could not be produced at will. Low-velocity convection currents produced by floor-wall-ceiling temperature differences appeared to be the controlling factor. Any disturbance causing air movement, regardless of how produced, caused dissipation of rich vapors and lowering of concentrations. As previously pointed out, the effect was noticeable whenever project personnel entered the chamber causing some air movement during a run. This was documented several times.

The concentrations observed in the confined test facility do not necessarily apply to typical USAF hangars with their large open areas where both convection currents and cross ventilation from external wind pressures can quickly sweep away and dilute fuel vapors to safe levels.

In Test 27, the open floor fuel spill at Randolph AFB, none of the readings at the 2-in. level exceeded 2660 ppm (21% of LEL), even at the edges of the spill. Scanning with an MSA Explosimeter showed readings above the LEL only at the immediate fuel surface in a low spot on the floor. The rich vapor layer, if any existed, could not be found as high as 1/2 in. off the floor. Under such conditions, it would not be logical to expect vapor travel along the floor into the adjacent hangar offices and shops, where none was detected.

A comparable effect was noted during Test 28 at Bergstrom AFB, when the area beside a 2 X 4-ft pan receiving JP-4 from a dripping RF-4 fuel tank never exceeded 1000 ppm (8% of LEL) at the 2-in. level.

The mass of data gathered in this study indicate that the overall mechanism is one in which the generation of vapor is evaporation-rate limited. That is, it is controlled by the ambient temperature and the vapor pressures of the volatile compounds in the fuels spilled.

The vapor concentrations in the spill area are determined by an equilibrium between the quantity of vapor evolved and the rapidity with which it is swept away and diluted by air currents. Classical diffusion theory, as such, does not apply under these conditions. Comparable results were obtained by Eastman Kodak in the previously cited work (Ref 7).

The data also indicate that most environmental factors have relatively little effect upon the results. Ambient temperature, barometric pressure, and relative humidity were found to be irrelevant. The differences between avgas and JP-4 were not appreciable. Both are high-volatility fuels and act in much the same manner. With any straight kerosene low-volatility fuel (such as JP-5, JP-8, or Jet A), the estimated hazard zone would appear to be well under the 2-in, level. A high degree of confinement and a volatile fuel can raise the hazard zone up to approximately 6 to 7 in, above the floor. Under such conditions, there is little or no justification for some protective techniques such as vapor seal barriers or pressurizing areas to prevent inward vapor flow.

Any device to produce positive air movement at floor level will immediately reduce the vapor concentration at the floor to a low level. This was demonstrated in Test 4B and again in Tests 30 through 33. For any confined area subject to spills, the use of an exhaust fan taking suction at floor level would be a logical and effective safety measure.

The objective of this research effort was to determine the extent of hazardous concentrations of explosive vapors in aircraft hangars in order to define areas which require explosion-proof electrical wiring and equipment. From the values shown in Figure 10 for a confined area, which is in itself an extreme situation, it can be seen that the nonhazardous area for hangars could be established as beginning at 12 inches above the floor and still retain an adequate margin of safety. This conclusion is supported by the results of actual tests in USAF hangars.

In the absence of measuring equipment, a strong smell of fuel vapors tends to alert personnel to the possible existence of an explosion hazard. It was noted again and again that such smells could exist at concentrations as low as 50 ppm—far below the LEL. The light petroleum vapors which constitute the hazard are odorless. The residual sulfur components which can be detected by the nose are no index as to the vapor concentration and can lead to highly erroneous conclusions as to the degree of hazard.

2. CONCLUSIONS

Presented in order, the following conclusions have been reached during the progress of the study:

- (1) Any spill or leak of a flammable liquid in a hangar can represent a fire hazard consistent with the amount released.

 The overall vapor explosibility hazard is low, of relatively short duration, and confined to a space only a few inches above the floor.
- (2) Even with the use of the most volatile fuels and spills covering up to 38 percent of the floor area, the expected vapor concentration was below the LEL at the 12-in, level. Thus, ordinary sized spills or leaks, representing up to 25 percent or more of the floor area, do not represent a serious vapor explosibility hazard. Ordinary washdown procedures not only reduce the fuel present but supply vapor mixing and dilution as well.
- (3) There appears to be little practical difference between avgas and JP4 in their vapor hazard aspects except that avgas has a higher volatile content. Avgas can be expected to vaporize more rapidly and reach a somewhat higher short period peak vapor concentration within the 12-in. distance.
- (4) Fuel evaporation rate is temperature dependent. As the ambient temperature is increased, vapor is released more rapidly, and the available volatiles are dissipated in less time. There appears to be no significant effect on vapor concentrations within normal hangar temperature ranges. Humidity and barometric pressure are insignificant factors in the evaporation process.
- (5) Since normal convection currents in hangars already serve to dilute and dissipate vapors (keeping them below the LEL at working levels), the effect of hangar door cracks and openings is not significant, except to further improve ventilation and decrease vapor concentrations.
- (6) No penetration of vapors through closed doors or wall openings into adjoining areas was observed during the spill test at Randolph AFB. There was an intervening 3-in, sill between the spaces, and blocking of the high concentrations expectable along the floor could have been due either to this low barrier or to dissipation of the vapor by convection currents before it reached the wall.
- (7) Inasmuch as no penetration of vapors into adjacent unpressurized areas could be observed, there is no justification for pressurizing to block vapor flow.
- (8) Experiments investigated the action of a floor level fan and showed it to be extremely effective in lowering vapor concentrations. This is a mixing and dissipating action and does not require the vapor to be exhausted from the building.
- (9) Reviewing the provisions of Paragraphs 7 through 10 Hazardous Areas, of AFM 28-15 in the light of the test program and the preceding conclusions, it appears that a redefinition of the hazards is warranted.

3. RECOMMENDED REVISED TEXT FOR PAR 7-10, AFM 88-15

The following is recommended as a revision of AFM 88-15:

7-10. Hazardous Areas:

- a. Requirements. Unless otherwise authorized, wiring materials and equipment within hazardous areas shall conform to the requirements for the particular hazard involved as specified in the National Electrical Code.
 - b. Hangars and Docks:
- (1) All spaces below grade shall be considered to be Class 1, Division 1, Group D of hazardous locations.
- (a) The entire area of the hangar, including any adjacent and communicating areas not suitably cut off, shall be considered to be Class 1, Division 2, Group D hazardous locations up to a level 12 in, above the floor.
- (b) Where docks and hangars are used for fuel system and fuel cell repairs, the above criteria are applicable provided that any other special treatment requirements are also met.
- (c) Wiring and equipment in nonhazardous areas shall meet the requirements of the National Electrical Code.
- (d) Adjacent areas cut off at floor level by a barrier not less than 3-ft high are considered nonhazardous unless the usage of the area is hazardous.
- c. POL Areas. All spaces below grade shall be considered Class 1, Division 1, Group D hazardous areas. The following spaces shall be considered Class 1, Division 2, Group D hazardous areas:
- (1) Above grade pump, valve rooms, or similar areas.
 - (2) Locations within 20 ft of tank vents.
 - (3) Locations within tank dikes.
- (4) Within 50 ft of tank loading or unloading outlets.
- d. General. Any spaces above ground normally considered to be Class 1 Division 2 may be specified to fall within Division 1 if evidence exists that vapor concentrations exceeding the LEL regularly exist at least 2 inches above grade in the vicinity of electrical equipment.

APPENDIX I

EXCERPTS FROM AFM 88-15 AND NATIONAL ELECTRICAL CODE

Excerpts from AFM 88-15, 3 March 1970

7-10. Hazardous Areas:

- a. Requirements. Unless otherwise authorized, wiring materials and equipment within hazardous areas shall conform to the requirements for the particular hazard involved as specified in the National Electrical Code.
 - b. Hangars and Docks:
- (1) The following spaces are considered to be class 1, division 1, group C of hazardous locations:
- (a) The main hangar or dock area inclosed by the building walls, exclusive of adjoining rooms, and extending from the floor to the top of highest hangar door, except for the space within 2 feet of the wall above a 4-foot level. (Special situations wherein encroachment may be acceptable due to particular aircraft size or configuration will be referred to AFOCE-KC.)
- (b) The space below a 4 foot level from the floor in adjacent areas not cut off from the main area by doors or walls.
- (c) The space below an 18 inch level from the floor in adjacent areas cut off from the main area by doors or walls subject to fume leakage.
- (2) Adjacent areas cut off from the main area by a minimum 4 foot elevation or by walls not subject to fume leakage are considered nonhazardous unless the usage of the specific area itself is hazardous.
- (3) All fixed electrical equipment and wiring should be located outside the hazardous space, wherever possible. If, in special cases, it is necessary to encroach into the hazardous space for installation of nonexplosion proof equipment, such equipment will be confined to the space 5 feet or more above the upper surface, or 5 feet or more horizontally out from the edges of the wings, fuselage, or any part of the aircraft which normally contains fuel tanks or vents for the largest aircraft that can be accommodated in the facility.

- (4) Where docks and hangars are used for fuel system and fuel cell repair the above criteria are applicable, provided other special treatment requirements (vapor detection, fuel disposal, and approved exhaust air movements) are also met.
- (5) Except as specifically stated above, all remaining electrical wiring and equipment shall meet requirements of the National Electrical Code.
- c. *POL Areas*. Electrical equipment will be explosion proof as approved for class 1, group C, division 1, locations when installed under the following conditions.
 - (1) In below-grade housing or pits.
- (2) In above-grade pump rooms, valve rooms, and similar areas.
- (3) Within 20 feet of vents for underground tanks.
- (4) Within dikes of above-ground tanks.
- (5) Within 50 feet of tank loading or unloading outlets.
- d. When required for industrial areas, explosion-pr of lighting fixtures will be of incandescent type. Fluorescent type is not permitted in these areas.

NATIONAL ELECTRICAL CODE

ARTICLE 500 — HAZARDOUS LOCATIONS

500-1. Scope. The provisions of Articles 500 through 503 apply to locations in which the authority having jurisdiction judges the apparatus and wiring to be subject to the conditions indicated by the following classifications. It is intended that each room, section or area (including motor and generator rooms, and rooms for the enclosure of control equipment) shall be considered individually in determining its classification. Except as modified in Articles 500 through 503, all other applicable rules contained in this Code shall apply to electrical apparatus and wiring installed in hazardous locations. For definitions of "approved" and "explosion-proof" as used in these Articles, refer to Article 100; "dust-ignition-proof" is defined in Section 502-1.

Equipment and associated wiring approved as intrinsically safe may be installed in any hazardous location for which it is approved, and the provisions of Articles 500 through 517 need not apply to such installation. Intrinsically safe equipment and wiring are incapable of releasing sufficient electrical energy under normal or abnormal conditions to cause ignition of a specific hazardous atmospheric mixture. Abnormal conditions will include accidental damage to any part of the equipment or wiring, insulation or other failure of electrical components, application of overvoltage, adjustment and maintenance operations, and other similar conditions.

For further information see NFPA No. 493-1969 Standard for Intrinsically Safe Process Control Equipment for use in Class I Hazardous Locations.

Through the exercise of ingenuity in the layout of electrical installations for hazardous locations, it is frequently possible to locate much of the equipment in less hazardous or in nonhazardous areas and thus to reduce the amount of special equipment required. In some cases, hazards may be reduced or hazardous areas limited or eliminated by adequate positive-pressure ventilation from a source of clean air in conjunction with effective safeguards against ventilation failure. For further information see NFPA No. 496-1967 Standard for Purged Enclosures for Electrical Equipment in Hazardous Locations. It is recommended also that the authority having jurisdiction be familiar with such recorded industrial experience as well as with

Table 500-2(b). Identification Numbers

Max Tempe	Identification	
Degrees C	Degrees F	Number
450 300 280 260 230 215 200 180 165 160 135 120	842 572 536 500 446 419 392 356 329 320 275 248 212	T1 T2 T2A T2B T2C T2D T3 T3A T3B T3C T4
<u>85</u>	185	T6

ARTICLE 500-HAZARDOUS LOCATIONS

70-289

Group D Atmospheres

Table 500-2(c). Chemicals by Groups

Group A Atmospheres

Chemical	Chemical
acetylene	acetone
	acrylonitrile
Group & Atmospheres	ammonia¹
butadiene ¹	benzene
ethylene oxide	butane
hydrogen	1-butanol (butyl alcohol)
manufactured gases containing more	2-butanol (secondary butyl alcohol)
than 30% hydrogen (by volume)	n-butyl acetate
propylene oxide	isobutyl acetate
	ethane
Group C Atmospheres	ethanol (ethyl alcohol) ethyl acetate
acetaldehyde	ethylacetate ethylene dichloride
cyclopropane	gasoline
diethyl ether	heptanes
ethylene	hexanes
isoprene	methane (natural gas)
unsymmetrical dimethyl hydrazine	methanol (methyl alcohol)
(UDMH 1, 1-dimethyl hydrazine)	3-methyl-1-butanol (isoamyl alcohol)
,	methyl ethyl ketone
	methyl isobutyl ketone
	2-methyl-1-propanol
	(isobutyl alcohol)
	2-methyl-2-propanol
	(tertiary butyl alcohol)
	petroleum naphtha'
	octanes
	pentanes
	1-pentanol (amyl alcohol)
	propane
	1-propanol (propyl alcohol) 2-propanol (isopropyl alcohol)
	propylene
	styrene
	toluene
	vinyl acetate
	vinyl chloride
	xylenes

¹ Group D equipment may be used for this atmosphere if such equipment is isolated in accordance with Section 501-5(a) by sealing all conduit ½-inch size or larger.

² Group C equipment may be used for this atmosphere if such equipment is isolated in accordance with Section 501-5(a) by sealing all conduit ¹2-inch size or larger.

For Classification of areas involving ammonia atmosphere refer to ANSI B9.1 Safety Code for Mechanical Refrigeration-1971 and ANSI K61.1 Storage and Handling of Anhydrous Ammonia-1971.

⁴A saturated hydrocarbon mixture boiling in the range 20-135°C (68-275 F). Also known by the synonyms benzine, ligroin, petroleum ether or naptha.

- **500-4.** Class I locations. Class I locations are those in which flammable gases or vapors are or may be present in the air in quantities sufficient to produce explosive or ignitible mixtures. Class I locations shall include the following:
- (a) Closs I. Division 1. I ocations (1) in which hazardous concentrations of flammable gases or vapors exist continuously, intermittently, or periodically under normal operating conditions. (2) in which hazardous concentrations of such gases or vapors may exist frequently because of repair or maintenance operations or because of leakage, or (3) in which breakdown or faulty operation of equipment or processes which might release hazardous concentrations of flammable gases or vapors, might also cause simultaneous failure of electrical equipment.

This classification usually includes locations where volatile flammable liquids or liquefied flammable gases are transferred from one container to another, interiors of spray booths and areas in the vicinity of spraying and painting operations where volatile flammable solvents are used; locations containing open tanks or vats of volatile flammable liquids; drying rooms or compartments for the evaporation of flammable solvents; locations containing fat and oil extraction apparatus using volatile flammable solvents; portions of cleaning and dyeing plants where hazardous liquids are used; gas generator rooms and other portions of gas manufacturing plants where flammable gas may escape; inadequately ventilated pump rooms for flammable gas or for volatile flammable liquids; the interiors of refrigerators and freezers in which volatile, flammable materials are stored in open, lightly stoppered, or easily ruptured containers, and all other locations where hazardous concentrations of flammable vapors or gases are likely to occur in the course of normal operations.

(b) Class 1, Division 2. Locations (1) in which volatile flammable liquids or flammable gases are handled, processed or used, but in which the hazardous liquids, vapors or gases will normally be confined within closed containers or closed systems from which they can escape only in case of accidental rupture or breakdown of such containers or systems, or in case of abnormal operation of equipment. (2) in which hazardous concentrations of gases or vapors are normally prevented by positive mechanical ventilation, but which might become hazardous through failure or abnormal operation of the ventilating equipment, or (3) which are adjacent to Class I. Division 1 locations, and to which hazardous concentrations of gases or vapors might occasionally be communicated unless such communication is prevented by adequate positive-pressure ventilation from a source of clean air, and effective safeguards against ventilation failure are provided.

This classification usually includes locations where volatile flammable liquids or flammable gases or vapors are used, but which, in the judgment of the authority having jurisdiction, would become hazardous only in case of an accident or of some unusual operating condition. The quantity of hazardous material that might escape in case of accident, the adequacy of ventilating equipment, the total area involved, and the record of the industry or business with respect to explosions or fires are all factors that should receive consideration in determining the classification and extent of each hazardous area.

Piping without valves, checks, meters and similar devices would not ordinarily be deemed to introduce a hazardous condition even though used for hazardous liquids or gases. Locations used for the storage of hazardous liquids or of liquefied or compressed gases in sealed containers would not normally be considered hazardous unless subject to other hazardous conditions also

Electrical conduits and their associated enclosures separated from process fluids by a single seal or barrier shall be classed as Division 2 locations if the outside of conduit and enclosures is a nonhazardous area.

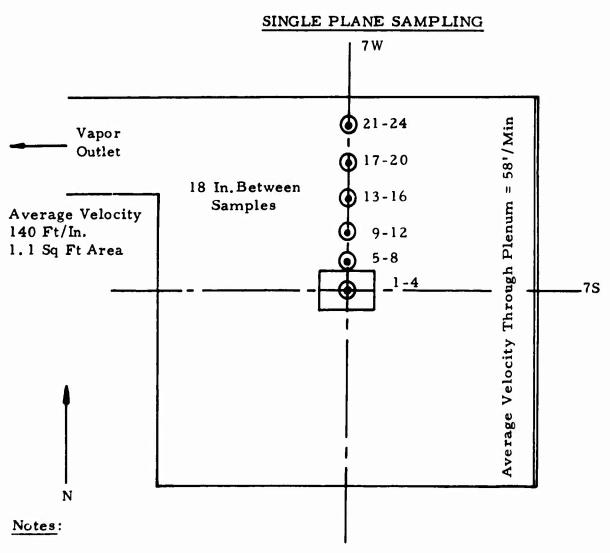
ARTICLE 513 — AIRCRAFT HANGARS

- 513-1. Definition. This occupancy shall include locations used for storage or servicing of aircraft in which gasoline, jet fuels, or other volatile flammable liquids, or flammable gases, are used, but shall not include such locations when used exclusively for aircraft which have never contained such liquids or gases, or which have been drained and properly purged.
- 513-2. Hazardous Areas. Classification under Article 500.
- (a) Any pit or depression below the level of the hangar floor shall be considered to be a Class I. Division I location which shall extend up to said floor level.
- (b) The entire area of the hangar including any adjacent and communicating areas not suitably cut off from the hangar shall be considered to be a Class I. Division 2 location up to a level 18 inches above the floor.
- (c) The area within 5 feet horizontally from aircraft power plants, aircraft fuel tanks or aircraft structures containing fuel shall be considered to be a Class 1. Division 2 hazardous location which shall ext. id upward from the floor to a level 5 feet above the upper surface of wings and of engine enclosures.
- (d) Adjacent areas in which hazardous vapors are not likely to be released such as stock rooms, electrical control rooms, and other similar locations, should not be classed as hazardous when adequately ventilated and when effectively cut off from the hangar itself by walls or partitions.
- 513-3. Wiring and Equipment in Hazardous Areas. All fixed and portable wiring and equipment which is or may be installed or operated within any of the hazardous locations defined in Section 513-2 shall conform to applicable provisions of Article 501. All wiring installed in or under the hangar floor shall conform to the requirements for Class I, Division 1. When such wiring is located in vaults, pits, or ducts, adequate drainage shall be provided, and the wiring shall not be placed within the same compartment with any other service except piped compressed air.

Attachment plugs and receptacles in hazardous locations shall be explosion-proof or shall be so designed that they cannot be energized while the connections are being made or broken.

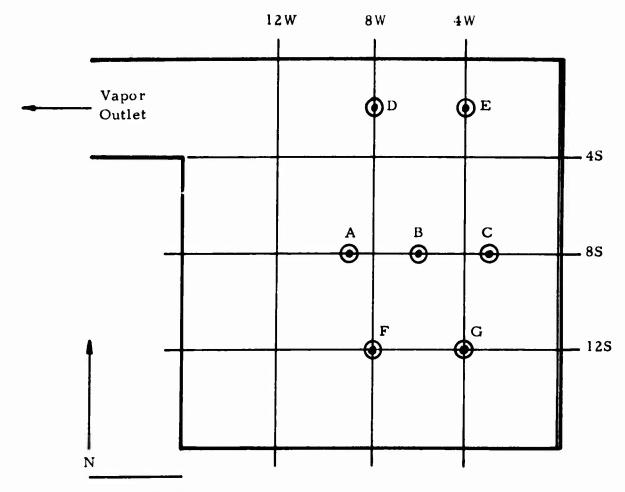
APPENDIX II

SAMPLING CONFIGURATIONS



- 1. Sample points numbered upward from the floor 4, 8, 12, 16 in. levels.
- 2. For Test No. 4A, pan was upended to direct contents toward east wall.
- 3. For Test No. 4B, blowers were turned on. Average velocities shown refer only to this test.

FIGURE II-1. SAMPLE CONFIGURATION NO. 1 FOR TESTS 1 THROUGH 5



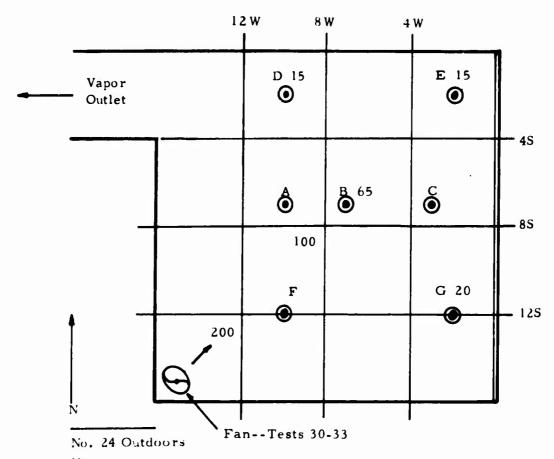
No. 24 Outdoors

Note:

Grid lines are at 4-ft intervals.

Point No.	Location	Elevation, in.	Point No.	Location	Elevation, in.
Ì	С	96	13	E	2
7.	Α	96	14	D	2.
3	В	96	15	C	2
4	В	48	16	F	2
5	E	48	17	G	2
6	D	48	18	G	12
7	D	18	19	F	12
8	E	18	20	F	18
9	В	18	21	G	18
10	В	12	22	G	48
11	E	12	23	F	48
12	D	12	24	Outdoors	

FIGURE II-2. SAMPLE CONFIGURATION NO. 2 FOR TESTS 6 THROUGH 11

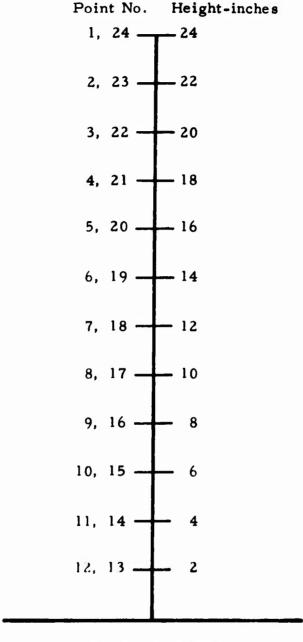


Note:

- 1. Sample configuration No. 3 differs from No. 2 only in wider spacing between D-E and F-G.
- 2. Grid lines are at 4-ft intervals. Numbers are air velocities in ft/min with fan at 13W, 13S operating during parts of tests 30-33.

Point No.	Location	Elevation, in.	Point No.	Location	Elevation, in.
1	С	96	13	E	2
2	Α	96	14	D	2
3	В	96	15	В	2
4	В	48	16	F	2
5	E	48	17	G	2
6	D	48	18	G	12
7	D	18	19	F	12
8	E	18	20	F	18
9	В	18	21	G	18
10	В	12	22	G	48
11	E	12	23	F	48
12	D	12	24	Outside	

FIGURE II-3. SAMPLE CONFIGURATION NO. 3 FOR TESTS 12 THROUGH 22

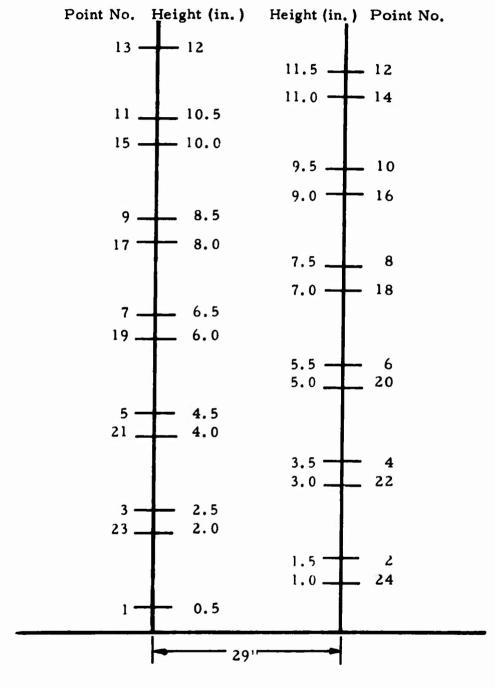


Tests 23 and 29

Note:

All sampling at center of room (7W, 7S). For tests 23 and 29, sample points are alternated 90° apart to reduce effect of sample air currents on vapor layer buildup.

FIGURE II.4. VERTICAL PROFILE-SAMPLE-CONFIGURATION
NO. 4 FOR TEST NOS. 23 & 29



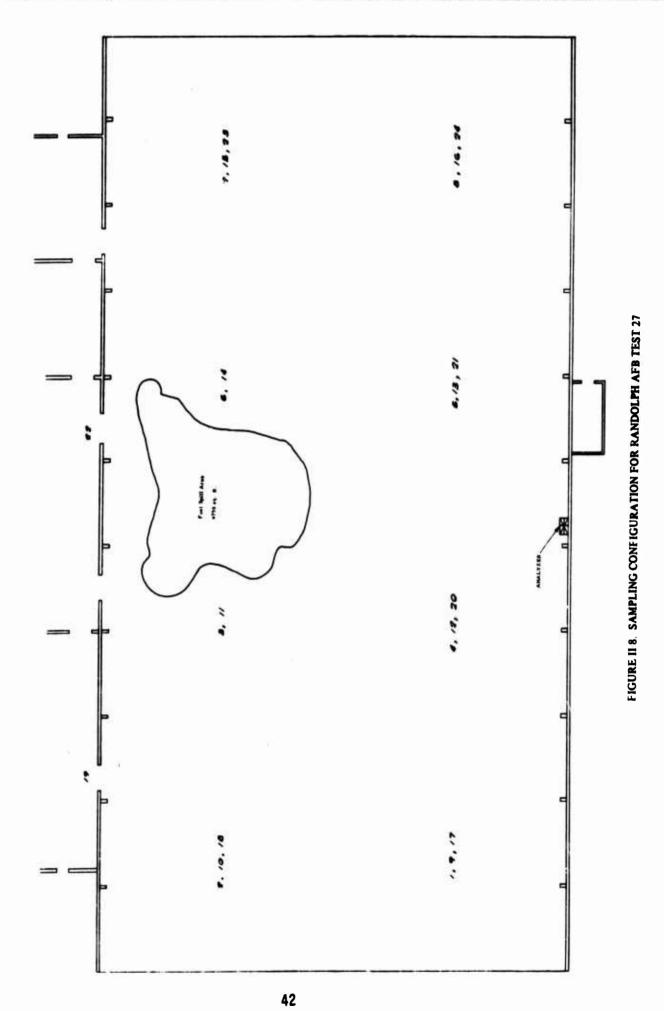
Note:

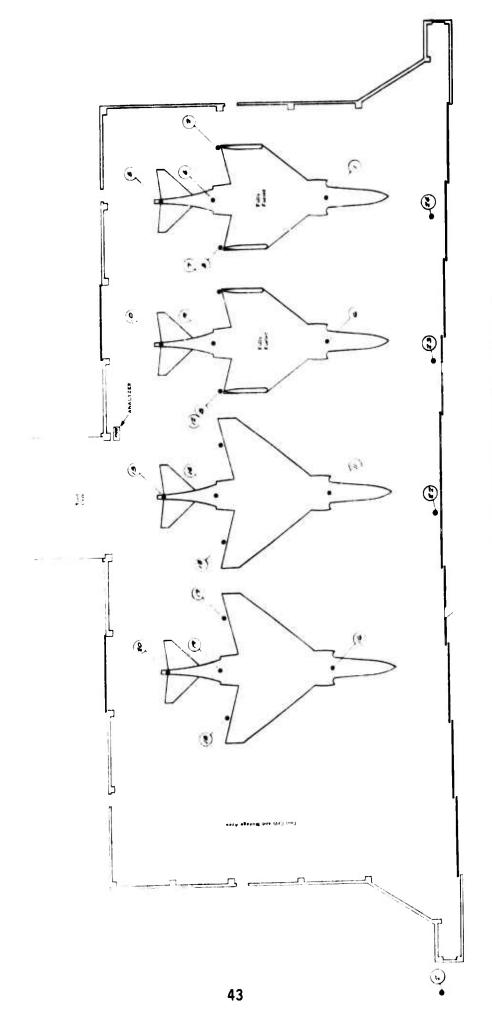
Consecutive sampling points are separated 29 inches horizontally to minimize effects on vapor environment.

FIGURE II-5. VERTICAL PROFILE SAMPLINGS CONFIGURATION NO. 5 FOR TESTS NOS. 34-37

FIGURE 11-6. SAMPLING CONFIGURATION FOR KELLY AFB TESTS 24 AND 25

FIGURE II-7 SAMPLING CONFIGURATION FOR RANDOLPH AFB TEST 26





APPENDIX III

PLOTS OF THE TEST INFORMATION

ILLUSTRATIONS

Figure	Run	Fuel	Temp, °F	Condition
III-1	1	Avgas	71	1 gal in 6-sq ft pan
111-2	2	JP-4	73	l gal in 6-sq ft pan
111-3	3	Avgas	62	2 gal in 5-sq ft pan
III-4A	4A	Avgas	64	Fuel from Test 3 spilled on floor
III-4B	4B	Avgas	63	Continue 4A-floor fan started
111-5	5	ЈР-4	66	2 gal in 5-sq ft pan w/fan
III-6	6	Avgas	71	2 gal in 5-sq ft pan
111-7	7	ЛР-4	75	2 gal in 5-sq ft pan
8-111	8	Avgas	72	2 gal dripped from 5 ft
111.9	9	· JP-4	54	2 gal dripped from 5 ft
111-10	10	JP-4	71	4 gal dripped from 5 ft
III-11	11	Avgas	79	4 gal dripped from 5 ft
111-12	12	Avgas	52	4 gal spilled on floor
111-13	13	Avgas	98	4 gal spilled on floor
III-14	14	JP-4	97	4 gal spilled on floor
111-15	15	Avgas	52	4 gal spilled on floor
III-16	16	Avgas	60	10 gal spilled on floor
III-17	17	JP-4	50	4 gal spilled on floor
111-18	18	JP-4	64	10 gal spilled on floor
111-19	19	Avgas	67	4 gal spilled on floor
111-20	20	JP-4	67	4 gal spilled on floor
111-21	21	JP-4	65	4 gal spilled on floor
111-22	22	JP-4	77	4 gal spilled on floor
111-23	23	JP-4	62	4 gal spilled on floor
				(vertical profile run)
111-24	29	Avgas	69	4 gal spilled on floor
		-		(vertical profile)
111-25	30	Avgas	82	4-gal spill, w/fan
111-26	31	JP-4	89	4-gal spill, w/fan
111-27	32	Avgas	90	4-gal drip, w/fan
111-28	33	JP-4	85	4-gal drip, w/fan
				•

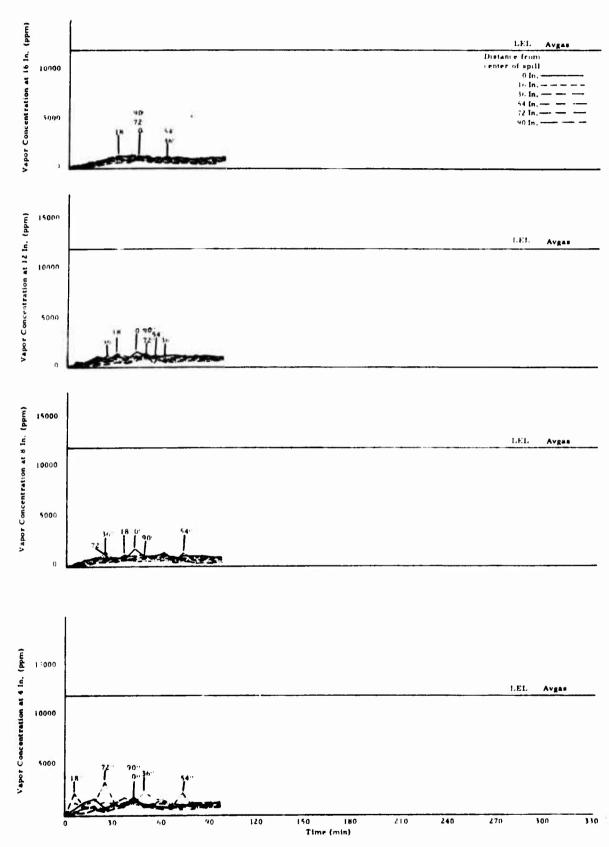


FIGURE III-1. TEST NO. 1-ONE GALLON AVGAS IN A $2' \times 3'$ PAN

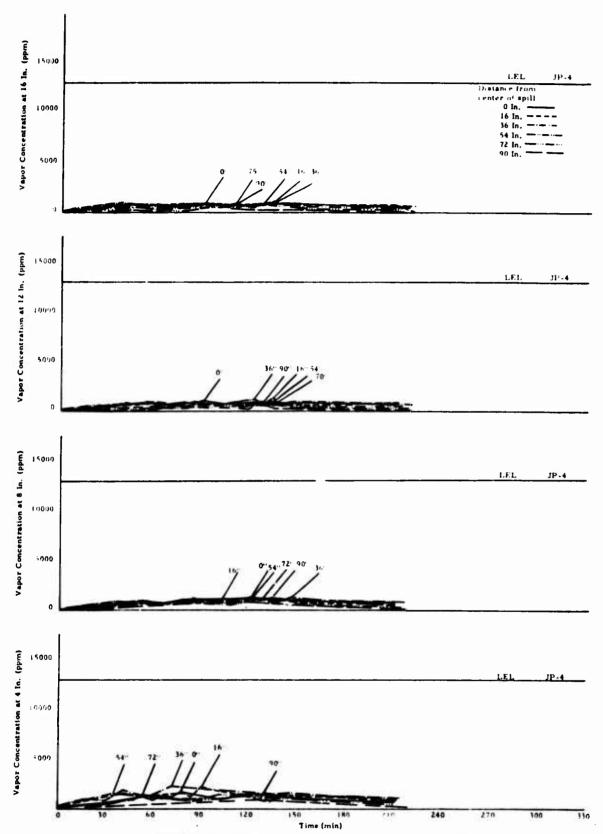


FIGURE III-2. TEST NO. 2 ONE GALLON OF JP-4 IN A 2' x 3' PAN

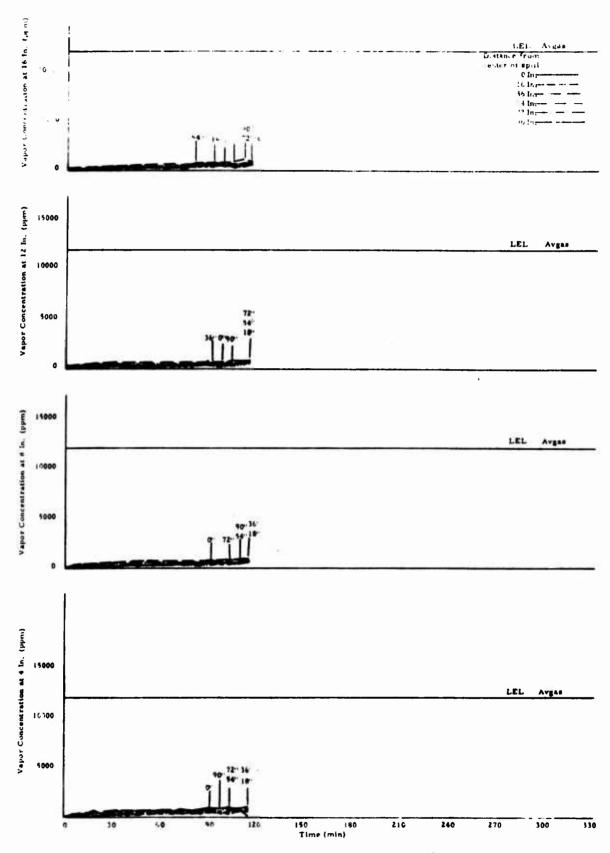


FIGURE III-3. TEST NO. 3-TWO GALLONS AVGAS IN A 2' X 3' PAN

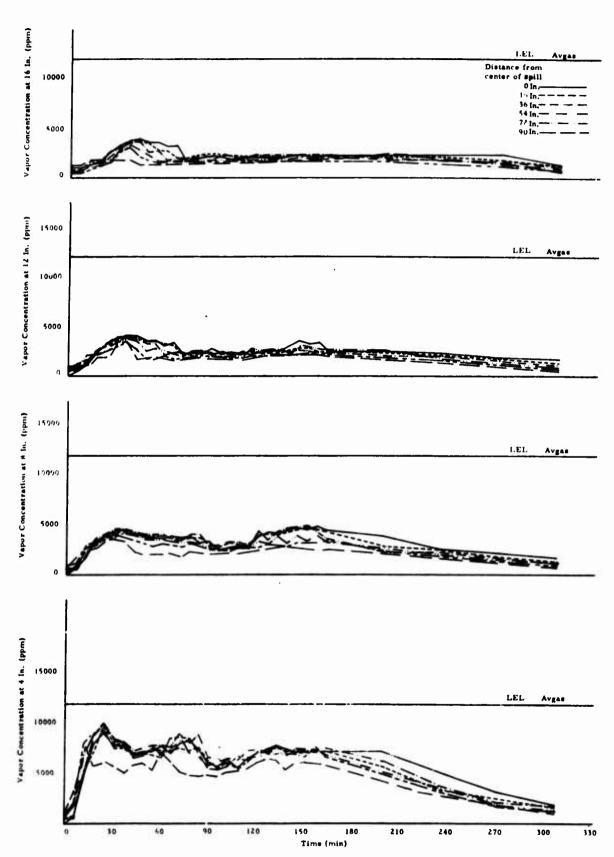


FIGURE 111-4A. TEST NO. 4A-FUEL FROM TEST 3 SPILLED ON THE FLOOR

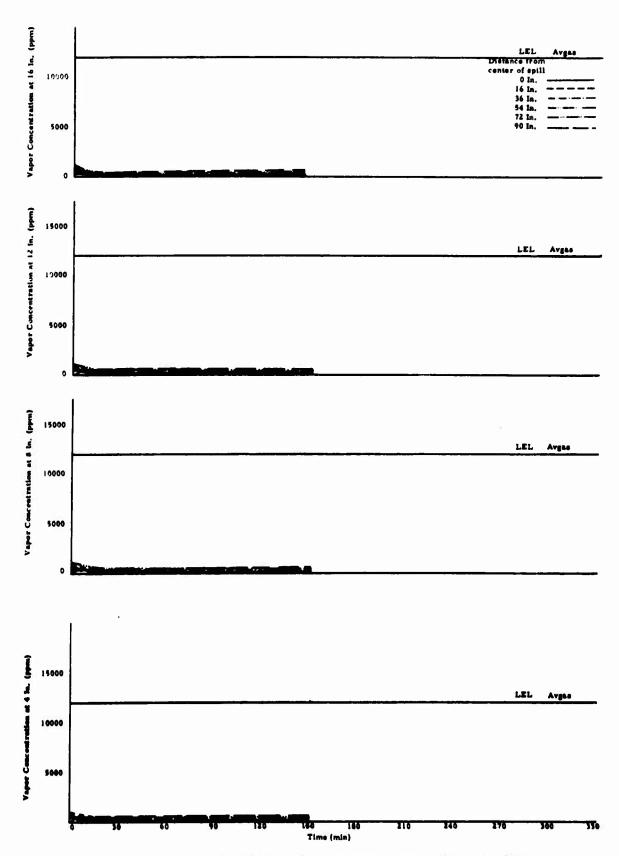


FIGURE III-4B. TEST NO. 4B-TWO GALLONS AVGAS SPILL IN CENTER OF ROOM WITH BLOWERS ON

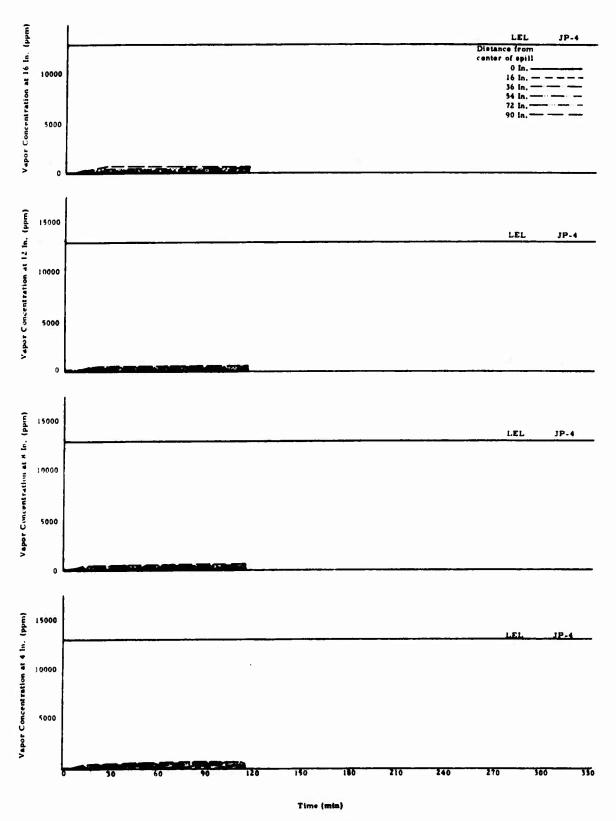


FIGURE III-5. TEST NO. 5-TWO GALLONS JP-4 IN A 2' × 3' PAN

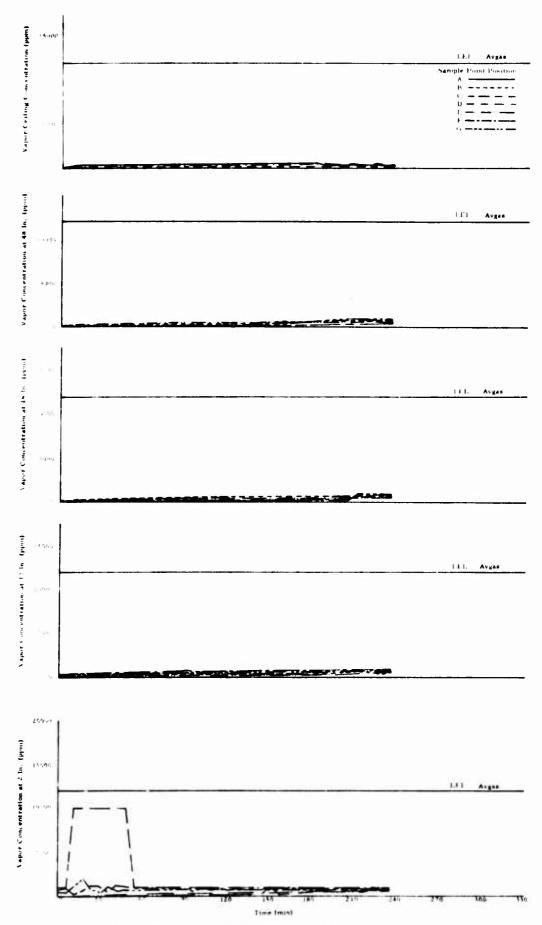


FIGURE III-6. TEST NO. 6 TWO GALLONS OF AVGAS IN A 24" × 30" × 2" PAN

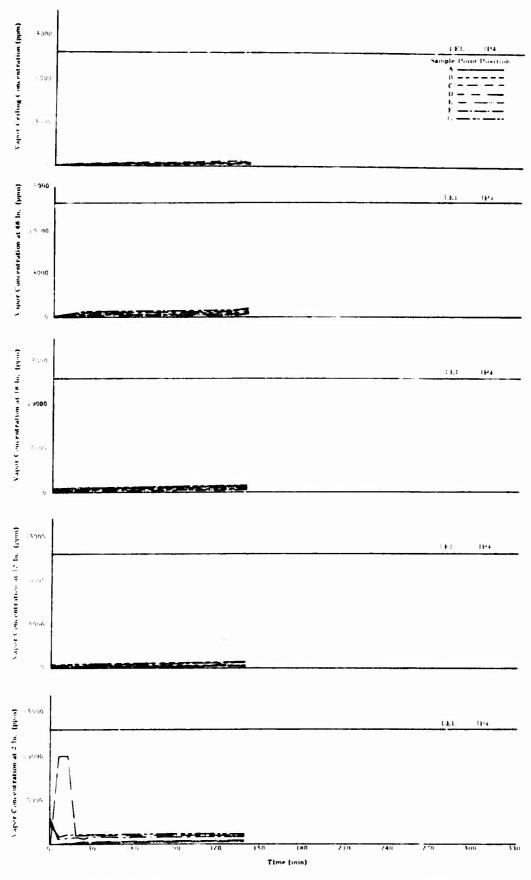


FIGURE III-7. TEST NO. 7. TWO GALLONS OF JP-4 IN A 24" x 30" x 2" PAN

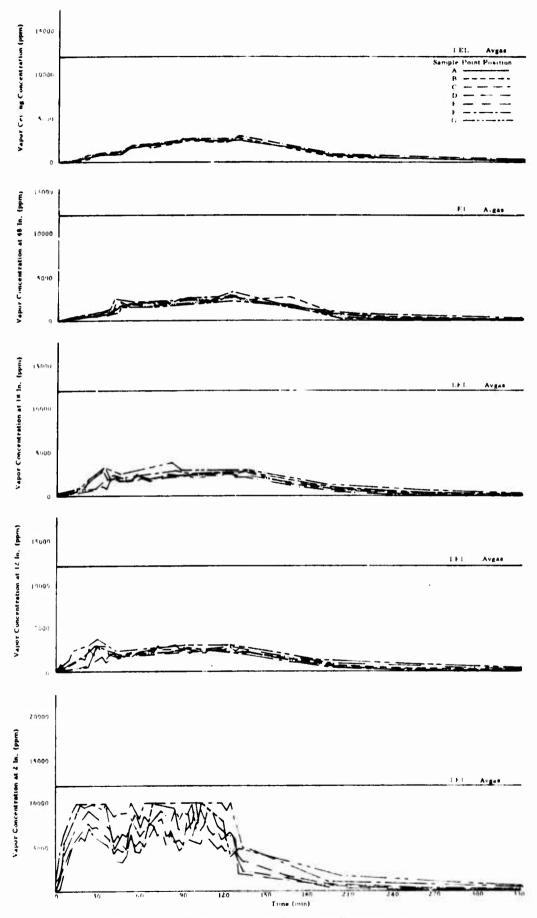


FIGURE III-8. TEST NO. 8-TWO GALLONS OF AVGAS IN DRIP TEST

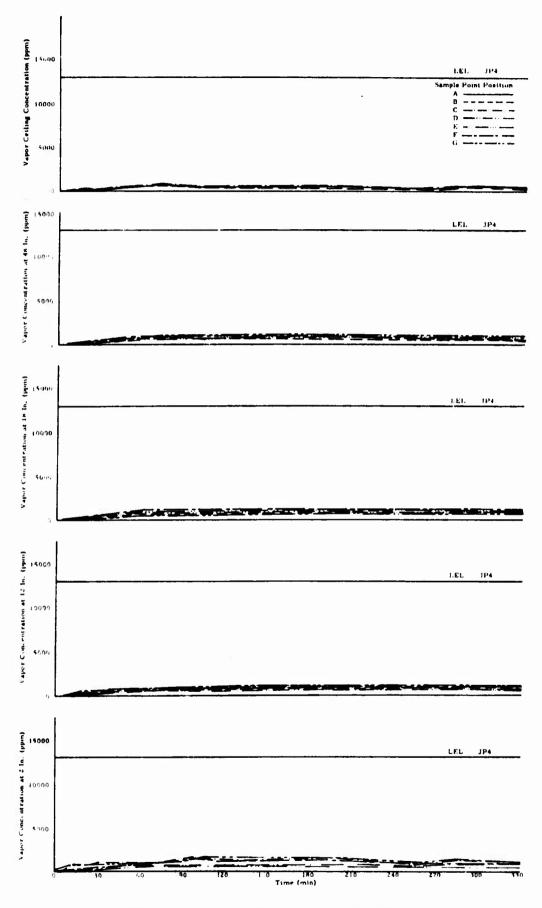


FIGURE III-9. TEST NO. 9-TWO GALLONS OF JP-4 IN DRIP TEST

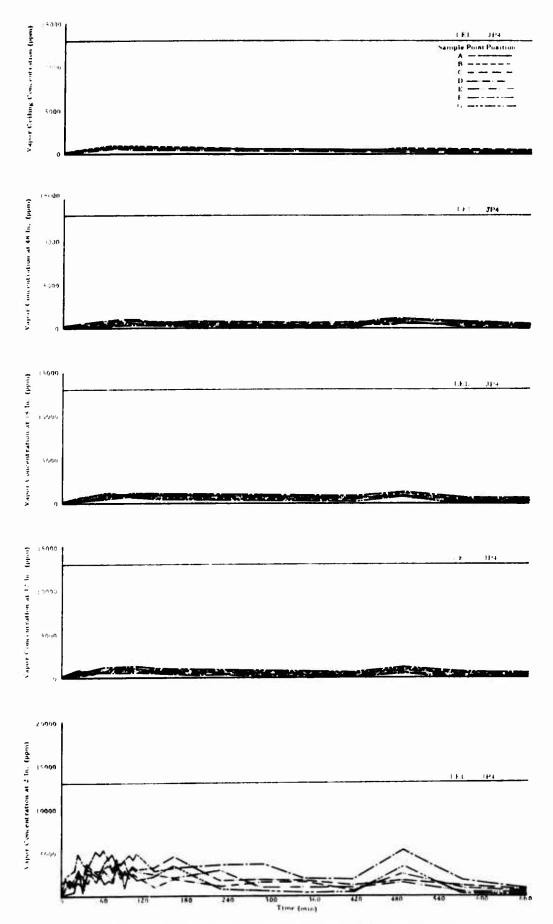


FIGURE 111-10. TEST NO. 10-FOUR GALLONS OF JP-4 IN DRIP TEST

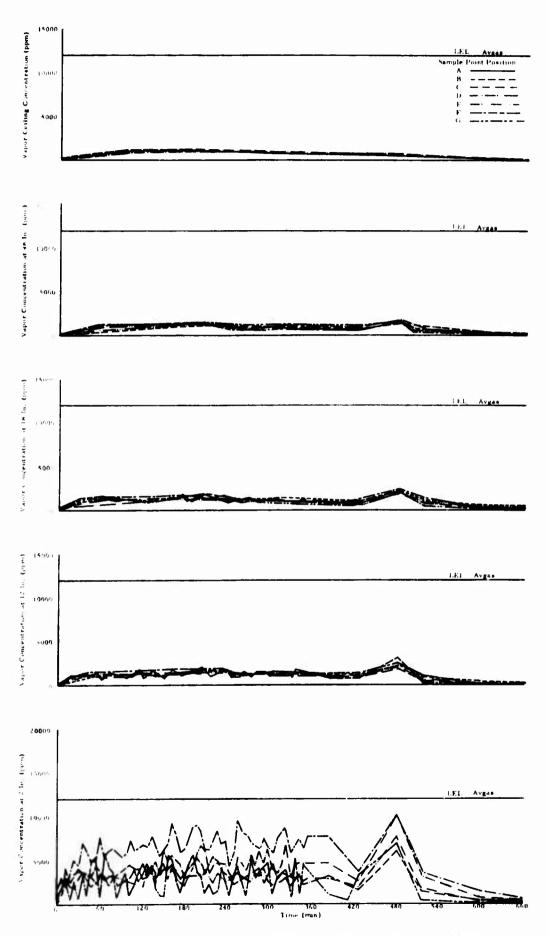


FIGURE III-11. TEST NO. 11-FOUR GALLONS OF AVGAS IN DRIP TEST

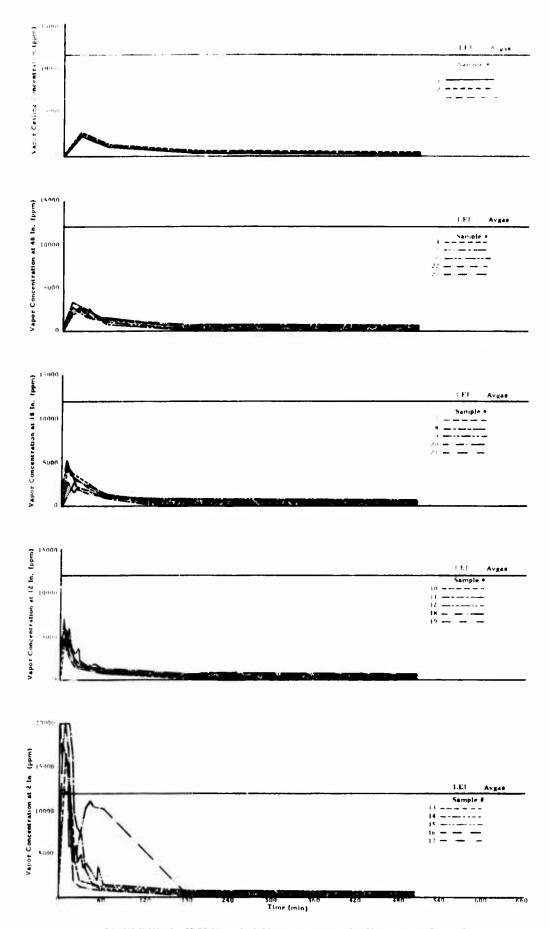


FIGURE 111-12. TEST NO. 12 FOUR GALLONS OF AVGAS IN A SPILL TEST

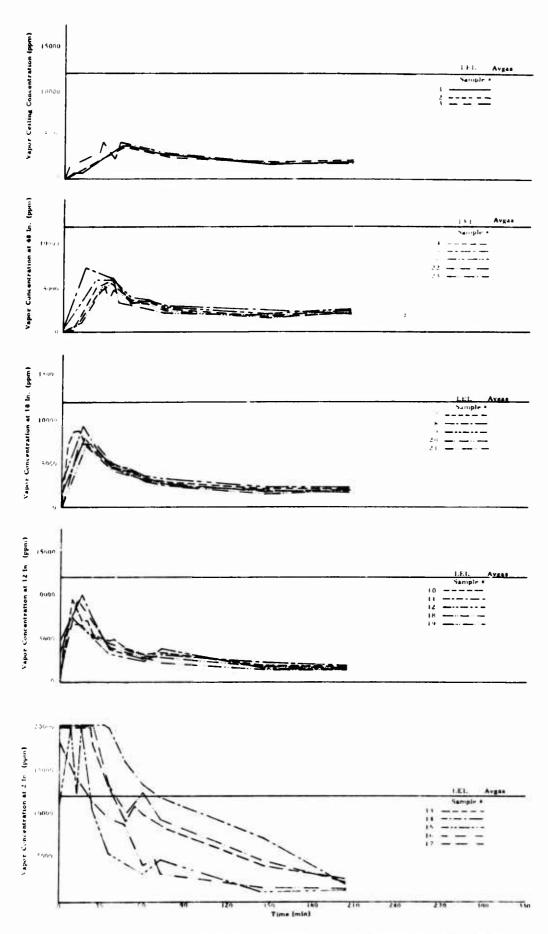
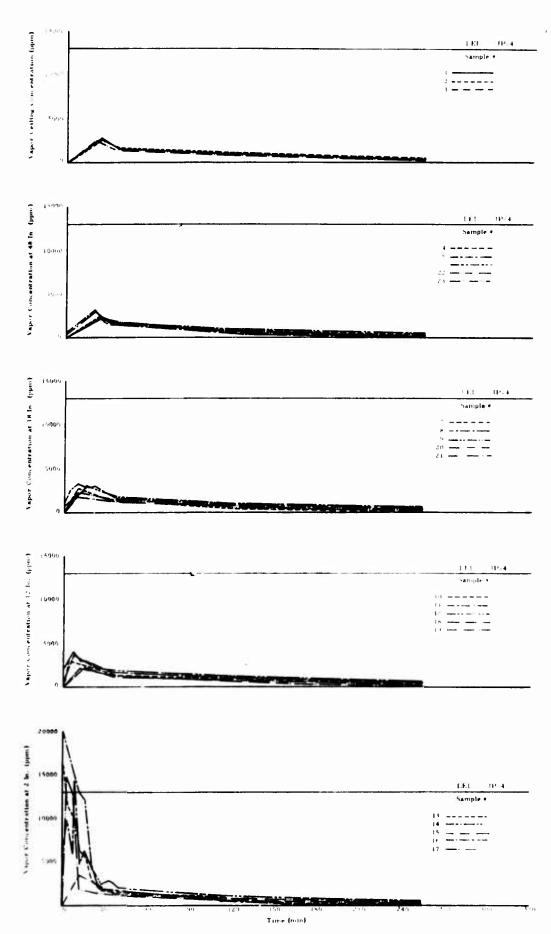


FIGURE III-13. TEST NO. 13 FOUR GALLONS OF AVGAS IN A SPILL TEST



THE STATE OF THE PARTY OF THE P

FIGURE III-14. TEST NO. 14-FOUR GALLONS OF JP-4 IN A SPILL TEST

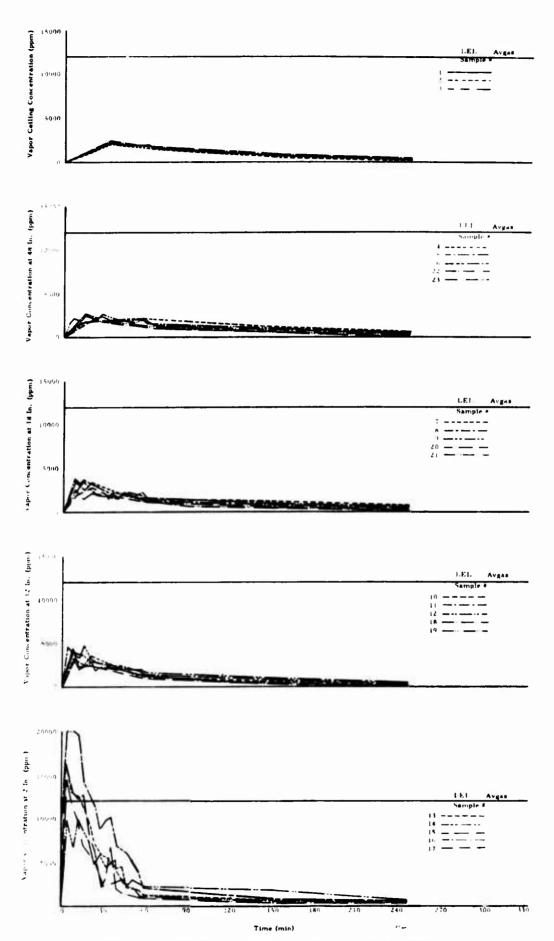


FIGURE III-15. TEST NO. 15-FOUR GALLONS OF AVGAS IN A SPILL TEST

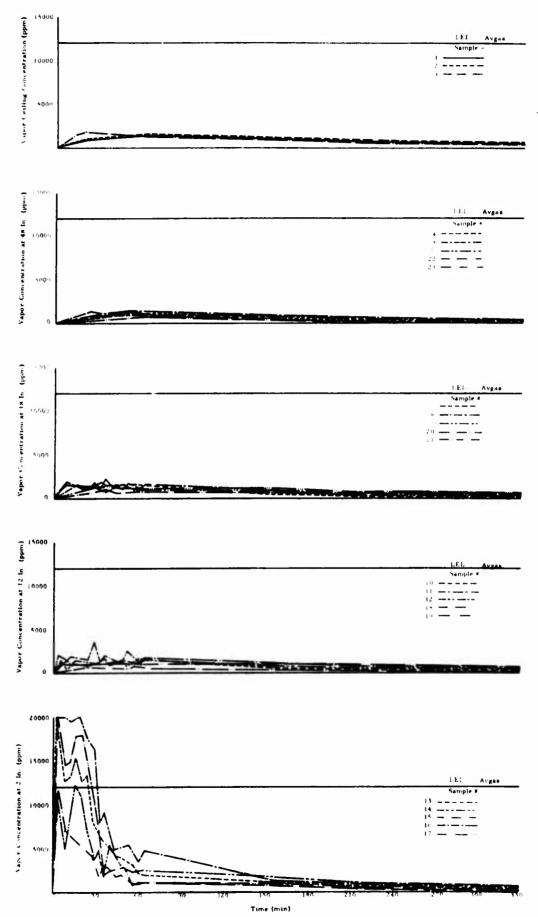


FIGURE III-16. TEST NO. 16-TEN GALLONS OF AVGAS IN A SPILL TEST

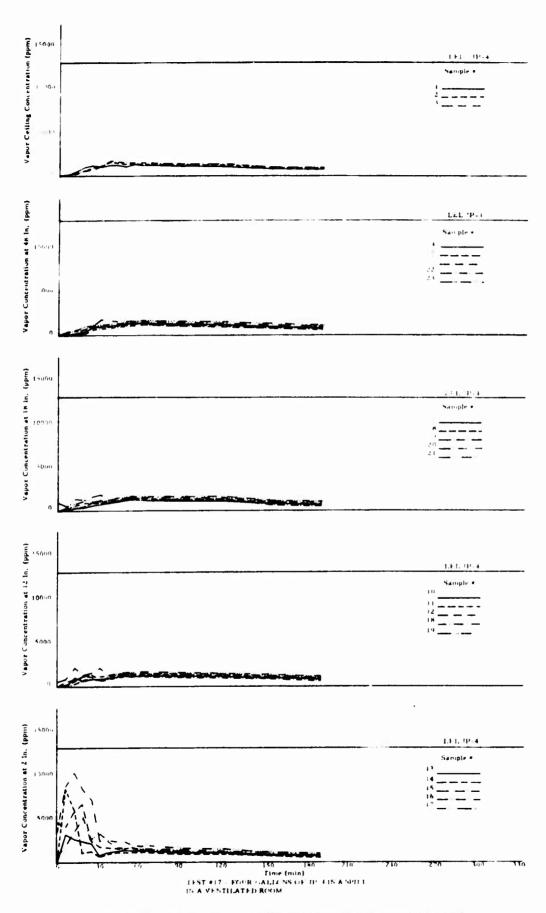


FIGURE III-17. TEST NO. 17--FOUR GALLONS OF JP-4 IN A SPILL TEST

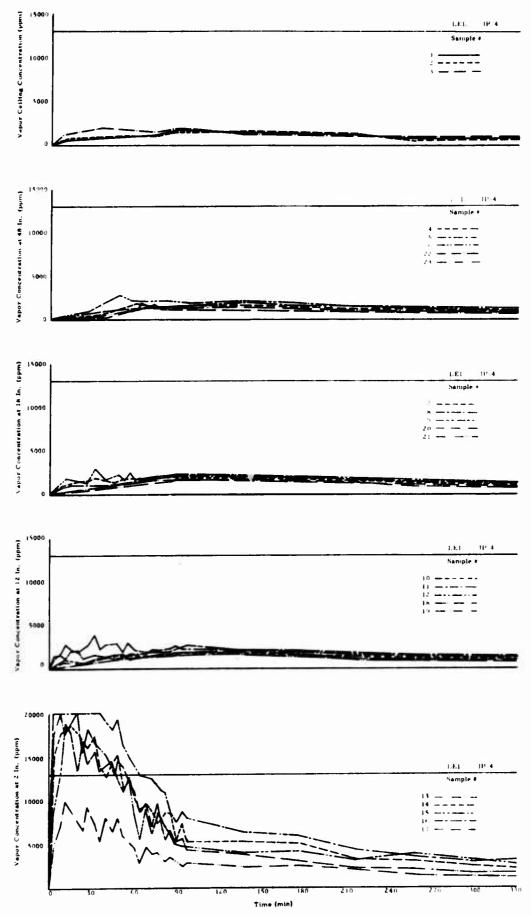


FIGURE III-18. TEST NO. 18-TEN GALLONS OF JP-4 IN A SPILL TEST

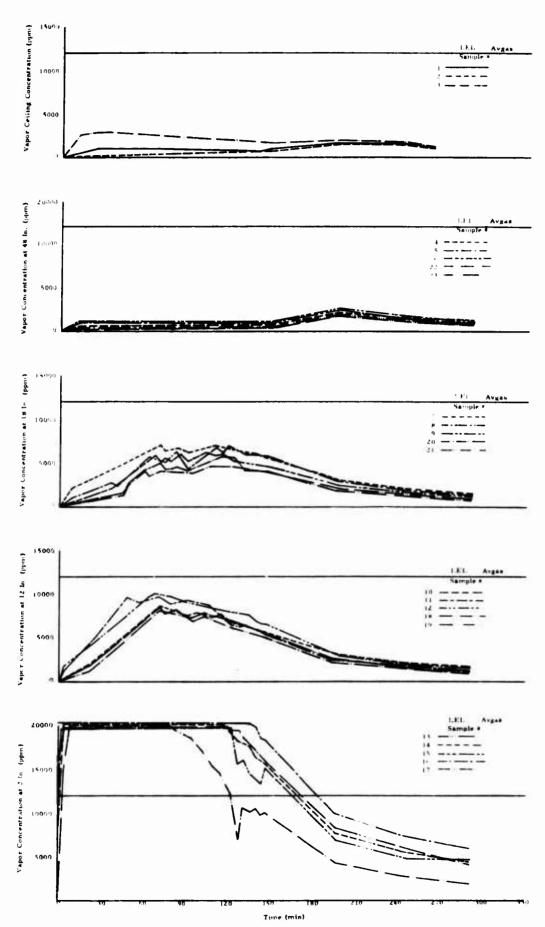


FIGURE III-19. TEST NO. 19-FOUR GALLONS OF AVGAS IN A SPILL TEST

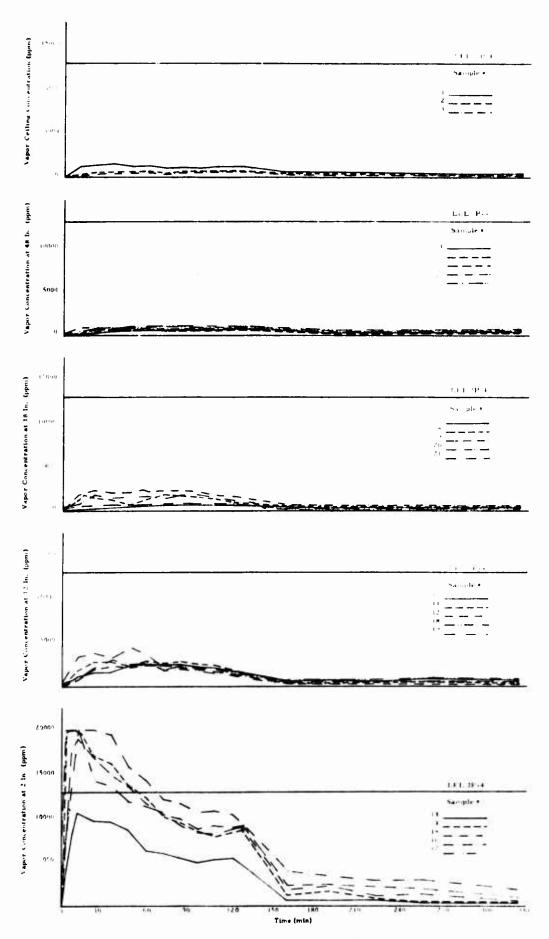


FIGURE III-20. TEST NO. 20 - FOUR GALLONS OF JP-4 IN A SPILL TEST

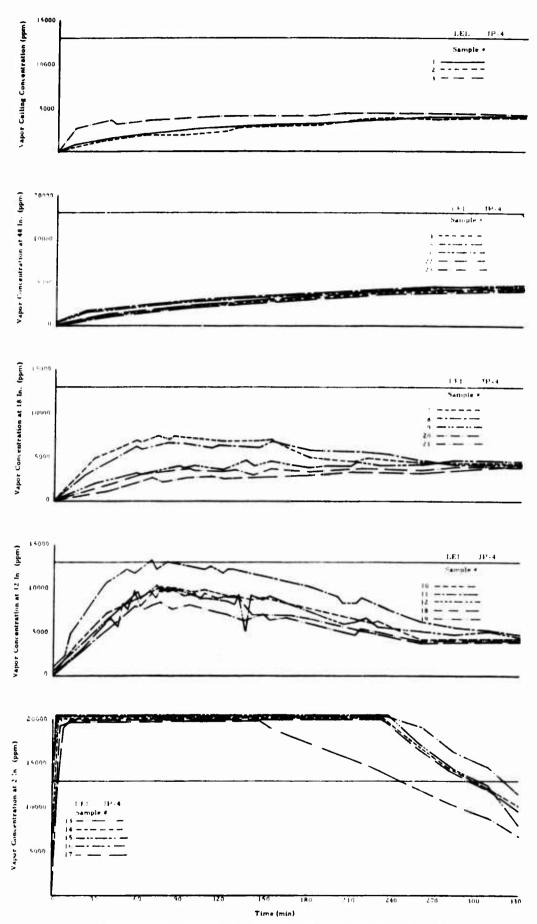


FIGURE 111-21. TEST NO. 2: -FOUR GALLONS OF JP-4 IN A SPILL TEST

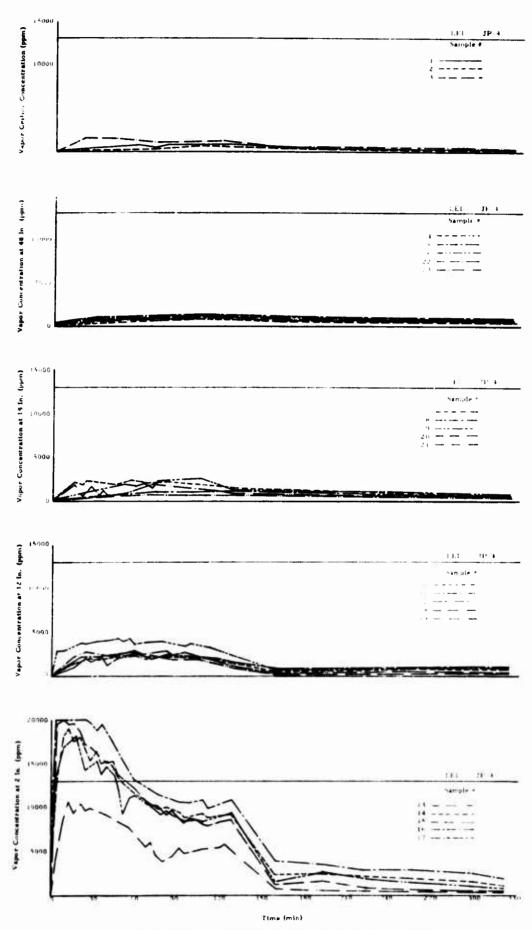


FIGURE III-22. TEST NO. 22 -FOUR GALLONS OF JP-4 IN A SPILL TEST

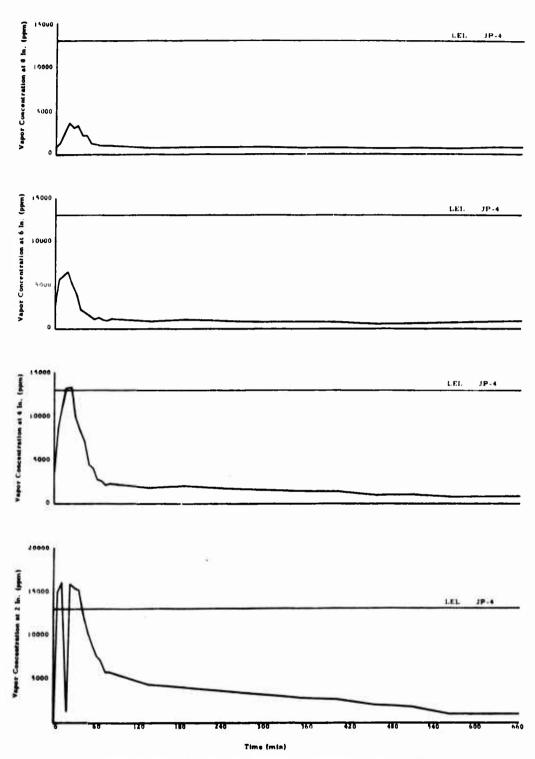


FIGURE III-23. TEST NO. 23 - FOUR GALLONS OF JP-4 IN A SPILL TEST

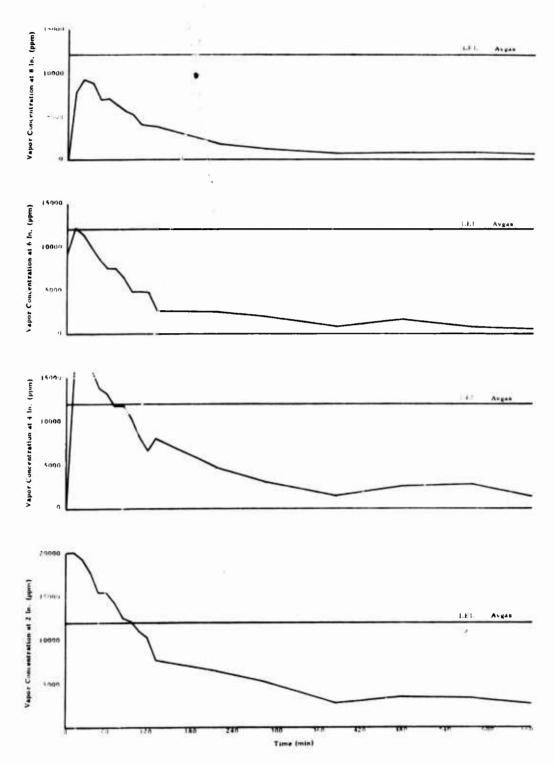


FIGURE III-24. TEST NO. 29-FOUR GALLONS OF AVGAS IN A SPILL TEST

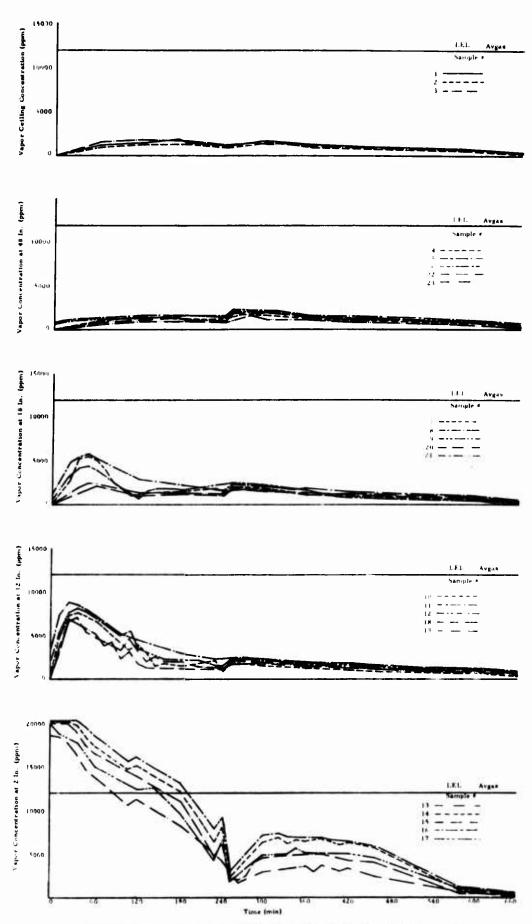


FIGURE III-25. TEST NO. 30-FOUR GALLONS OF AVGAS IN A SPILL TEST

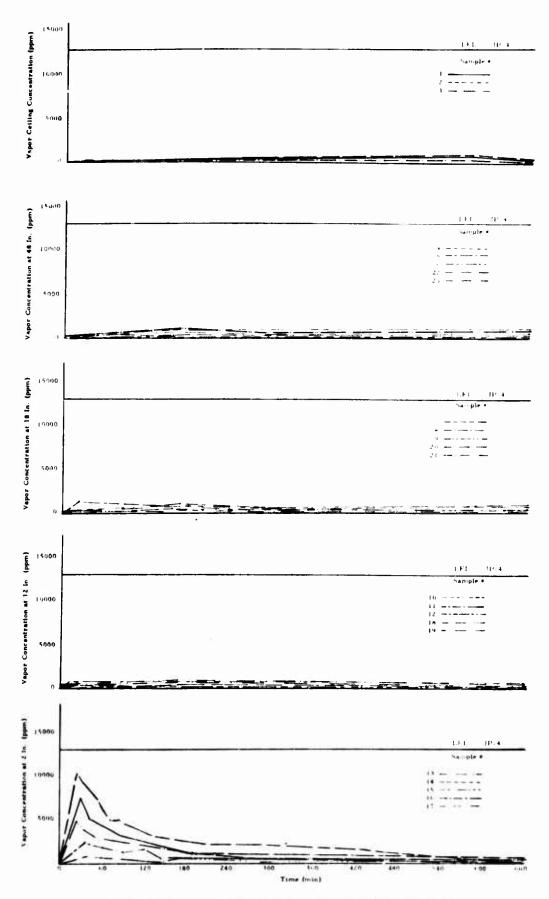


FIGURE III-26. TEST NO. 31 - FOUR GALLONS OF JP-4 IN A SPILL TEST

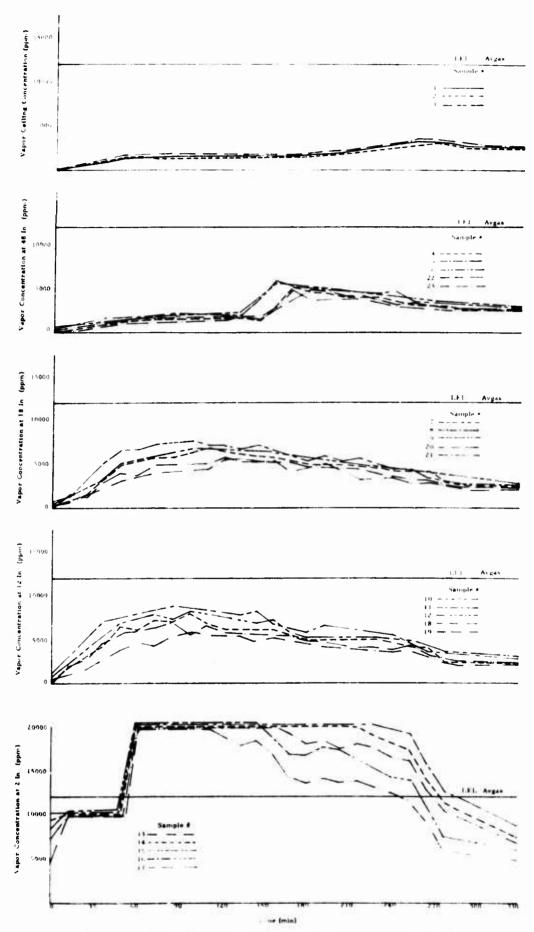


FIGURE 111-27. TEST NO. 32-FOCK GALLONS OF AVGAS IN A DRIP TEST

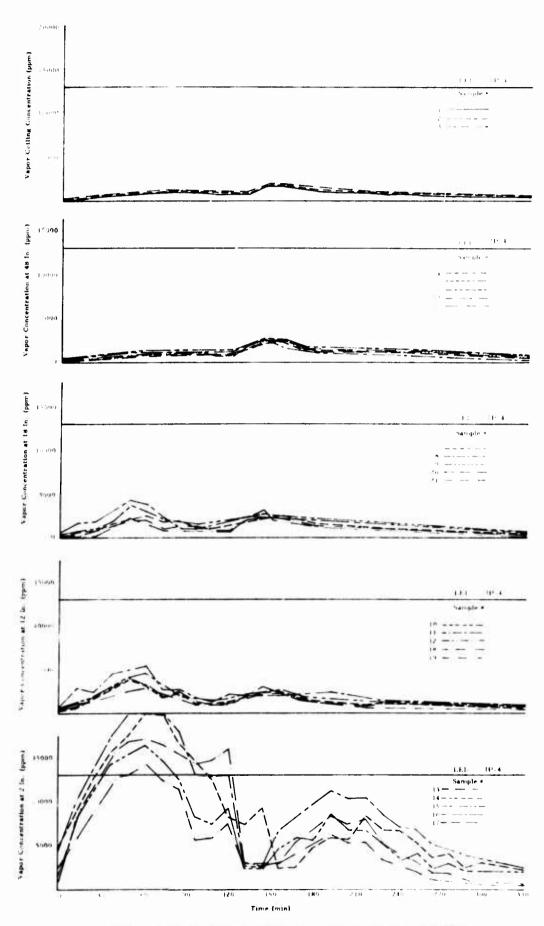


FIGURE HI-28. TEST NO. 33 FOUR GALLONS OF JP-4 IN A DRIP TEST

APPENDIX IV

TABLES OF TEST RESULTS

TABLES

Lable	Run	Fuel	Temp, °F	Condition
IV-1	1	Avgas	71	I gal in 6-sq ft pan
1V-2	2	JP-4	7.3	I gal in 6-sq ft pan
1V-3	3	Avgas	62	2 gal in 5-sq ft pan
IV-4A	4A	Avgas	64	Fuel from Test 3 spilled on floor
IV-4B	4B	Avgas	63	Continue 4A-floor fan started
IV-5	5	JP-4	66	2 gal in 5-sq ft pan w/fan
IV-6	6	Avgas	71	2 gal in 5-sq ft pan
IV-7	7	JP-4	75	2 gal in 5-sq ft pan
IV-8	8	Avgas	72	2 gal dripped from 5 ft
IV-0	9	JP-4	54	2 gal dripped from 5 ft
IV-10	10	JP-4	71	4 gal dripped from 5 ft
IV-11	11	Avgas	79	4 gal dripped from 5 ft
IV-12	12	Avgas	52	4 gal spilled on floor
IV-13	13	Avgas	98	4 gal spilled on floor
IV-14	14	JP-4	97	4 gal spilled on floor
IV-15	15	Avgas	52	4 gal spilled on floor
IV-16	16	Avgas	60	10 gal spilled on floor
IV-17	17	JP-4	50	4 gal spilled on floor
IV-18	18	JP-4	64	10 gal spilled on floor
IV-19	19	Avgas	67	4 gal spilled on floor
IV-20	20	JP-4	67	4 gal spilled on floor
IV-21	21	JP-4	65	4 gal spilled on floor
IV-22	22	JP-4	77	4 gal spilled on floor
IV-23	23	JP-4	62	4 gal spilled on floor
				(vertical profile run)
IV-24	24	JP-4	45-66	Hangar 935, Kelly AFB
IV-25	25	JP-4	47-78	Hangar 935, Kelly AFB
IV-26	26	JP-4	45-69	Hangar 5, Randolph AFB
IV-27	27	JP-4	57	55-gal spill, Randolph AFB
IV-28	28	JP-4	46-66	Hangar 4337, Bergstrom AFB
IV-29	29	Avgas	69	4 gal spilled on floor
				(vertical profile)
IV-30	30	Avgas	82	4-gal spill w/fan
IV-31	31	JP-4	89	4-gal spill w/fan
IV-32	32	Avgas	90	4-gal drip w/fan
IV-33	3.3	JP-4	85	4-gal drip w/fan
IV 34	34	Avgas	75	4-gal spill
				(vertical profile)
IV-35	35	JP-4	88	4-gal spill
				(vertical profile)
IV-36	36	Avgas	88	4-gal spill
		-		(vertical profile)
IV-37	37	Avgas	76	4-gal drip
				(vertical profile)

TABLE IV-1. FUEL VAPOR CONCENTRATIONS IN PPM

Test I Conditions: Fuel - avgas. Iemperature - 71°F. R.H. - 25%. Sample Configuration No. 1. One gallon of avgas poured into a 6-sq ft pan in the center of the room. 11/4/71.

	57	0	250	050	550	750	850	950	1100	1750	1100	950	1000	1190	950	1050	1050	
	23	0	250	00	9	550	750	850	850	0511	1000	650	1000	1100	1000	950	005	
	77	0	250	250	909	900	750	800	850	1000	950	000	850	950	900	950	206	
	12	0	250	300	550	650	700	850	900	900	056	800	800	006	006	006	900	000
	50	20	700	350	550	009	0001	1050	1200	1200	150	800	1100	1050	1150	1100	1100	1100
	2	20	200	550	550	750	1100	1050	1100	1200	1000	006	950	1050	1100	1150	006	1100
	2	0	250	750	1050	1100	850	850	850	750	900	850	00€	750	850	006	850	056
	=	0	200	1200	1500	3350	1400	1350	1250	850	1050	850	850	800	850	006	006	056
	9	•	250	850	750	950	850	1 000	1050	1050	1000	1150	1000	850	056	1000	1000	1 000
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	2		150	350	909	1500	850	900	850	000	1050	1400	850	006	000	350	006	950
	0		450	750	950	1450	1200	1250	1400	2250	1850	1350	00ь	800	1300	050	1200	1050
	30		200	100	006	750	1350	0521	0511	1150	1050	1150	1100	1100	950	056	950	1150
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	+		200	550	900	1100	1150	006	1400	1200	1200	0501	1250	1150	1100	1150	1200	1130
	-		200	850	1050	900	1250	900	1600	1250	1150	1200	1250	1100	0001	1200	1150	1100
	~		300	909	900	850	950	35c	1800	1050	1100	1400	006	1150	1050	1100	1000	1000
	-		700	1400	1550	850	1000	850	1900	000	056	050	S U	1050	056	1 200	0.11	1250
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TABLE IV-2 TUEL VAPOR CONCENTRATIONS IN PPM

Test 2 Conditions Final JP 4 Temperature 73°F R H 24% Sample Configuration No 1 One gallon JP-4 poured into a 6-sq ft pan in the center of the room, 11/4/71, Time

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TABLE IV-3 FUEL VAPOR CONCENTRATIONS IN PPM

Test 3 Conditions: Fuel - avgae. Temperature - 62"F. R. H. - 60% Sample Configuration No. 1. Two gallons of vygas poured into a 5-sq ft pan in the center of the room. 11/8/71.

	12	100	001	180	577	285	300	330	345	360	004	4.5	435	540	900	580	054	435	730	75	0
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•	0510	4100	1340	24.00	1700	1.45.0	007	2650	1750	43.00	.101.	2, 40											
96	7850	4450	4400	1140	4490	445.11	0 9 14	=	7 7		í,												•
£	2750	45.00	41.00	0.4.1		1													116 - 2 - 400	7100	3400	14.00	· ·
:	2		00			r		,	7		2	20	0504	1200	1.00	1400	1 11	4 time 14	1459 4160	0.000	0 3450	1.0.4	000
÷	1000	1.50	0.50	9450	505	÷1.0	001	* * *	.01.	057		Pr.00	9540	1.00	1550 2	2 etter 1-	1.100	346.5 27	9612 3542	0075 0	0 2200	le on	3,14
7	2350	3450	.)U4	1 00	7-9-90	11.	54	1,6.21	F-		0.11	54.4		1440	35.50	2 35.00 7	2050	11504	1581 (188)	5 4015	0.5000	1700	14.
;	1350	3753	3650	34.00	2<00	145.3	6628	€ X n,	146.3	000	665	2800	7600	38:0 7	t 00 87	1750	2 056	2450 17	1550	0 81941	0 2140	00-1	1550
0.9	7800	34.50	3150	3200	0012	1250	\$200	2750	96	00.7	0 > 77	00=1	0074	37.30	20502	i MSu c	1 0523	17 001	211. 1750	0 5150	0 1 1 0		170
6	1.0	3400	3400	0571	1150	1860	1150	22.50	ě.	01.14	2450	22.30	7000	14.30	1950	00. *	8550	\$ 150	00#1 5#1	00	0017 0		1000
£,	6040	3750	2450	0521	00:	M AN	0,07	503	- +	00.4	•	0	3400	3.400	1 0567	×	7 90 K	#1 05m7	1450	0.415 0			1700
t-	8400	3800	2450	0561	7400	3400	23.30	5.100	00	00€	0522	2040	0545	1350	2 5 00 2	2460 7	1 00002	\$200 Zu	2000 1 455	0074 4	0 2300	1400	24
3	7500	3250	2200	2050	2450	3700	2600	2400	1300	0.00	0057	2300	5700	1.50	7550 2	2000	100	1300 21	2150 1+50	0 \$0\$0	0 202 0		1 400
?	£200	3400	2700	0577	6.2 30	3100	7150	2500	0012	3150	2200	\$000	5,000	2700 2	7 0577	9 0517	6050 2	25.50 22	22.10 2050	0 4490	2001		10.
ę	5750	0557	230€	2100	2050	2750	0517	2200	(1551)	3.40	3 1 7	2250	6.050.5	7.0027	0577	6 0077	2.0024	72 0557	2100 2000	0 4700	0517 0	1.540	3
102	0044	2700	2350	1450	6250	3200	2350	2300	0504	1200	2240	2150	4.200	65.7	2250 2	2 000 5	5450 2	2400 21	2100 2000	0 \$100	0 2250	0507	0541
101	00 as	2400	2250	9012	2500	1000	2300	2200	6.14.0	1240	91.	00	1063	0527	2250 2	2100 6	5 00 H2	2800 21	2150 1959	0 5250	0 2200	2100	006.1
• -	1550	0562	,200	2000	6300	3200	2500	2300	7390	ć	07+4	2.00	051	0557	2.0072	215	1 (51.	1700 75	0517 0527	1 \$500	0 2550	2500	2100
120	100	3800	2450	2200	7200	4000	0087	2100	7450	0544	0.47	2150	2150	3400	2409 2	2296 +	.703 2	22 0527	2200 2000	0 4100	2400	2150	2660
623	7550	4350	2650	2 1 00		0514	2450	\$200	2100	3540	2450	2.100	2500	3350	2 0545	2200	180 1	1150 23	230 2050	0 6500	0057 0	2430	2100
132	1700	001+	2500	2150	7h.00	901+	0582	0512	76.00	1300	1. 4.	2350	2.00	3.40	2550 2	2300 7	7150 2	2800 23	2305 2150	0 6300	3000	2590	2100
135	1500	4 5 00	3100	0577	7450	4450	5650	2200	7300	4750	3547	2250	0.469	3200 2	7 0547	7 0017	7000 2	+7 WORT	2456 2200	0 5450	3000	2400	2150
<u> </u>	7250	4150	3500	2400	7250	4550	0097	0577	05+2	00.	3660	2230	1250	3,400	25.50 2	2300 7	7200	1150 23	2360 2150	0 6:00	0 2500	2500	2000
150	7300	4550	3250	7100	7100	4650	2700	22.00	7150	-0-+	5.2	22.00	7000	3400	2500 2	7300	1 05.4	1200 23	2300 2100	0 6200	0 2450	2400	110
15.	7250	4850	3350	2200	0014	4550	2450	2200	7300	001+	2500	2300	73.30	3450 2	2 0052	2300 7	76.00 3	3200 23	2300 2100	0 6150	0 2530	2350	0517
162	350	4500	2550	2350	73.0	00++	2550	2400	7400	3750	0 5 5 7	2350	0084	3250	2 0057	2300 .	\$ 00K4	£7 03 %	0017 0387	0005 0	0 2500	2450	2150
1 98	2350	3900	2550	2 100	0585	2950	2400	2300	4	2243	3000	2350	5250	2 00 2	2350 2	\$ 0522	2 0035	2500 23	234 . 2250	4200	0 2709	2350	2250
234	2500	2650	0047	2250	3500	2500	2200	2200	3800	2353	2050	0512	3750	2360 2	2200 2	2200	1100 2	2150 20	2000 1800	0 2500	0 2050	2000	2
0_2	3050	2250	1950	2300	2450	1800	2000	1750	2050	1750	0.55	04 41	056	1750	1500	1500 3	2300 1	1800 17	1700 1650	0 1650	0 1650	1650	16.00
33e	1950	1700	1750	1350	1500	1350	1400	1330	1550	** **	1 \$ 90	0 \$ 7 1	1400	1250	1300	1 300	1450	1250 12	J641 US71	1400	0 1350	1450	1400
The tur	T.e show	The time shown corresponds	epuodea		to Sample Point No	~ %	Each	* mple	point beyond		No 1 to	Paced:	15 sec ((e. ff S	Sample P	Point No. 2 to		30 060	Triple Point	int No. 20	20 18 300	0 844 01	S min)

TABLE IV 46 FUEL VAPOR CONCENTRATIONS IN PPM

Test 4B Conditions: Fuel - avgas. Temperature - 53 F. R.H. - 73%. Sample Configuration No. 1. Fans were turned on at the end of Test 4A in which two gallons of avgas that had weathered in Test 3 were dumped onto the floor. 11/8/71.

	54	584	306	0 K	501	90	-10	7.0	0	2	ů	Ç	
	23	\$45	315	185	115	90	7.5	70	59	00	55	9	
	2	24.0	320	180	105	7.	70	70	70	20	50	0	
	2	588	295	0	115	85	7.5	70	7.0	3.5	59	0	
	07	635	355	215	130	*	80	10	10	9	99	0	
	0	680	36.0	210	135	06	20	70	70	09	59	0	
	=	069	370	220	140	95	70	75	80	9	59	45	
	=	099	380	230	145	100	80	80	75	65	9	\$	
	9	100	410	230	5+;	96	90	80	70	70	99	40	
	5	100	415	240	150	95	90	88	7.0	70	70	45	
	-	700	\$ \$	255	160	105	80	85	70	70	20	50	
Sample Point Numbers	=	750	425	502	175	110	95	6	88	0.80	\$9	55	
ole Pour	21	R00	435	597	165	110	ş	75	80	59	09	9	
25	=	800	405	275	170	110	105	88	80	25	70	50	
·	0-	850	445	275	175	130	90	95	80	70	09	90	
	0	850	485	567	195	130	105	90	88	80	70	09	
	80	006	475	300	170	110	06	80	88	70	09	20	
	-	056	064	305	185	110	06	88	80	20	09	20	
	اه	950	200	502	581	120	06	88	80	70	09	50	
	.	400	510	320	200	135	45	6	100	80	70	09	
	4	920	950	305	185	120	45	80	80	70	59	55	
	~		850	305	180	150	00	80	80	ት የ	70	55	45
	~		545	310	185	120	96	80	75	7.5	99	55	50
	-		535	310	200 185 180 185 200 185	130	100	90	88	0	75	0.9	20
				2		7.7	30	30	7	¥	ę	* + -	150

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min)

TABLE IV-5 FUEL VAPOR CONCENTRATIONS IN PPM

Test 5 Conditions: Fuel - JP-6. Temperature - 66°F R H - 76% Sample Configuration No. 1. Two gallons of JP-4 in 5-sq ft pan in the center of the room; the fuel was not dumped onto the floor, but the blowers were turned on.

Time	1										Sample	Sample Point Number	Number											
min	-	7	-	+	اء	اء	-	TC	0	01	=	17	<u></u>	₹	5	91	17	=	61	62	717	22	2	77
0	•	•	0	•	0	0	•	0	0	0	0	0	0	0	0	0	0	0	0	0	0	٥	0	0
•	•	•	9	10	ď	~	٧	10	01	ď	ď	0	0	c	С	0	0	0	0	0	0	0	0	0
12	110	200	90	355	30	30	35	59	0+	35	30	0	45	90	09	\$0	70	45	30	30	20	\$0	50	50
81	105	0	\$	\$\$	90	35	45	0+	52	0.	0+	0+	5.5	50	35	35	65	4.5	3.5	5.5	0,	04	20	20
\$ 2	130	100	09	09	70	09	45	0,2	90	45	59	5.5	20	09	45	09	30 7.	09	\$	45	95	0.8	75	85
30	760	120	95	70	. 55	75	59	75	06	9.5	09	100	95	70	59	55	06	70	90	70	06	001	9.5	001
36	592	2	75	2	96	66	75	80	20	80	06	001	110	105	501	70	110	105	70	09	011	100	»	105
7	410	135	90	96	80	10	90	06	120	96	95	56	110	115	90	90	120	95	501	20	120	115	105	120
8	335	\$9	25	09	02	88	90	š6	95	100	80	75	100	88	65	55	115	36	20	0.80	120	110	06	80
\$	125	96	90	9.6	135	115	001	25	110	115	7.5	98	120	100	100	56	0	125	105	001	041	521	105	011
90	403	82	80	8 0	115	125	\$6	×	120	001	85	96	130	105	\$6	۶۲	130	05	56	20	120	115	75	125
92	180	110	90	88	140	125	100	\$6	140	145	09	02	120	100	06	100	125	011	105	105	135	885	120	591
22	355	185	95	98	135	135	130	06	155	120	2.2	59	135	120	88	06	125	115	70	95	105	105	501	001
78	250	110	80	45	120	105	75	70	85	90	06	95	110	80	10	105	115	105	011	7.	120	511	96	115
*	410	145	35	9	9.8	100	88	85	105	115	125	90	120	90	0	09	135	011	70	06	125	511	105	001
06	365	115	105	135	225	125	100	35	06	80	06	011	100	100	06	50	5.80	0	0	\$	001	100	35	00
96	475	155	80	55	155	120	09	04	700	70	59	59	125	115	100	96	100	1 00	0,	75	105	06	59	95
102	150	09	55	55	110	115	185	60	110	001	88	59	130	105	980	06	130	-1-	001	501	051	150	7.5	æ S
801	370	220	150	501	190	90	75	90	115	105	105	75	135	95	20	55	011	09	09	55	011	001	100	105
+	561	100	75	80	150	110	011	501	105	75	0.7	60	100	55	75	80	75	8,						

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec or 5 min)

FABLE IV 6 FUEL VAPOR CONCENTRATIONS IN PPM

Test & Conditions Fuel - avgas Temperature - 71°F R H - 87%. Sample Configuration No. 2. Two gallons of avgas in a 5-sq ft pan in the center of the room, the run was made to coordinate the sample configuration with that used in Tests 1-5 - 11/10/71

Lime			-	-				1				sample !	Sample Point Number	mper.										
min)•	-	2		*	2	٥	7	a	2	10	=	15	13	<u>*</u>	1.5	91	17	x.	13	07	21	22	2	17
c	0	0	0	0	0	0	o	0	0.7	0	0	0	0	0	1000	825	0.64	0	7.0	3	3.6	3		
ø	100	250	5.0	0	20	C	0	0	0	0	0	0	0	0	CED	1000	054	2.5	001	0 0		9		
71	100	150	100	9.0	100	100	50	5.0	5.0	5.0	5.0	50	50	0	1000	350	1100	150	100	205	100	2	2	
œ.	150	150	150	100	100	100	5.0	5.0	100	20	100	5.0	100	9	1 (000)	600	1800	150	001	2	2	9	2 6	
*	150	200	150	1 00	150	150	100	05.	100	0.5	100	100	1 00	5.0	1000	1200	950	150	50	001	205	9	200	
01	200	750	200	150	200	200	150	051	150	100	() 5	150	150	001	1 0000	1200	350	150	200	4.50	150	0.5	2 4	
9	700	250	057	150	200	200	150	150	150	150	700	150	700	150	10000	200	1000	200	250	200	200	200	250	
2	250	300	750	250	250	250	200	200	200	150	700	150	200	100	1000	1250	550	250	750	200	250	250	250	
90	250	750	250	250	750	250	250	250	250	200	250	200	250	200	0000	1050	750	250	300	300	250	300	300	
*	052	300	300	310	305	350	3+5	330	3.20	245	310	300	320	270	1000	1000	059	330	3.70	335	320	310	335	
00	300	450	320	365	360	305	370	325	325	310	320	3 ! 5	345	280	1000	10001	1000	350	335	35.5	330	325	320	
90	300	335	300	360	395	355	355	365	350	345	335	345	250	378	1000	10001	740	355	405	445	5 7 8	385	495	
7.5	370	014	310	405	375	305	330	300	320	320	345	305	340	760	1006.	1000	855	350	4. 5. 5.	340	330	360	390	
on :	325	350	325	305	400	410	375	360	320	310	350	330	365	310	1000	1000	910	375	3 6	435	345	3.75	505	
*	325	430	330	425	475	340	365	365	300	340	330	355	7 30	350	1000	820	290	430	470	40+	340	380	515	
0	315	30.5	210	475	404	385	325	350	335	330	330	315	365	575	1000	695	1000	358	578	440	355	380	480	
9	335	370	355	376	415	415	004	375	355	335	355	350	380	355	1000	1000	880	620	346	308	385	305	400	
-1	345	350	335	375	430	380	07	3.10	0 7	101	340	375	350	135	1000	0 44	1000	+0+	0 [+	480	405	450	575	
20 •	375	545	0 7	45.5	475	0	360	380	355	320	360	315	368	335	1000	1000	1000	380	404	365	305	400	405	
• 9	346	275	000	000		0 * *	50	9 6	5.50	310	365	315	350	270	1000	10001	1000	375	335	0 7 +	350	100	510	
2	380	375	3 20 3	9 4	47.5	0 0	2 2	010	ree.	350	575	3.50	385	355	1000	00-	54,5	305	004	4	404	454	n	5 2
	175	3.85	175	2 2	2 2	0			0 0	3.5		E 0.0	0 ;	066	1000	10001	10/10	000	370	0	340	425	<u>u</u>	3.5
ı aç	3.00	405	00	4 4	7	475	415	664	475	2 4 4	r u	502	455	260	.000	0.00	2.0	1000	430	420	120	**	4	¥.
	3.25	415	405	4.45	250	175	105	15	1 7 2	150	7 7	0 1/2	100	7 6	1000	-000:	2 0 0	200	il a	\$ 0 t	450	4	555	m L
0	100	400	405	4.	530	500	460	054	430	u u	2.0	0++	262	1000-	1000.	1000	7 . 47	n in	ר ז <u>י</u>	2 4	0 C T		000	
0	435	430	0++	270	5 3 2	515	05+	5.00	if if	09+	475	00+	4 1, 1,	450	1000	1900	750	2 (ur ur	450	u v	1 to	1 L	1 2
ú	୍ର 🛨	470	06	530	240	6 30	J C S	07.7	7	470	506	**	ư ♂ 寸	455	1000	000	of C	7 4	550	505	505	7.3	.30	Li.
x.	435	04	455	525	175	525	+32	5 A	+ 20	3 T +	ं •	15	510	07.	1000	10001	07.0	630	510	505	50.5	4	6.20	
*	460	455	£0. *	ur ur	530	500	u/ • † u'	.6	573	430	of T	435	505	ارد ارد دو	1000	83 0	1000	· · ·	615	٧ (-	uf utc	u'		1 ~
0	ur ur	505	0 5	788	989	is m is	-	520	200	45.5	1.)" ("*	€	200	470	1000	1900-	0++	01	530	5.15	40.	7. .1	1,25	100
٤.	250	200	02+	a.	5 + 2	ir S ir	674	530	520	200	ur T	503	0.5	065	1000.	1000.	1000	4	019	5 1,	0	540	0	
75	475	+ 20	470	5 5 5	574	665	ir ir	3.0	538	210	1. 1. 5	0 5 5	550	515	1000.	-0001	0 4	26	54,5	550	545	500	560	
÷ ;	5 - 4	510	500	909	550	1 30	5	21.0	580	615	1. 1. 1.	535	455	210	10001	1000	1000	065	* 85	or or	500	4	4	4
+	505	200	505	30	oc :	2	275	4.05	5.5	245	540	5.53	200	u i	1000-	1000	0	200	11	635	78.7	4	0.5 4	4
٥	5	21.5	005	560	024	705	000	5+3	509	5+0	54.0	555	530	505	1000	1000	1000	130	705	204	001	403	200	0 7
0:	이 1 다	500	T.	7 C L	502	576	077	57:	019	600	270	404	260	ur. oc	1000	1000	1000	0.40	0 [584	0+0	044	0.40	
7]	075	2.0	4	0 10	200	720	5	0001	17	610	2,00	480	5c0	1000	10001	1000	1000-	620	u z u	01-	504	if if if	710	
10 to	4	515	C)	25.0	623	0+9	450	565	505	580	620	585	580	565	1000	1000	1000	520	324	0+.	1 15	.20	.20	
+	9++0	450	45.5	979	2	0+0	520	0+9	204	014	£03	er er	909	5 5	1000	1000	1000.	0 2.	420	455	515	0+9	4	

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec. Sample Point No. 20 is 300 sec or 5 min)

TABLE IV ? FUEL VAPOR CONCENTRATIONS IN PPM

Test 7 Conditions: Fuel - JP-4. Temperature - 75°F. R.H. - 39%. Sample Configuration No. 2. Two gallons of JP-4 in 5-sq ft pan in the center of the room, the run was made for the same purpose as Test 6 using JP-4. 11/10/71.

Time											Sample	Point !	Number										
- laum	-	7	-	+	اء	•	۰	œ	۰	의	11 12	2	13	14	2	=	=	5	02	77	2	2	2
0	•	0	•	0	•	0	0	0	•	200	0	0	•	0 10000+	0+ 2850	5002 0	001	150	200	100	\$0	0	0
•	0	0	o	•	0	•	0	001	20	90	0	0	0	0 10000+	009 +0	0 950	200	50	\$0	150	150	001	0
12	120	8	110	175	170	017	522	200	205	021	591	0.	1 091	190 1000	0+ 0	1000	4 370	290	280	340	335	280	90
	195	170	150	180	160	\$12	512	255	275	552	027	1 022	185 1	185 1000+	0+ 830	1000	. 355	350	370	340	390	445	90
\$ 7	240	200	180	335	561	270	552	592	582	270	052	2 552	2 512	260 1000+	065 +0	1000+	+ 415	240	340	385	305	430	90
30	760	230	210	335	250	375	290	305	305	290	582	275	270 3	300 1000+	+0001 +0	+0001 +0	4 365	330	380	435	485	360	55
36	290	092	230	310	335	355	300	300	355	315	330	592	315 3	310 1000+	916 +0	+0001 5	+ 550	370	440	430	420	370	9
45	760	250	240	380	335	365	350	340	340	345	340	350	330 3	380 1000+	0+ 915	1000+	450	370	455	490	475	470	9
‡	305	325	315	340	335	355	355	380	360	360	355	340	345 3	360 1000+	0+ 820	0 745	460	390	420	\$20	40	480	09
Z.	345	335	35	410	325	385	400	385	380	395	385	375	35r 3	385 1000+	964 +0	5 735	515	455	455	495	425	260	09
0,9	345	345	340	360	405	430	405	415	014	385	390	385	385 3	385 1000+	986 +0	5 705	450	455	435	45	500	260	9
3	380	370	365	475	450	460	415	415	465	094	405	395	405 4	+15 1000+	0+ 815	5 775	435	375	375	480	510	535	9
22	450	410	400	455	450	475	405	450	415	000	014	355	450 4	435 1000+	0+ 190	0 835	\$25	425	490	585	910	575	0.0
78	410	410	390	400	405	435	430	440	455	455	430	410	430 4	440 1000+	906 +0	5 630	999	470	455	445	480	460	09
8	390	395	390	435	460	410	425	450	0#	475	420	370	4 5 2 4	435 1000+	0+ 610	0 950	515	490	520	480	540	475	09
90	420	360	365	490	385	64	440	455	525	415	425	450	450 4	440 1000+	-0001 +0	988	510	430	425	550	445	200	09
96	410	425	415	450	445	405	430	445	450	460	390	410	4 514	425 1000+	04 620	1000+	475	455	455	535	545	530	09
102	390	360	350	480	450	455	460	410	480	455	445	415	455 4	435 1000+	965	1000+	+ 530	480	520	475	445	540	09
108	365	360	340	475	505	480	435	445	460	455	435	425	435 4	455 1000+	0001 +0	1000+	+ 500	540	520	\$05	595	580	59
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921	395	395	405	929	555	540	410	455	450	435	445	435 4	+ 09+	460 1000+	069 +0	068 (520	510	540	009	\$0\$	520	59
132	450	455	440	415	910	485	425	200	485	465	435	455 4	455 4	425 1300+	+0001 +0	1000+	+ 625	480	575	909	\$25	909	09
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The ti	me sho	1 CO L	The time shown corresponds to Sample Point No. 1.	to Sam	ple Poin	t No. 1		Each sample point beyond No. 1 is	point be	yond No		spaced 1	15 sec (e. g		ple Poir	Sample Point No. 2 is 30 sec,	is 30 se		ole Poin	t No. 20	is 300	Sample Point No. 20 is 300 sec or 5	min).

TABLE IV-8. FUEL VAPOR CONCENTRATIONS IN PPM

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100				800	850	900	1900	2850	2900	1550	200	5450	7450	6400		0526	3400	2750	3000	3400	800	800	3
8				006	1050	1900	2300	2000	1900	2200	1700	4900	7000	2900	9550	6400	1900	1750	2060	3050	950	000	ŏ
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16.5				1050	1750	0591	0017	1700	1650	1850	1700	3250	5300	4500	8800	6550	1850	1600	1850	1700	1750	750	ě
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715			0007	0007	1950	2000	2050	7100	2950	2150	2050	6300	9150	2900	1 0000	9700	3450	2650	2100	2750	2100	050	9
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2500				2350	2400	2400	2500	2450	2300	2500	0557	2750	2800	6250		8900	3050	2300	2550	2600	2350	400	150
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253				2550	2550	2500	2700	2450	2400	2600	2450	6850	7400	6700		5350	2850	2550	2500	2750	2550	009	150
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2500				2500	2500	3300	2300	2700	2600	2200	2200	2150	2000	4000	9 200	4700	2300	2250	2250	2250	2350 2	450	100
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1650				1700	1700	1450	1400	1450	1400	1400	2100	2100	1900	3300	4800	2750	2650	2200	2300	2350	2300	350	100
85				900	900	800	750	800	750	750	750	2002	0071	1550	1400	2150	1400	1350	1300	1350	1500	450	٠
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TABLE IV 9 FUEL VAPOR CONCENTRATIONS IN PPM

Test 9 Conditions: Fuel - JP-4. Temperature 54'F R H. - 77%. Sample Configuration No. 2. Two gallons of JP-4 in a can suspended 5 ft above the floor just east of the center of the room and allowed to drip steadily. 11/11/71.

Time											Sar	nple Po	Sample Point Numbers	bers										
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94	5	040	017	069	502	695	202	089	645	865	670	630	100	570	,	1000+	935	710	599				735	55
22	850	260	90	780	240	745	502	57/	402	589	705	089	720	715		10001	880	785	680				785	9
82	200	2002	920	760	650	6.50	, ,	650	049	200	000	570	45	575	,	1000	735	069	645				150	0
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791	9	009	009	750	750	000	750	800	750	800	150	700	200	150		2150	850	006	800				900	,
192	000	000	200	950	006	056	000	000	950	750	850	800	850	800		1950	1100	200	850				000	
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704		007	0 0	000	067	067	067	057	057	250	250	057	250	250		250	350	250	250				300	0
522	2.0	260	250	330	330	587	145	336	587	517	582	275	280	240		567	395	320	280				340	3.0
552	335	335	325	335	350	360	305	340	320	362	575	3.5	320	0 1		455	355	325	320				340	09
582	270	290	290	265	275	285	295	300	0	90	206	300	200	200		340	570	355	330				340	75
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249	235	240	245	240	250	245	240	245	245	245	245	240	245	245		245	360	255	250				046	10
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732	061	195	561	200	200	200	190	061	140	185	061	185	190	190		200	245	200	195				205	0
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TABLE IV-10. FUEL VAPOR CONCENTRATIONS IN PPM

Test 10 Conditions: Fuel - JP-4. Temperature - 71°F. R.H. - 875. Sample Configuration No. 2. Four gallons of JP-4 in the same location as Test 9. 11/15/71.

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	22		00	150	300	200	8	3	200	9	750	750	00	2	00	750	150	820	820	8	820	900	650	850	650	550	450	400	9	250	901	80	09	*
	ž	:	9	8	350	450	2	3	900	150	650	150	650	220	200	120	200	200	8	950	8	89	650	200	750	909	90	00+	900	250	00	22	9	AR
	07	2	3	200	250	300	450		000	000	250	650	8	8	820	9	850	820	800	020	820	950	750	750	850	150	220	450	950	350	150	80	55	7.5
	61	350	200	300	350	350	450	200	2 5	066	000	200	8	202	000	3	850	3	820	9	90	900	200	800	950	150	000	200	050	450	001	9	20	**
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		0	907	200	90	3	350	350	550	200	550	650	750	750	800	750	900	800	850	850	750	650	800	750	200	200	460	200	250	200	3 4	2 5	4	
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1		•	•	21	=	2	•	2	2	7	?	I										132												

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec or 5 min).

TABLE IV-11. FUEL VAPOR CONCENTRATIONS IN PPM

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The time shown corresponds to Sample Point No. 1. Each sample point heyond No. 1 is spaced 15 sec. Sample Point No. 2 is 10 sec. Sample Point No. 20 is 410 sec. or 5 min)

TABLE IV 12 FUEL VAPOR CONCENTRATIONS IN PPM

Test 12 Conditions: Fuel - avgas. Temperature - 52°F. R. H. - 50%. Sample onfiguration No. 3. Four gallons of avgas in a spill at the center of the east wall. 11/19/71.

	12	5	200	3	00+	9	400	300	200	200	200	200	200	150	150	150	100	20	4	¥		0	07	52
	2	901	2 2	300	0047	2800	2600	2100	1950	1950	1750	2350	2000	0061	1650	009	1300	1150	435	1		683	507	200
	22											2150												
	12	98	1300	2000	2500	3500	2400	2200	2500	2100	2100	2150	1700	1600	1450	1400	1500	1200	430	425	366	200	2	230
	02	2400	7 300	200	3	000	2600	2300	2550	2250	2150	1850	2350	1850	1550	1450	1100	1150	455	310	205	600	200	200
	=	3100	4900	200	3	00	3300	2600	2850	2650	2400	2000	2100	1700	1550	1400	1200	1250	410	300	290	200	3	195
	=	2900	2000	35.00	0000	0000	3700	3000	3450	2250	2050	1600	1700	1700	1750	1500	1350	1200	460	305	200	2 6	2	180
	=	2900	12300	12100	3	200571	2900	4400	4250	9050	3550	4050	3600	3550	3450	1950	3500	1463	710	385	315	446	,	310
	2	20000+	20000+	20000	2000	10000	16500	10000	8200	7250	7350	3400	2500	1700	1550	1750	1350	1250	435	330	285	1 9		207
	2	_	_			-						1950												
mbere	=											1150												
Sample Point Numbers	2		_	_								1350												
ample I	2	00	5700	4600	2000	2300	2007	1800	1800	1600	1550	1400	1500	1400	1400	1350	1250	1100	400	280	255	165	140	201
Ŋ	=	1700	4100	3800	3100	90	2	2600	2100	1650	1550	1500	1600	1650	1500	1450	1350	1300	450	325	275	195	210	3
1	2	067	4300	5400	4400	2600	2007	900	200	0091	1700	1400	1600	1450	1400	1400	1350	8 = 1	400	295	250	185	200	3
	0	200	2600	4100	3200	2000	200	0017	2000	1800	1700	1600	1600	1550	1600	1500	1350	1200	400	300	260	205	206	3
	-		•			•	•	•	•			1500			-									
	-	100	1800	2700	1600	2 4	2000	2007	906	9	1650	1500	1600	1500	1600	1500	1250	100	350	270	260	210	210	•
	اه	100	700	1600	2100	246	200	2005	2100	2	1750	1600	1600	1650	1700	1550	1550	1400	450	340	305	215	22.0	}
	~	001	200	1400	1800	24		3	20047	2000	89	1500	289	1600	1650	1880	1400	1350	200	335	562	215	220	}
	•	100	700	1500	006	228	2	3	0017	0002	138	1650	899	1600	1700	1600	1450	1350	450	335	310	215	220	}
	3										- ·	2022												
	~							-				2250												
	-	8	800	1300	1800	210	9	200	2047	0567	2200	2250	2050	1950	1900	909	1500	300	450	335	296	215	150	1
Time	min	0	•	•	12	16	20	2	,	87	3 ?	9 (2 :	\$:	*	7 ?	9 5	3	180	270	360	450	504	1

TABLE IV 13 FUEL VAPOR CONCENTRATIONS IN PPM

Test 13 Conditions: Fuel - aygas. Temperature - 98°F. R.H. - 79%. Sample Configuration No. 3. Same as Test 12 but at a higher room temperature. 11/22/71,

	-	3		200	909	800	6	300	000	0071	3	000	1000	900	800	000	200	9 5	00/	200	009	009	9	200	300	300
	1.	3		200	1000	2700	4700	2300	200	2000	200	0079	0009	2600	4400	4100	200	2200	00/5	2600	3500	3100	2800	2500	1700	1800
	12	:		200	300	1700	3500	6700	24.5	2007	2000	2800	2500	5300	4200	3200	270	0076	2300	35.00	3600	2900	2900	2600	1600	2100
	2	:		00+	0019	7200	7400	76.00	0014	7	0000	2600	4500	4100	4600	3600	200	3300	35.00	0065	2000	2600	2600	2600	1700	1800
	2	;	0000	2300	8000	7700	8300	9200	7500	2000	200	0079	4800	4400	4300	4000	3000	2000	2000	200	200	2600	3200	2800	2000	1700
	0.7	i	4000	200	9800	7100	2600	0000	8200	2200	2077	0000	4500	3900	2000	3900	3200		200	000	35.00	3000	3500	3600	2300	1700
	81	:	0000	0000	2100	7500	6700	2000	5400	4800	1300	3	2800	3200	4760	4000	4000	2200	200	200	200	7300	3000	3800	1800	1800
	-1		11400	0000	15300	20000+	12400	1900	13600	10500	0000	200	2000	2400	4900	2600	2400	2500	1800	3200	0000	1800	2500	4800	1100	1400
	٩		20000	2000	+00007	20000÷	20000+	20000+	20000-	20000	20000	10000	20000+	19800	00961	16800	15900	16000	14500	3300	0000	00671	15100	11900	7300	2000
	15		200004	3000	700007	±00007	20000+	200004	20000+	17800	15100	200	2000	13300	12400	12700	9100	0060	9500	9800	0076	0000	0400	8200	4100	3100
nbers	2		20000	2000	+00007	+00007	20000+	20000+	20000+	20000+	18900	2000	2300	13200	13500	11400	10300	10000	10400	10500	0100	3	9600	9400	4100	2200
oint Numbers	=		18000	15600	0000	13000	1420	17100	13100	11400	10100	0000	2000	9500	929	9500	4700	9200	5300	4100	4000	000	4 700	3200	009	1500
Sample Po	21		1100	9400	000	2067	9300	8800	8600	6800	5300	4300	000	1000	4500	000+	3500	3200	2800	2900	3000	2000	7,000	2200	1500	1900
S	=		700	2300	2000	0040	96600	6500	5800	\$200	2000	4800	000	914	4100	4000	3800	3600	2900	3200	2700		0047	0067	1900	1700
	0.		200	7100		000	8200	7000	2100	5400	2900	2600	100	3	4900	1300	3800	4000	3100	3200	2700		00/7	3 3 0 0	1400	1700
	•		00+	2000	200	2000	8600	7400	7800	9009	5600	5800	0077	000	2100	4800	4100	3700	3300	3300	2900	000	0067	00/7	0007	1800
	æ		0	5200	100	0000	0000	0369	5300	2800	4500	5400	1300	200	4800	4400	4100	3300	3300	3000	2900	2300	2300	0057	004	1400
	1		0	6100	4700	000	007/	0099	7200	2100	5500	5200	0000	0000	4800	4600	3900	3600	3300	3100	3000	2100	2000	00/7	1800	2000
	٥		•	400	90	000	1000	3700	4600	4400	5500	3700	60.78	2	2400	3000	3400	3000	3200	3200	2600	3000	2007	0077	1000	2200
	٧.		0	100	100	9 6	906	1000	2400	3800	2400	3600	AROO	000	200	3400	3400	3300	3300	3100	2700	2700	200	0007	8	7100
	*		0	001	400		3	3800	4500	2100	5700	5800	5300			3100	3600	3200	3300	3400	2600	2700	36.00	0000	200	0017
	7		0	200	400	3	3	800	1300	1700	2500	3300	1500	3000	2000	2/00	3500	3500	3300	2900	2900	2600	0000	200	3 6	7000
	~		0	400	600	900	3	1000	1400	1800	2400	3000	3400	3000	0000	2800	3400	3500	3400	3000	3100	2700	000	000	000	3
	-		•	1300	1600	000	200	7300	2800	2400	901	3900	2200	1000	000	3400	3600	3600	3400	3100	3000	2700	2000	1800	000	200
Time	dim.		0	*	40	-	::	2	20	*2	82	32	36	4	; ;		*	25	96	3	89	77	1	1		\$ 7

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-14. FUEL VAPOR CONCENTRATIONS IN PPM

Test 14 Conditions: Fuel - JP-4. Temperature - 97'F. R. H. - 85%. Sample Configuration No. 3. Four gallons of JP-4 in a spill at the center of the east wall. 11/23/71.

	2	700	2 6	3 5	200	200	200	200	400	604	2	2 4		175	140	120
	5	900	2 9	2000	2500	2500	2500	2400	1800	1650	1600	1500	850	490	485	305
	2	400	2000	2000	2300	2500	2800	2400	2000	1800	1800	1650	900	485	425	335
	77	200	1600	2200	2200	2900	2700	2200	1750	1650	1550	1500	850	200	400	320
	2	1200	2600	3200	2400	2800	3100	2100	1700	1500	1500	1400	850	200	365	300
	67	2500	4400	3700	2500	4100	3100	2200	1650	1550	1500	1400	800	485	365	562
	81	2200	3100	3900	2900	2900	2600	2400	2000	1800	1750	1550	850	470	380	345
	2	2600	9700	2900	4800	6200	4300	4200	2400	2850	2650	2100	006	460	430	345
	9]	20000+	18000	14200	13100	12000	4900	2600	1800	1600	1600	1450	800	200	350	290
	2	16000	11600	0066	6300	2600	3000	2400	1700	1500	1550	1300	800	485	340	082
bere	±	0	14700	12800	1900	1700	1600	1700	1300	1250	1200	1150	700	00+	305	245
Sample Point Numbers	=	300	3700	2900	3400	2100	1600	1800	1350	1300	1300	1200	700	420	315	255
nple Po	2	200	909	1600	2100	1800	1700	1900	1400	1400	1350	1250	750	445	340	270
San	=	0	1600	1900	2200	2300	1700	1700	1400	1350	1350	1250	750	445	350	275
	2	200	2900	2300	2500	2500	1800	1800	1450	1400	1400	1300	800	455	360	280
	ام	0	1600	2500	2500	2600	2100	1800	1500	1450	1400	1300	800	455	360	290
	∞	0	909	1000	1700	1900	1800	1700	1450	1450	1400	1300	800	455	300	562
	-	0	300	1000	1800	2200	1900	1900	1600	1650	1550	1400	850	200	390	320
	0	0	200	1200	1800	2000	2000	2300	1850	1750	1600	1600	900	515	014	340
	اء	0	100	1200	1800	1800	2100	2300	1900	1800	1700	1650	950	515	410	345
	•	•	400	1100	1700	2100	2100	2400	1900	1850	1650	1600	900	210	410	335
	-	•	8	9	1200	1900	2200	2600	1900	1750	1550	1500	9	200	400	325
	7	0	200	1100	1600	2200	2300	2700	1950	1700	1550	1550	850	495	390	320
	-	0	200	1400	1800	2200	2400	2400	2050	1600	1400	00	800	+30	340	285
Time	(min)	0	•	•	12	91	50	54	87	32	36	9	901	168	872	252

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 in and 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-15 FUEL VAPOR CONCENTRATIONS IN PPM

Test 15 Conditions: Fuel - augas. Temperature - 52°F. R. H. - 74%. Sample Configuration No. 3. Four gallons of augas in spill at the center of the east wall. 12/1/71.

	74		000	3	000	900	900	900	700	400	200	3	909	9	200	400	2	3	350	350	150	2	000	30
	23		9	000	000	1900	2000	2500	2500	2100	200	200	0007	2000	1800	000	2	3	7000	2050	1750	000		9
	22		91		000	2100	006	2400	2100	2100	2400	200	2100	2300	2000	1850	1750		1750	1900	1650	1060		676
	12		200	200	2007	2900	3100	3600	2800	2200	2300	200	0047	2100	1600	2250	2000		0061	2350	1600	860	,	2
	20		200	3,00	2007	2000	3300	3600	2700	2400	2400	2300	2300	1950	1800	2150	2350	3000	2007	1950	1450	800	7.5	-
	6-		300	207	200	001	001+	3600	2900	2400	2700	34.00	2000	7100	1900	2350	7150	200	006	2000	1500	800		î
	x		200	2000	2000	000	2400	4600	3400	2900	2600	2200	200	7.00	2400	2350	2150	3200	277	2150	1800	1100	415	
	17		1750	0000	2000	0000	200	8600	7500	5000	5800	4500	200	2100	5300	2800	2400	3050	0000	0597	2200	1800	440	
	اء		0000	10000		10000	300	4300	4600	11600	8900	0000	0000	200	0069	6700	0009	6250	0000	5850	2200	800	410	2
	2		2200	4700	900	200	200	1700	9400	7300	0009	6700	0007	06.00	4300	2000	2250	1850	000	1800	1300	750	490	
bere	=		0	0009	3100		200	00/7	8200	0059	2200	3200	4700	00.0	2000	1500	1500	1200	000	200	900	550	326	ì
Sample Point Numbers	13				_	200		_																
ple Pot	2		0	700	1000	200		200	3000	2200	1500	1900	1600	200	400	1500	1600	1500	250	06.7	1150	750	395	:
Sam	=		0	1600	1200	2200	2000	200	3000	2500	2400	2600	000	200	0061	2100	1800	1450	0071	200	1300	800	410	
	01		0	2450	3200	2700	26.00	000	3700	2700	2200	2100	2000	200	1500	1600	1600	1450	1400	200	0071	750	395	
	6		0	1350	3600	1000	24.00		2400	2800	2400	2400	2100	000	0061	1700	1750	1550	1350	000	0571	800	410	
	80					2000																		
	<u>-</u>					800																		
	9		0	0	100	1700	000	3 6	3	80	000	006	000	000	200	009	059	009	200	200	400	006	470	
	2		0			1500																		
	•		0			1500																		
	-	,	0			009					0.1													
	2	•				300												_						
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Lime	nin	,	5	+	-	17	6 2		3 3		28 2				• •	•								
H	5					-		•	• •	•	•	-1	1	1	,	•	*	-1	•	,	,	=	ň	

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-16 FUEL VAPOR CONCENTRATIONS IN PPM

Test 16 Conditions: Fuel - avgae. Temperature - 60°F. R. H. - 78%. Sample Configuration No. 3. Ten gallons avgae in large spill at the center of the east wall. 12/2/71.

	ž	i,	•	8	300	000	200	200	400	2	1200	1300	1050	350	400	800	650	008	9		3	250	300	207
	2	•	-	90	000	8	000	00 :	000	000	300	1450	1350	1400	1450	1550	1400	1450	1460		3	200	057	20
	22	•	•	3	9	00	000	000	900	200	90	820	1350	950	001	1050	1000	1150	8		200	000	200	20
	[=	•		3	8	008	8	900		200	1300	820	0091	1150	1500	1200	1050	1150	1200		3 5	950	2 2	3
	02	•	9	3	00+1	000	200		300	3	1300	7300	1550	1350	1100	1750	1650	1200	1650	9001	3	200	180	?
	2	•		300	00/1	200	9 6	200	200	0000	200	0007	2	2150	1250	2550	2300	1300	1850	2		3 5	150	
	=	•	200	200	200	3 5	3	200	1300	200	900	906	1 20	1500	1500	1300	1250	1250	1500	000	9	3 6	200	}
	=	•	11200	200	200	12100	200	22.00	200	200	200	200	2200	7100	3150	1700	2400	2350	2500	9081		4 6 6 6	200	
	2	c	20000	2000	1000	20000	19300	18500	140	200	30.0	2016	3	4820	4100	\$250	2000	3650	4550	1150	650	2 5	150	
	=	0	20000	12600	200	23.00	12600	13400	8100	626	300	0000	0000	4500	4150	4450	3150	2350	2000	850	850	250	150	
:	=	0	20000+	14600	400	17700	17900	14800	10300	2000	3 5	2007	200	0057	2550	2700	906	90	950	800	200	250	150	
K Numbers	=	0	11600	2100	2300	4900	4600	4300	4200	900	2000	200	0017	1850	2000	1250	1150	950	1150	950	200	250	150	
Sample Point	2	0	100	200	9	200	9	9	800	700	9	3 5	200	900	800	9	900	100	750	750	450	200	150	
Sam	=	0	300	1300	9	800	900	800	1000	1000	2	200	200	0001	200	1050	1200	1200	1150	900	009	300	150	
	2	0	90	1500	9	8	800	800	1600	1400	1700	200	3 6	3	3	8	1050	1200	1050	850	200	250	150	
	6	•	2	_		_	_	_	_								_	_	_				150	
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The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-17. FUEL VAPOR CONCENTRATIONS IN PPM

Test 17 Conditions: Fuel - JP-4. Temperature - 50°F. R.H. - 74%. Sample Configuration No. 3. Four gallons of JP-4 in a spill at the center of the east wall. 12/3/71.

	1	5		•	200	300	300	300	200	100	8	3 :	120	150	150	150	100		3	2	120	105
	;		•	0	300	009	800	900	1800	1600	1400		1420	400	300	1400	1200	090	000	820	775	705
	,	:	•	0	200	9	000	906	1100	1100	300		3	1450	1300	1500	1200	1200	200	450	870	775
	7	:	•	9	00	1400	90	000	1200	1100	1300	35.	000	00+	400	1450	1200	1150		9	840	730
	20		9	3	200	006	007	0091	1800	1300	1400	2		1350	1550	1300	1200	1000		900	745	969
	0		7	200	3	2017	1300	1500	2100	1400	1400	1460	200	3	0571	1350	1150	1050		920	740	9
	887	1	•	9	2 6	300	0071	90 -	1200	1200	1300	1550	200		1350	1400	1400	1150	000		47.7	730
	2		400	9	200		0000	2007	3000	2400	2300	2350	200	000	0001	1950	0091	1500	0	200	463	730
	91		3500	8400	2000	200	0000	3	2400	2400	1700	1600	400		000	1350	1150	000	080		2	680
	22		4500	4000	2008	6440	2000	36.	00/	1600	1500	1450	1200	1350		0661	1150	0001	000	136	67	989
	=		0	RIOO	6000	900	3 5	3	90	900	1100	1150	9	2 2	3 5	0611	950	950	900	377	00	280
Numbe	2		0	3100	2600	2300	2100	300	009	1100	300	1400	1400	1350	200	0661	1050	0011	950	918		730
Sample Point	12		0	0	404	20,	9	2 6	200	200	000	1150	1150	9	2	0011	0001	1000	800	716		665
Semp	=		0	100	909	1200	300		200	000	1200	1300	1350	1300	1300		1150	100	950	830	3	22
	9		0	90	1000	009	800	9	200	3	90	1200	1150	1250	1200	001	001	1050	900	800		(1)
	6		0	100	009	800	900	8	3 6	3	1100	1250	1350	1300	1260		0011	1050	950	820		2
	80		0	0	300	200	900	800	200	2	0071	1300	1350	1350	300	300	200	1100	950	845	200	9
	7		0	0	300	004	009	200	9	200	1000	1150	1250	1200	100	9	3	1050	850	755		2
	9		0	0	001	400	200	ADO	8	2	200	1250	1350	1300	1300	200	3	8	900	800	100	200
	s		0	8	001	400	900	000	9	200	8	1300	1350	1400	1300	1260	200	100	950	815	100	2
	+		0	0	200	00+	800	906	90	3	3	1350	1400	1350	1350	1200		201	950	780	324	2
	-		0	8	00+	90	900	1100	1600		3	1500	1450	1350	1350	1200	200	3	900	290	770	2
	7		0	•	400	200	1000	1100	1600	200	200	1400	1450	1350	1350	1200	000	9	900	780	760	3
	-		0	700	009	1000	1200	1100	1300	000	200	0071	1350	1250	1250	1150	0 20 1	1030	850	725	705	3
Time	min		•	•	•	12	91	20	24		27	32	36	ş	\$	6	. 30		150	180	186	3

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-18 FUEL VAPOR CONCENTRATIONS IN PPM

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	23	•	2	3 8	8	3	3 8	3 8	8	8	900	1000	1200	1300	1300	1300	1500	1500	1500	1600	1700	1800	1800	1800	1800	1800	2000	1750	1600	1400	2	725
	2	•	9	3 5	9	3	3 5	9	900	1300	1500	100	2000	2800	1400	2200	2100	1600	2100	1900	1900	2200	1900	1800	1900	1900	2100	1900	1550	300	90	8
	17	8	2 5	8	1800	40	200	300	1600	2800	2000	1700	2100	2300	1700	2500	1700	1800	1700	1800	1900	2000	1900	1800	1900	2100	1900	1750	1700	1200	1200	1200
	2	901	8	9	200	2	9	000	1000	00	1100	1100	1000	1200	1300	1400	1500	1400	1600	1800	1700	1800	1800	2200	1800	1900	1900	1850	1450	1250	90	1050
	2	200	400	1700	1300	2000	2200	1100	1300	1700	1300	1300	1200	1400	1400	1700	1600	1600	1900	2200	2200	1900	2400	2600	2400	2300	2300	2100	1550	1350	1150	200
	=	200	000	800	2800	2300	2000	2300	2700	3900	2300	2800	2700	2900	2000	3000	2200	2000	2000	1700	2000	2000	2000	2100	2100	2700	2000	1800	1600	1450	1200	1300
	=	3100	8600	13400	18800	17200	13600	16800	14300	15600	13400	13200	14500	12500	11200	12600	8400	2600	9100	6400	8700	7100	9100	5300	4800	4600	3900	4150	3150	3800	3000	2600
	2	9	20000+	20000+	20000+	20000+	20000+	20000+	20000+	20000	20000±	19100	18100	19200	16400	14900	14700	13000	12000	12500	1100	10900	8700	7200	8700	8000	9	6050	4400	3500	2800	3100
	2	0	15100	17600	18100	18500	17900	17300	16100	17400	14000	12800	14300	15200	11400	12400	10700	8700	0096	8900	1500	8600	8500	5500	7400	5400	2400	5100	3300	3250	2550	2200
:	=	0	17600	20000	17700	18900	20000	15600	18200	16600	15800	15300	13300	14500	13800	12200	11000	9000	9400	7500	9700	\$700	0099	2400	2600	4400	3800	3250	2250	2200	1600	1700
Sample Point Numbers	2	0	4700	700	9900	9700	7600	6800	9200	7400	5700	8000	9	1900	9009	\$200	4600	2800	4100	3800	4100	3100	3500	3100	2500	2800	2400	2550	2000	1450	1300	1100
ple Poi	21	0	8	00+	300	200	200	909	100	800	200	9	800	900	0001	200	1200	1700	1200	1300	1400	1500	1600	100	1700	1700	1700	1550	1350	001	1000	900
Sam	=	0	200	400	200	9	900	200	800	1100	800	1000	900	0001	1500	1200	1300	300	1300	1400	1500	1700	1600	1600	1700	1800	1800	1650	1350	1150	000	880
	2	0	300	909	1100	800	900	700	1100	1600	800	900	906	1500	1100	1100	1200	1300	300	1400	1600	1500	1600	1700	1800	1700	1800	1600	1400	1250	100	1000
	•	•	•	1000	1400	1300	1500	1400	1600	1900	200	1400	1500	1600	1700	1700	1700	1800	1700	1700	1800	1800	1800	006-	2000	1900	906	1700	1500	1250	1100	950
	••	•	0	200	400	9	400	200	9	200	8	100	800	800	1200	1200	1200	1500	1300	2600	1600	1400	1600	1700	1700	1700	1700	1550	1400	1150	000	900
	-	0	0	90	300	300	200	400	200	909	009	009	200	9	800	8	100	1200	200	1200	1300	1400	1500	200	1700	909	1700	1500	1400	1150	1050	900
	٥	0	0	200	300	\$	8	900	200	909	8	100	200	800	906	138	1200	1200	300	1400	1600	1600	1600	1 700	009	909	100	1600	1450	1200	1050	800
	~	•	0	200	300	3	400	200	909	9	90	8	2	8	000	1300	9	1200	200	400	00/1	1600	009	200	200	009	1700	1700	900	1150	950	820
	7	•	•	300	00+	200	200	100	9	9	3	800	800	900	200	2	2800	1500	1300	1300	1500	1600	0091	90.	1600	1700	100	1550	1350	1200	1000	950
		•	•	300	400	9	9	9	100	200	100	8	900	000	8	000	2	000	200	000	2071	200	200	009	0097	1700	1500	1250	2	800	300	750
	7	•	•	9	8	700	28	100	800	00	008	200	906	006	2	1500	00	00 1	000	0011	204	1400	0091	3	0001	00/	1200	1300	1150	820	850	750
j	-	0	•	1200	1600	1600	1700	1700	1600	28	900	1600	1700	1700	200	1800	1700	1700	1500	1500	00/1	00/1	0081	0081	00.	2008	1 700	1350	1250	900	900	8
Time	(win)	0	•	•	12	91	20	54	82	2	2	•	‡ :	₽ :	25	20	9	\$:	2 6	2 7	9 8	9 6	\$ 8	0 0	2 3	?	20	176	412	526	2%	336

oThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV 19. FUEL CONCENTRATIONS IN PPM

Test 19 Conditions: Fuel - avgas. Temperature - 67*F R.H - 90%. Sample Configuration No. 3. Four gallons of avgas in spill at the center of the east wall. 12/8/71.

Time										Sampl	· Point	Sample Point Numbers	:									
Tinim.	N	-	*	<u>~</u>	اه	-	60	0	2	=	2	=	=	2	2	-	2	2 61	12 02	2	2	77
0	_		0	0	•	•	0	0	0	•	•	_	0099	8700 20	-	0090	200	400	400			3
8 +	_		8	100	001	001	300	800	200	400	200	14900 2		7	0000- 20	-	_				3	900
8 220	_		300	00+	909	300	200	7100	200	300	~		~	~	~	~	. ~	_	-		_	2000
•	_		400	009	300	300	300	2500	100	009	800 2	2 -0000	00000	00000+ 20	~	~		_		_		2100
16 280	_		9	00	300	300	300	2800	1600	1000			~	~	~		-	_	_			2100
•	_		000	00+	200	00+	400	2300	2000	1300	~	4		~	~	0000	4 0061	1300 13	300 1300	_	_	2200
•			000	400	000	00+	400	3000	7600	1700	~		~	r,	~	•		_	_	_	_	2200
•			200	200	00+	200	200	3200	3700	2400	~		~	~	~	•	9 0029	-	800 2000	_	_	2200
•	_		009	200	200	009	200	3300	4100	3300	~			~	~	Ť	_	_	•	_	_	2100
•			900	200	000	200	0001	3600	4900	4000	~			~	~	•	0007	_		_	_	2000
			600	200	005	006	1400	000+	0009	2000	6100 2	•		~	~	111	_	_	2800 2400	00 71 00	_	2000
•			9 9	200	000	1300	0091	4400	6300	2400	-			~	~	_	_	•••	•	_	_	2000
•			000	000	200	0047	2500	2100	1000	9009	~				~	•	_	•		_	_	1900
26 220	_		3 6	000	900	2000	0027	2000	7400	7300	~		•••		~		_	Ì	1700 4500	0 1200	_	1900
•	_		3 3	000	900	2500	2500	0009	9000	1900	~		• •		20000- 20		•	•	•	_	0 1200	1800
-				3	3	006	000	000	000	000	_			•••	~		_		•	1200	0021 0	1900
•			3 5	3 5	000	00/5	2000	6 300	7800	1900	~					20000- 9	_	9600 56	5600 5700	_	_	1800
			3 5	009	006	0074	4100	9 100	8200	8000	8600					-	6 0010	•	900 5600	_	_	1700
•			3 5	200	000	4200	2500	2000	8600	8100	~				~	~	Ť	-	5300 5500	_	_	1700
•			9	000	3 5	0000	4200	9400	67.00	1300	7800 2					00000	9400 9	95 0096	_	_		1700
•			3	000	009	4000	4400	9 200	8100	1100						20000+ 9	_	8900 52	5200 5700	_		1700
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•			9 6	000	009	2006	4300	6500	1800	7300	_		~	. •	~	-	~	3800 58	•	1300	_	1600
•			200	000	200	4100	4800	0000	2006	7500	_	~					_	-	•	_	_	1500
	_		200	909	9 9	4600	26.00	00/00	7500	7300	1600	7100 2					_	_	•	_	_	1400
	_		200	2	90,	4600	2002	2000	200	2300	-	4 (•	٠,	4		_		2800 6600	_	_	1500
116 2100	006 00	800	100	009	009	4600	5800	0069	7500	2000	-	4 ~	2 +0000	0000- 20	00000 50	8 +00002			•	_	_	1400
	_		100	700	100	4400	5400	6700	7200	9	_	١ ٨	• ~		•		0000	29 000	0000 0000			1400
•	_		700	009	009	4600	2600	0099	6700	6700	_		-	. ~			•	, 4	0069 0066	0000		1300
	_		200	9	9	4400	5200	9200	9200	9300	9500	_	_	_	_		, ,	•	-		0001	9071
			100	200	009	4300	5200	9400	0099	9029	_	_	_	~	-	•		5500 54				0071
	_		100	9	909	4 100	2200	9700	0099	0019	_	1200	1 0018	7600 20	_	•	_	•				
	_		100	009	9	4200	2100	0009	9100	0009	2400	1 0051	7100	_	_			•				3
	_		200	100	200	4000	4100	5700	5700	5700		1 0086	2900	-	_	•	· w			1200		900
			100	800	200	4000	2100	2600	5700	2500	_	~	-	_	-	•	_	_	-	_		1000
•			7,00	0007	0061	2000	2500	3000	2700	2600	5200	4300	8400	_	_	···	1100 2	~	_	~	~	800
			190	0041	1500	200	1600	2000	900	1200	1600	2800	9100	5700 7	4 0054	7 0081	000	800 17	700 190	0 1900	1500	909
	_		1300	1100	000	1200	1200	1400	1200	1200	1200	1800	0011	9 001	0009	1 0051	1 005	_	300 1400		_	400

oThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 15 sec (e.g., Sample Point No. 2 is 30 sec, Sample Point No. 20 is 300 sec).

TABLE IV-20. FUEL CONCENTRATIONS IN PPM

Test 20 Conditions: Fuel - JP-4. Temperature - 67°F. R.H. - 100%. Sample Configuration No. 3. Four gallons of JP-4 in spill at the center of the east wall. 12/9/71.

			,	,	,				Semp	Sample Point Numbers	Numbe											
	-	*	^	اء	-	50	•	2	=	21	13	=	13	2	=	2	=	70	12	22	2	77
	0	•	0	0	0	0	0	0	0	•	90	800	800	3400	902	200	8	•	•	•	1	
	0	•	0	0	0	0	8	001	300	0	2100	6500		20000	12400	200	3 5	9	9	9	0	8
	8	8	100	0	0	0	800	400	300	300	11300	+00000	8400	20000+	16800	1100	1300	909	3 8	9	3 5	3 3
	2007	007	002	00 5	8	00	1200	800	00	100	12300		+00002	20000+	18500	1600	2200	800	100	400	200	8
	3 5	30,	200	2007	00 5	007	1400	1300	200	1200	_		+0000	20000+	20000+	2600	2700	1100	200	200	600	1100
	2 5	3 6	007	007	200	007	0091	0061	1600	906			+0000	20000+	20000+	2800	3600	1400	1000	009	9	0
	2 5	9 6	000	200	200	90	200	0047	1800	2500			+0000	20000+	20000+	3600	4200	1700	1200	609	9	1100
	3 5	3 8	9 6	200	9 6	400	2000	0087	0022	2800	15700		+0000	20000+	20000+	3900	009	1800	1400	9	909	1200
	3 5	3 6	9	200	3	000	2077	2000	0047	3400			10000	20000+	20000+	4300	2500	1900	1500	900	009	1100
3 8	3	200		200	000	002	2300	3500	2700	3700			+0000	20000+	20000+	4100	5700	2200	1800	100	200	1200
	3 4	200	000	200	200	900	2500	3800	3200	000			+0000	20000+	20000	2100	6200	2600	1900	200	200	110
	3	3 8	9 6	000	2 5	2011	0087	1300	3500	4600			+0000	20000+	20000-	2600	6800	2900	2100	100	100	1100
	3	3 5	200	000	200	200	2100	9 100	3900	2000			+0000	20000+	20000+	9009	9	3400	2500	200	100	100
	3	3	200	300	200	1700	3400	0064	4300	5200			+0000	20000+	20000	6400	7100	3500	2700	200	200	110
	00+	9	00	300	1900	1900	3500	\$200	#400	2600			+00000	20000+	20000	6400	7300	3700	3000	200	200	
_	200	8	400	300	2100	2350	3900	2400	4800	2100			+0000	20000+	20000	6400	7500	4100	3200	800		
_	00	00	400	300	2500	2690	4400	5700	2000	2600			+0000	200004	19000	0099	7500	4400	3700	800	200	
	200	Ş	90	300	2600	2900	4300	5700	5300	5800			9800	20000+	19100	6800	7700	4500	3000	9 6	2 6	
_	200	00	00	300	2900	3100	4100	200	5300	0009			9300	20000+	19400	7200	7700	4800	4100	9 6	3 6	
_	200	400	400	300	3000	3200	4900	0009	5500	2900			19300	20000+	18600	7190	7800	4800	4200	0 0	3 6	5 6
0	200	90	90	300	3100	3300	006+	0009	2500	2900			0006	20000	18600	7100	7800	2100	4300	000	200	
	200	60	9	9	3200	3400	2000	9700	2800	0009	4000	18400	18500	20000+	18400	7400	7800	5160	4600	000	200	2
	200	400	9 9	004	3400	3500	2500	6300	2100	0009			8500	20000+	17600	9069	8000	2400	4800	800	800	8
	000	000	400	400	3500	3800	2400	9500	2500	0009			17400	20000+	17100	1000	7500	5400	2000	900	800	100
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	100	200	200	200	3300	3900	4800	2600	2100	2200	8500	00901	_		11400	6300	6400	2000	2000	200	8	9
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																			>>.	222		

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

IABLE IV-21, I UEL CONCENTRATIONS IN PPM

12/14/71.
comer of the east wall.
JP-4 in spill at the
3. Four gallons of
Sample Configuration No.
. 75%
Temperature - 65°F. R. H.
unditions: Fuel - JP-4
Test 21 C

4 800 300 112 2700 1100 22 3100 1120 24 3200 1100 25 3100 1120 26 3100 1100 36 3100 1100 46 3400 1800 46 3400 2000 46 3400 2000 46 3400 2000 46 3400 2000 46 3400 2000 48 3400 2000 48 3400 2000 48 3400 2000 48 3400 2000 48 3400 2000 49 3400 2000 40 3400 40 3400 2000 40 3400 2000 40 3400 2000 40 3400 2000 40 3400 2000	900 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	200 600 600 600 600 600 600 600 600 600	100 500 500 500 600 1000 1100 1100 1100	600 600 600 600 600 600 600 600 600 600	2000 2000 2000 2000 2000 2000 2000 200	0 4600 2000 10000 11000 11200	600 600 600 600 600 600 600 600 600 600	2500 2500 2500 2500 2500 2500 2500 2500	11000 11000	11800 20 111 1800	20000-20	13940 11900-1 2000 11900-1 2000	5 100 13100 10000- 20000 10000- 20000 10000- 20000 10000- 20000 10000- 20000 10000- 20000	20000 20000	000000000000000000000000000000000000000	2200 2200 5700 5700 5700	1,000	1200	300 800 1200 1400	3 9 8 8
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3900							7300 7300 7200 7000 7000 4800	9600		9300 20 9400 20 9400 21 9300 21	00000- 20	000- 200	00- 200	00. 2000	9	12700	4400	3700	2400	24.00
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4300							4800	2200		9400	8000 20			100- 200	30- 676	-	5500	3900	3600	3500
4300							4100	7100		1 0009	7900 24	02 -000	200 -200	100- 200	0099 -00		5300	4000	3800	36.00
4300							4100	1000		5700	7700 20	1000 - 20°	000+ 20C			7	-	4000	3800	3700
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4400							4800	0009		4300	4500 20	1000- 20	900+ 200		90- 590	9000	_	4200	3000	
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3400							3500	3400		3200	3100	4 004	100	200	98	446	4100	200	200	200
2850							3000	3050		2950	2700	050	25 054	100	25	3000	2200	2000	3 5	2500
2850							3000	3000		2950	2900	050	150 44	1	105	200	31.60	2000	2017	3130
2700							3050	3050		3000	2950	100	150 33		200	1200	1200	300	3 5	2000
							3000	3000		3000	1000	901	100	111	210	200		2000	3	200
															316	210	2130	2016	3020	3100

TABLE IV 22. FUEL CONCENTRATIONS IN PPM

Test 22 Conditions: Fuel - JP-4. Temperature - 77°F. R. H. - 65%. Sample Configuration No. 3. Four gallone JP-4 in spill at the center of the east wall. 12/14/71.

Time	-		,								Sempl	Sample Point	Numbers	Z										
THE STATE OF	-	1	-	1	•	•	-	•	•	의	=	21	2	=	<u> </u> =	2	=	<u>se</u>	61	20	12	22	23	2
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71	1300	90	300	200	200	200	200	1300	1900	1200	1800	_	0090		-	0000	0000	200	009	200	800	9	200	900
91	1400	400	300	300	300	300	300	1900	2200	1700	2300		9400			0000	000	200	0001	000	8	900	8	8
20	1500	200	400	400	300	300	300	909	2000	1700	0061	_	0400		-	0000	200		000	200	800	900	909	200
77	1500	909	900	00+	700	400	400	1500	2300	2100	2800		9700			000	7300	2000	0017	100	800	200	009	1100
82	1500	009	400	9	9	200	00+	1600	2200	2000	2500	_	0000			9200	200	00/5	0077	90	1700	100	909	1000
32	1500	909	200	200	700	200	00+	700	2000	1900	2300	_	9800				62.50	0000	0007	00,	0071	00	100	8
2	1500	009	200	200	700	909	400	1300	2100	2100	2700	_	0096			9800	3	3 5	2000	9 6	0091	002	200	8
9	1500	100	200	200	700	200	200	700	1900	1800	2100	_	9200			8500	4400	200	3300	3	9 6	90	100	8
\$	1500	700	909	009	700	200	200	800	1900	1800	2000	-	8200			7500	3700	200	2000	200	000	900	90	200
6	1400	100	909	9	909	9	200	800	2100	2400	2400	_	8700			000	2000	200	300	3	200	900	8	9
25	1400	28	009	909	700	900	200	1400	2100	2300	2600		8000			5800	9400	4000	2400	3 5	0000	000	00,	8
95	9	200	909	9	200	009	009	1200	2400	2400	2600	_	7700			4400	1000	4300	2200	000	200	3 6	200	900
09	90	8	8	9	8	909	909	1300	2300	2600	2900	_	6300			4400	1400	3600	2500	90	200	3 6	2 6	5 6
9	400	909	200	200	200	450	200	1500	2000	2300	2450	_	5550			13200	0020	3800	2100	200	2000	3 5	3 5	200
22	8	8	9	200	200	200	100	1900	2300	2500	2600	_	0009			12200	0050	3700	2000	9	1500	2	2 2 2	3 6
2	0071	909	200	9	200	009	200	1900	2300	2600	2800	_	4700			11500	10100	3800	2200	000	2200	5 6	3 5	3 5
	0071	90	009	009	9	009	100	1800	2200	2500	2800		5800			11400	9600	3900	2200	800	1900	8	3 3	3 5
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100	1200	200	200	200	9 6	2 6	3 5	200	2100	0077	2000		4900			10700	8500	3500	2300	0001	1900	006	800	700
\$	1200	100	200	200	2 6	2 5	3 2	3 5	200	0077	2400		2100			10500	8800	3700	2200	900	1800	1 000	800	100
108	1300	800	100	200	200	800	2	1400	1800	200	2400		0000			0000	8100	3500	2200	1000	2500	900	800	100
112	1300	800	800	800	800	200	100	1500	1900	2000	2400		200			0080	0018	3400	2000	000	1700	1000	900	200
911	1300	800	800	800	800	200	100	1200	1700	1900	2100		5500			0000	0000	2200	0017	006	200	000	800	2
120	1300	800	800	800	800	100	200	900	1600	1700	1700	_	5500			00200	8900	27.00		200	0071	0001	906	8
124	1300	006	800	800	800	800	100	800	1600	1500	1400	_	5700			00901	0006	2600	006	200	128		3 6	8 8
871	1300	906	800	800	800	800	100	800	1500	1500	1100	_	2500			10800	9400	2400	1600	001	1200	200	200	3 5
091	909	200	200	200	400	400	400	400	009	009	400	_	200			4000	1600	200	909	400	400	200		3 5
761	200	9	0	300	200	200	300	300	200	800	90		009			3500	2300	200	009	400	300	400	400	2 2
*27	000	200	900	200	200	300	300	300	200	009	400	_	200			2900	1800	400	200	400	300	300	300	200
200	3 8	3 6	3 5	3 6	200	250	300	300	200	900	200		300			2900	1500	400	200	400	00+	9	400	300
324	3 5	3 6	9 9	200	200	200	90	300	009	800	200	_	300			2500	1000	400	200	400	00+	400	400	200
	3	20	•	3	200	200	200	300	200	200	400	_	300			1800	100	00	200	400	300	00	004	200

The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 10 sec (e.g., Sample Point No. 2 is 20 sec, Sample Point No. 20 is 200 sec).

TABLE IV-23 FUEL CONCENTRATIONS IN PPM

Test 23 Conditions: Fuel - JP-4 Temperature - 62°F R.H. - 65%. Sample Configuration No. 4. Four gallons of JP-4 in spill at the center of the east wall to coordinate Configuration No. 3 with No. 4. 12/16/71.

	77		2600	4400	1200	4400	00++1	1300	00201	8400	2600	6400	5800	4400	4100	5700	3250	3600	3050	2400	2350	2150	0061	1800	800	900	800	750	650
	23		4300	8300	1900	8300	1900	6700	4600	2500	2300	1400	1800	1300	1200	1800	1350	1450	1200	1100	1000	906	009	100	750	800	800	750	059
	22		3300	2600	0009	6500	2100	3800	2200	1900	1600	1100	1300	00	1000	1300	80°C	1150	950	200	150	200	200	650	750	820	750	200	650
	=		200	700	2 300	2000	1700	1500	1400	1200	1100	000	900	800	800	006	9	200	750	550	100	200	009	00/	150	800	800	200	650
	2	6	200	0001	2	001	8	1200	1200	00	000	000	000	900	800	800	009	00	059	009	00/	200	650	00 ;	150	800	800	200	650
	9	,	200	0011	200	006	0001	00 !	1000	200	000	1000	006	008	800	900	009	650	750	059	3	750	0.00	200	05/	006	800	100	2 6
	2	0.76	2 6	9 5	007	004	000	0001	0001	0001	0001	0011	0001	0001	000	006	000	000	750	150	200	00,	2,50	200	200	850	200	750	9 6
	=	•		200	9 9	000	200	006	0001	000	2001	0071	9 5	3 5	0011	0007	000	064	920	3 5	0 0 0	9 5	0 2	2 2	2 6	920	820	750	25.00
	9	9		1700	200	9	000	0001	000	000	200	200	200	3 5	961	001	000	0.00	900	ָרָרֶרָּ סייר	200	36.0	750	2 4	000	020	920	05/	250
	2	400		120	2	000	000	000	300	1300	200	2007	1001	3 6		000	1 000	00.0	000	200	2 0	0.00	200	2 2	2 6	000	000	0 0	550
	=	100	40	300	000	000	200	0001	2 2	2 2	200	1200	200	2 6		260	7 20	2 2	750	2 6	2 2	750	750	75.0	200	8 6	2 5	00,0	550
at Numbers		200	40	000	000	000	2 2	200	1200	1200	200	1100	000	200		200	2 2	000	2 6	3 6	2 4	750	750	750	9 6	2 6	2 6	2 5	\$50
Sample Point	2	400	400	800	006	000	2 2	200		1200		8 2	1000	1000	0001	200	750	7.0	2 5	2 6	750	700	750	750	000	000	0.00	7 20	550
E	=	200	400	9	900	000			000	1200	1100	9	1100	1000	000	200	200	20.	9	2002	200	20.0	750	750	6	9 6	7 6	700	550
	2	300	400	909	700	006	1000	9	100	1200	1100	1200	1100	1100	000	700	909	200	650	750	750	750	200	200	900	850	750	200	550
	٥	200	400	200	800	006	90	000	1100	1200	1200	1300	1100	1100	1 00	750	600	200	650	750	750	200	200	700	850	850	750	200	550
	20	200	200	700	1100	1200	0001	1000	1000	1100	1000	1300	1100	1200	1000	200	650	650	000	750	750	200	200	700	850	850	200	700	550
	-				_		_		_				_	_															550
	٥																											700	
	5																											700	
	*																											650	
	•							Ī																				9	
	7	3800	8700	11200	13200	13300	10500	8400	7100	4503	4000	2800	2600	2100	2300	1850	2050	1800	1650	1500	1400	1050	1100	700	850	800	700	650	200
	-	100	14900	16000	1400	15900	15300	15100	12400	10200																		700	
Line	Ē	0	٥	12	81	77	30	36	45	84	5.4	9	90	72	78	132	186	240	294	348	402	456	510	264	618	672	726	780	810

TABLE IV-24. FUEL CONCENTRATIONS IN PPM

Test 24 Conditions: Temperature - 45"-66"F. R.H. - 31-93%. Preliminary Run at Hangar 935 at Kelly AFB; six F-100 aircraft. 12/18/71 to 12/20/71.

	2		•	•	07	9		0	0	•	•	0	0	0	•	•	0	c
	23		•	> ;	07	91		•	0	c	•	•	0	0	c	•	9	•
	77		•	9	07	0	•	>	0	•	•	>	•	0	c	•	>	c
	21		•		07	9	•	•	0	c			0	0	c		•	0
	20		•	•	9	2	•	•	•	•		•	>	0	0	•	•	0
	61		9	: :	63	30	•	•	0	c	•	•	>	0	0	•	•	0
	18		c	,		25	c	•	0	0	•	•		0	0	•	•	0
	12		c	, ,	9	30	c	•	0	0	c	•		-	0	c	•	0
	9]		•		2	07	•	•	9	0	c	•	•	7	0	c		0
	2		0	20	2	07	c	•	•	0	c			~		0		0
	=		٥	, ,	: :	07	0		•	0	c	•	• -	-	0	0	•	0
Sample Point Numbers	=			26		5	0	•	•	0	0		•	•	0	0	•	>
Polat	121		0	2			0	•	•	0	0	•	٠.	-	0	0	•	>
Sample	=		0	4	:	2	0	c	•	0	0	•	•	•	0	0	•	>
	2		0	40		07	0	c	•	0	0	0	•		0	0	•	>
	 •		0	30	:	-	0	c	•	•	0	0	-	,	-	0	•	•
	•		0	35		63	0	c		0	0	0	•		0	0	•	•
	-		ď	35		Ç	0	c	•	•	0	•	•		•	0	•	•
	9		0	35	36	Ç	0	c		0	0	0	-	. ,	0	0	•	>
	\$		•	25	26	63	0	c	•	0	0	0	c	•	0	0	•	•
	+			25	•					•	•	•	•	•	0	0	<	•
	-		0	07	26	9	0	0		•	0	0	c	•	•	0	•	•
	~		0	52	20	?	0	0	•	•	0	0	c	•	•	•	•	•
	- -		0	52	60	2	0	0		•	0	0	0		•	0	c	•
Time	ale)		•	3	112		202	300		5	116	1524	1932		200	2748	2780	

TABLE IV-25 FUEL CONCENTRATIONS IN PPM

Test 25 Conditions: Temperature - 47*-78*F R H - 31-100%. Run at Hangar 915 at Kelly AFB, eight F-100 aircraft. 12/22/71 to 12/27/71.

Time											Sample	Sample Point	North Pers											
min.	-l	~	-	*	5	۰	7	æ	•	07	=		 -	7				1				1		-
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	0	2	01	2	9	01	01	0	_	2	2	, 5	• •		> :	٠.	-	•	0	0	0	•	0	0
	~	~	ď	•	•				2 4	2 4	•	2 .	2 '	2 '	2	2	2	0	2	9	01	9	01	2
1512	100	•	~	•		· v						٠ 4	٠,	۰,	r	•	٠.	~	~	•	٠	~	~	M.
	13	=	13	13	13	=	2		` =	~ =	~ =	• =	٠:	^ :	٠:	.	.	٠,	·	~	~	s	~	8
	01	2	0	01	9	2	01	2	2	2	2	2 5	2 2	2 2	2 :	2 :	<u> </u>	<u> </u>	2	2	2	13	13	
	<u>*</u>	<u>*</u>	<u>+</u>	<u>+</u>	<u>*</u>	<u>*</u>	<u>*</u>	2	_	· <u>·</u>	2 4	2	2 4	2 :	2 :	2 :	2 :	2	0	2	9	0	01	2
	15	15	5	15	15	2	2		: 2	· ·	2	71	<u> </u>	.	: :	I :	± :	<u>*</u>	1.5	1.5		15	15	*
	61	61	61	61	6	•	0	0	2	2	9 0	2 5	2 5	<u>.</u>	<u>.</u>	2	~	<u>.</u>	-2	-2	2	15	91	15
	91	61	61	18	8	61	2	. =				2 0	9 -	9 :	07	07	20	07	50	07	70	20	20	20
	19	61	6	19	6	70	2.1	20			, ,	, ,	•	2 :	2 :	<u>-</u>	6	<u>-</u>	<u>-</u>	61	61	19	61	6
	23	23	23	23	23	23	23	2	2	3 5	; ;		2 :	9 5	2 :	2 ;	0 7	<u>~</u>	<u>•</u>	6	20	20	20	6
	61	61	61	80	90	6	5	2	2	3 =	0	5 -	5 -	3	\$?	5 5	53	53	23	23	23	23	23	23
	52	52	52	97	52	76	97	52	. 22	` ×				<u>.</u>	2 .	2 ;	<u>-</u>	<u>-</u>	<u>-</u>	61	•	61	61	5
	25	57	52	92	25	76	25	. ×	, ,	; ;	; ;	5 .	Ç ;	5	5	4 7	*2	*	* 2	52	52	52	25	52
	~	2	5	•	•			ì		2 5	3 4	Ç •	ζ,	9 ,	57	57	52	52	52	52	52	52	25	25
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FABLE IV-26 FUEL CONCENTRATIONS IN PPM

Test 26 Conditions: Temperature - 45*-69*F. R.H. - 37-93%. Run at Hangar No. 5 at Randolph Field with 23 T-38 aircraft. 12/30/71 to 1/2/72.

	2	0	-	•	, 5	: :	23	7	! !	•			7.	٥	•	• -			- 0
	52	o	-		• =	: 0	20	•	• =	•	ė		24		4				. 0
	2	0	-		•	=	70	•	0	•	•	•	23	0	•	٠ -			. 0
	2	۰	~		•	=	20	•	0	•	•	•	23	0	•				•
	02	0	•	•	•	=	20	•	10	•	•	•	23	•	•	-	-		0
	2	•	•	7	•	=	20	6	01	•	•	•	23	•	•	_	_		•
	=	•	•	•	•	Ξ	12	•	0	*	9	6	23	•	•	_	_	-	0
	-	0	m	7	•	Ξ	70	•	2	4	9	6	23	6	+	_	-	-	•
	9	0	•	7	•	Ξ	17	•	01	•	•	6	23	•	*	_	_	_	0
	15	0	•	7	6	:	77	2	2	*	9	6	97	9	4	-		_	0
E	*	0	•	+	60	=	23	0	01	+	9	6	23	=	+	-		-	0
Sample Point Numbers	=	0	•	~	12	<u>*</u>	23	9	01	*	•	•	92	01	*	-	-	-	•
. Point	21	0	•	د	60	=	71	2	9	+	•	•	23	2	*	-	-	-	•
Sempl	=	0	~	•	-	2	70	2	2	*	9	•	22	6	+	-	-	_	0
	2	0	•	*	7	0	20	01	01	•	9	•	22	•	4	-	-	-	•
	•	•	•	m	7	=	20	01	2	*	٠	•	22	0	•	-	_	_	•
	•	0	~	m	-	2	70	2	2	*	•	•	22	•	*	_	~		•
	- -	0	~	~	9	9	20	0	0.7	•	•	•	22	•	•	-	-	-	0
	 •	•	7	•	•	0	70	2	<u>°</u>	•	•	•	77	•	•	-	-	_	0
	~	•	7	7	~	01	02	•	0	*	9	•	77	6	+	-	-	-	0
	+	•	7	~	•	01	20	•	01	*	9	•	22	•	*	-	-	_	0
	-	•	~	~	ĸ	0	70	•	9	*	•	6	77	•	•	-	-	_	0
	7	•	~	~	•	01	6	•	<u>•</u>	•	9	6	77	•	•	_		_	•
	-	•	~	~	•	2	61	•	0	+	9	•	22	•	+	_	_	_	0
Time	(min)	•				156								1894	2686	2830	3838	3910	4198

TABLE IV-27 FUEL CONCENTRATIONS IN PPM
Test 27 Conditions: Fuel - JP-4. Temperature - 57°F. R.H. - 100%. RAFB. Special Sample Configuration No. 2. Fifty-three gallons of fuel spilled as indicated on drawing. 1/18/72.

Time									1		Sample		Numbere											
(min)	-	4	-	•	\ ا	۰	۲	•	•	의	2		1 '	51	91	12	61	61	07 6	17	22	23	\$2	
0	0	0	•	•	0	0	0	0	0	•	0					c								
• ;	Ç	38	280	330	09	1150	430	80	9	20	75													
* :	2	S#	40	01+	_	1580	059	175	100	9	80													
2 :	061	9	•	280		1980	1940	280	180	9	240										•			
9	027	52	1330	830	1300	2000	2000	059	235	110	110									780 12				
07	•	071	3 5	680	_	+0007	2000	009	270	155	330						·							
•	8 5	2 :	1560	1490		2000	2000	290	330	185	300												-	
97	2 :	017	1080	0751	_	7660	140	00+	280	150	350												•	
25	076	017	0007	1450	_	2200	1650	535	2	235	567													
9 9	240	077	1450	054	_	+0007	2000	260	380	522	405													
: 1	3	300	3 6	0011		1000	2000	064	940	042	200													
;	2	250	1740	0661	0450	+0007	10007	480	365	175	450													
25	9	72	1806	1860		2000	607	016	3 6	350	6.00													
98	099	270	1840	1860		2000	1370	410	200	25.0	200	044	200	575	345	335 2	275 3	350 2	295 34	345 190	315		5 570	
09	200	445	2000	1780		200	2 2 2	276	000	633	643													
3	570	160	1600	1300		2400	200	£ 6	200	622	380				-									
89	240	400	1880	1860		2000	95		067	007	900													
72	640	2	1860	1260		200	000		200	007	430													
: 4	200	420	2000	1040		1000	000	ŝ	313	240	415													
2 6	630	170	1680	1300		2000	9	365	200	300	460													
**	200	4	1580	1360		1045	3		200	627	480													
60	450	350	1510	1180		1400		276	643	200	9 20													
26	390	290	1140	1080		300		240	226	500	133													
*	350	280	1070	1140		1080	220	730	246	543	290													
100	355	250	1370	1300		140	70,5	245	240	245	140													
3	370	235	1350	1240		1500	1000	275	265	242	200													
108	370	225	1030	066		1430	840	240	246	225	300													
112	350	215	970	850	275	1070	740	240	240	225	275													
911	562	215	1020	870	270	1490	950	260	240	226	305													
120	320	205	780	190	325	1230	820	230	210	į	240													
124	290	190	730	089	250	1350	850	230	220	2 2	280													
128	270	210	970	810	245	730	486	20.	200	220	200													
**132	255	200	260	495	215	1080	619	186	301		276													
***136	592	210	480	455	720	1580	920	270	275	236	200													
140	370	250	875	835	540	200	480	230	245	275	365													
<u> </u>	355	305	490	490	315	415	150	220	250	250	300													
****148	275	356	410	450	290	440	305	9	220	200	230													
152	210	170	270	9	8	250	216	2 4	777	5 5	200													
481	1 60	125	200	23.6	2		653	6	6	200	2 :													
091440	2 2	3 8			200		2 :	25	9	521	571													
	2 0	3 6	2 :	2 .	2 2	661	0 :	۲ :	6	00 :	9			90	2									
	6	2	2	091	9	130	125	80	80	08	80			75	0							09		
200	35	30	09	65	30	09	09	35	30	30	30	30	30	30	30	30	5	52	52	35 2	25 25	5 25	52	
877	20	20	45	\$	\$2	45	45	20	20	20	20	20	20	20	20	20	02	2		,	96			
		ı											,	,								9	07	

Test 28 Conditions: Temperature - 46"-66"F. Field test at Bergatrom AFB with four RF-4 aircraft in Hangar 4534. 1/21/72 to 1/24/72. TABLE IV-28 FUEL CONCENTRATIONS IN PPM

Time		1	1		- {			ı			Semple	3	unbers										
mia	-	, ~	- -	•	<u>-</u>	•	~ '	•	-	기	-1 =	13	기	15	91	1	=	2	02	≂	22	23	*
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156	•	•	•	•	•	50	S	~	~	•	v	80	8		8	•	~	•	•	•	•	•	•
2	•	٠,	•	٠,	٠,	•	~ !	0 :	2	0	01	2	01	•	01 0	2	01	0	2	. 21	2	. 5	2
200	<u>.</u>	<u>.</u>	2 4	2 •	<u>.</u>	<u>.</u>	2 •	2 4	5 '		2 '	9	2	01 01	0.	2	2	01	01	10	10	01	01
	•	h	•	n	n	n	^	n	n	•	^	^	•	~	.	•	₩.	i.	•	٠	•	80	₩.
240	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	•	0	•	•		•
372	9	01	2	2	01	2	2	91	0	01	01	01	01	01	•	2	91	2	9	9	9	2	9
720	91	2	20	01	91	9	01	01	01	2	01	01				9	9	9	9	9	9		•
732	2	2	\$2	51	2	2	07	51	01	01	01	0				2	2	2	2 2	2 9	9 9	2 2	2 5
1	2 :	2 :	52	2 :	2 :	2 :	50	2 :	9	0 9	2	2	2	10 10	0 10	2	2	2	2	2	2	2	2 2
Ē	2	2	9	C	2	2	S	5	2	0	9	0				2	0	9	9	01	2	2	01
3	2	2	2	51	2	2	50	15	01	9	91	01	10	1 01		2	01	10	01	0	9	10	01
	2 :	2 :	52	2	2	2	20	2	2	2	2	01	01	- 01		2	2	2	2	9	2	9	2
	2 :	3 :	ş ;	5 :	2 :	2 :	2 ;	2 :	2	2	2	2	9	- 01	01 01	-	2	9	2	01	2	2	9
	2 :	2 5	9 :	2 :	2 :	2 :	07	<u>.</u>	2 :	2	2 :	2	2	- 01		2	9	0.0	9	2	9	2	0.
7 4	2	2 5	<u>.</u> ×	<u></u>	2 5	2 5	2 %	<u>.</u>	9 9	2 :	2 :	2 :	2 :	0 :		2	2	2	9	0	01	0	9
8.76	2 9	2 9	: :	2 2	2 9	2 5	3 4	2 4	2 5	2 5	2 5	2 5	2 :	0 :		2 :	2	2	2	0	01	2	2
=	2	2	2	2	9	9	20	2	2 0	2 9	2 5	2 5	2 5	2 9		2 9	2 9	2 ∶	2 :	2 :	2	2	2
									2	1	:	:	2	-		2	2	2	2	<u> </u>	0	0	0
\$	2	2	2	01	01	9	52	15	0	2	2	01	01				2	01	10	0.	9	0	9
900	2	2	2	2	0	2	20	2	0	2	2	0	10				2	2	9	01	9	2	2 9
0201	2 :	2 :	2 :	<u> </u>	9	2	70	<u>S</u>	2	0	0	0	01				9	0	2	01	2	9	2
707	2 9	2 :	2 :	2 :	2 :	2 :	S :	<u>s</u> :	2 :	2 :	2	2	01				2	2	0	2	9	0	2
	2 :	2 :	2 ;	2 :	2 :	9 :	\$	2 :	2	2	2	2	2				2	9	0	10	9	0	2
950	2 :	2 :	9:	2 :	2 :	2 :	\$	02	<u>~</u>	2	2	2	2	2	01	2	10	2	2	01	01	10	2
8 9	2 :	2 :	<u>.</u>	2 :	2 :	2	9	52	2	~	2	9	01				2	2	01	2	01	0	0
8	2	2	2	0	2	0	ġ	\$2	2	2	2	2	9				10	01	9	01	0	10	01
9111	9	10	15	10	10	9	100	52	15	15	01	01					2	9	2	5	5		5
1128	2	9	15	2	9	15		35	9	52	15	01					2	2	2	2 2	2 5	2 5	2 5
1140	2 :	2	25	07	2	2		2	70	20	2	01					2	0	0	2	9	2	2 9
2511	2 :	2 :	07	<u>s</u> :	2	15		8	2	52	15	15					0.	2	0	2	5	2	2 2
72	<u>.</u>	<u>.</u>	2 4	07	07	07		8	0 :	\$;	5 2	2 :					0	10	0.1	9	15	15	2
	2	=	į	9 9		2 0		3 5	£ 5	9	07	07					2	2	2	15	-	12	2
1290	2	2	9	20				300		2 20	2 -	<u>.</u>					٠ 2	<u>°</u>	2 '	2	2	9	9
1212	2	0.	35	20	2	2		400	2 5	2 5	2 =						•	•	· :	2 :	2	2	2
1224	15	15	Š	07	20	150		200	9	30	: <u>*</u>	: <u>:</u>					2 5	2 5	2 9	2 :	2 :	2	- 12
1236	20	15	\$	52	20	15		570	2	\$8	20	20	2 2	15	15 15	2 2	2 5	2 4	2 4	2 4	2 :	2 :	٠ :
1248	15	15	135	30	20	07		4 05	115	45	20	20					2	10	2	2 2	2 2		2 5
1260	70	15	2	35	35	70		245	9	9	02	20					2	15	2	2	5		3 =
7171	07	2	9	20	07	70		355	20	35	50	20					12	15	15	15	15	20	50

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).

TABLE IV-28 FUEL CONCENTRATIONS IN PPM (Cont'd)
Test 26 Conditions: Temperature - 46" - 66"F. Field test at Bergetrom AFB with four RF-4 aircraft in Hangar 4534. 1/21/72 to 1/24/72.

	1296	<u> </u>	955	*	3 E	ž š	2424	75.77	27%	2928	3	355	3216 15 15 15 15 15 25 3696 5 5 5 5 10 The time shown corresponds to Sample Point No.	
-	00000	22 2	***	2 :	222		22	S: 02	02	. S	<u>s</u> •	. 2 2	2	
~	22222	57 0	52 52	2 :	222	2 2	22	S S:	07	2 2 3	2 4	~ ~ 9	15 5 1 corre	
~	22222	8 5 5	2 % %	s :	2 2 2	2 2	35	s :	120	215	02	vvõ	25 s	
•	2222	* * *	2 2 2	2	222	2 2	25	2 \$	\$	30 55	z ,	0	15 5 5 8mm]	
~	00000	22 2	2 2 2	5	222	9 9	22	21 0K	70	2 0	5 ·	5	15 5 ble Poin	
•	25 25 25 25 25 25 25 25 25 25 25 25 25 2	20 20 20	25 25 25	2	222	2 2	9 9	15	70	2 2	\$2	25 S 26 S 26 S 27 S 28 S 28 S 28 S 28 S 28 S 28 S 28 S 28	25 10 10 10 10 10	
-	740 1900 145 1000	1000	2 . 2	350	2 % %	315	50 375	592	1000	966	2	32 52	30 15 1. Each	
•	220 290 385 290 290	450 260 930	275 360 145	0	5 6 5	\$£	15	135	205	505	8	S	100- 60 60	•
•	46 55 57 57	071 85 120	36 35 35	20	2 2 2	2 2	3.5	2 9	150	25 211	20	998	30 15 point b	
0	\$ 2 2 5 5 5	35 59	50 20 20	2	2 2 2	0 0	15	\$ \$	\$	\$ 0	51	* * 2	15 10 10	
=	70 70 70 70 70 70 70	25 25 25 25	222	9	0 ° 0	o o	10	20	02	35	2	~ ~ Z	30 15 10 15 10 10 point beyond No. 1 is	
2	20 20 20 20 20 20 20	25 125 25	222	2	5 ~ 5	2 2	5 5	15	2 2	25	2	222		
=	20 20 115 115	07 07	222	9	5 ° 5	9 9	0 5	2. X	. 02	30	01	222	10 10 10 5 5 5 99aced 30 acc (e.g.	1
=	2222	20 15 20	000	9	o	2 2	2 2	ž ž	20	30	91	999	- 1	
51	22222	15 20	2 2 9	<u>e</u>	ö 2 ö	2 2	9 9	51 5	20	20	9	222	10 10 5 5 Semale Point No	
9	22222	5 5 5	222	01	0 ° 0	2 2	22	21	2 2	20	01	9 9 9	10 2 2	-
-	22222	z z z	222	2	23 ~ 0	2 2	22	2 3	12	51	0	222	01 2	:
=	22222	5 2 5	000	9	2 ° 0	2 2	2 2	2 :	z z	20	01	222	o	
2	55555	22 2	222	0	\$\$ ° 01	01 01	20	٤ :	. z	20	<u>o</u>	222	10 5	and un
02		21 22 23	222	9	~ ~ <u>0</u>	0 0	22	2 :	2 2	20	9	5 <u>5</u>	01 %	Sample Fount No. 20 ts 500 sec).
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2		51 51		15	0 ° 0	9 9			12 12	30	15	22	ō v	200 000
23		36 35		15	222	0 9			35 2	25 3	15	005	<u>.</u>	÷
2	20 20 20 115 115	0 4 5	ត គ.គ.គ.	5	200	2 2	2 2 2	2	15	30	5	000	io e	

TABLE IV 29. FUEL VAPOR CONCENTRATIONS IN PPM

Test 29 Conditions: Fuel - avgae. Temperature - 69°F. R.H. - 55%. Sample Configuration No. 4. Four gallons of avgae in a spill at the center of the east wall. 2/14/72.

10 11 12 13 14 15 16 17 18
500 100 200 1000 1400 2800 1800 1001 0011 0011 0001 000 1000 001 005
8600 7700 4500 3300 2100 800 600 400 400 400 400 400 400 400 400
11500 0200 6400 400 400 400 400 400 400 600 700
115/00 9220 6409 4100 2500 1600 800 600 400 400 400 400 800 900
10.400 0000 7100 0000 0000 0000 0000
0001 0007 0000 0070 0011 0000 0001
0067 0066 0076 0017 0000 00001
DONE DONE DONE
10500 9200 6400
11500 9200
100 500 100 200 16000 8600 7700 4500 16900 11500 9200 6400
9 9 9 9 9 3 1 3
005 001 0098 00091 0091 00691
9999
100
022

FABLE IV 30. FUEL VAPOR CONCENTRATIONS IN PPM

Test 30 Conditions: Fuel - avgas. Temperature - 82°F. R. H. - 43%. Sample Configuration No. 3. Four-gallon spill with floor fan operating part time to simulate draft under hangar unor

	77	8	- - - -	000	000	5	Š	ž.	9	250	Š	Š	350	926			300	200	000	9	200	96	200	9	326	250	7.75	250	275	275	250	250	300	535	200	200	200	200	175		7.5	75	C	0
	=		000	956	000	9 6	200	1350	1450	000	1450	1650	1500	1350	000	000	200		0661	1460	200	200	9	1826	1725	1825	1750	1725	1625	1575	1550	1500	1450	1425	976	1075	1050	1050	1000		200	675	679	3
	2	3	200	000	200		2	2 :	1250	3	0571	1350	1350	2	200	900	200	200	000	1450	2 5	1400	000	1775	1725	1775	1750	1125	1650	1650	1475	1500	1475	35	1200	1250	1175	1200	950		200	675	0	10
	17	1	2	0002	2000	0634	0000	0000	3550	0517	2000	2	0071	200	200	200	200	200	294	1450	350	1450	9	659	1675	1825	1600	1500	1575	1425	1425	1525	0571	1200	1250	1400	1325	1400	1375	į	2	527		01
	2	9	300	0067	200	26.60	2000	06.76	0440	2000	000	0656	0067	0697	2600	2450	2200	2150	1750	1750	1440	005	1850	1775	2125	2050	1975	2050	1900	1800	1850	1925	6791	1575	1375	1375	1325	1175	1100	;	6/0	700	3	٥
	2		200	0557	0000	7900	9 5 5	200	0690	9066	2000	0010	900	4100	3650	3200	3000	2850	1850	2150	2100	2350	0061	1825	2175	2250	2350	2375	1875	2275	2375	2400	6262	1675	1650	1825	1400	1750	1050	. 5	0 00	9 6	1	15
	=	3360	0627	2600	200	2300	200	2007	2040	2000	0000	2550	3550	2850	2000	2200	2050	2000	2000	1650	1450	1350	0061	1750	1750	1800	1675	1500	1650	1575	1475	1650	1300	1600	1400	1675	1700	2050	1325	000	736	200		30
	-	. 0000		7950	200	2 2 2 2 2	2000	4550	0000	2000	2000	200	2460	260	2100	1350	0596	0016	7950	7300	470C	6200	2000	3175	4475	1950	4825	5350	5175	2050	5750	5355	5276	5275	4875	2000	4950	2000	4650	376		050		•
	91	-	٠.	1 10000	_			-		•	-	-		_	_	_																								3.5	22.6	225		30
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	2		•	20000	_	_	_	_			_		٠-	_		_	_	_	_																					6.3	; 3	9		_
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nt Num	=	_		17850	_	_	_	_	_	_	_		_	_	_																									100	700	700		Q
Sample Point Numbers	2	650	2000	6700	9400	7 300	5 100	3950	4350	2450	3350	1800	1300	1450	1400	1400	1300	1250	1200	1150	1250	1150	1850	1650	1650	1675	1575	1475	1500	1425	1300	1250	1175	10.5	10.0	1025	9	6.5	050	675	h50	4.75		45
Sam	=	350	ROOM	6650	7050	5400	4800	4550	3450	3450	4600	3350	2050	2550	2050	2300	2050	1500	1500	1400	1350	1350	1850	1725	1650	1875	1700	9	1525	1525	1373	1250	1200	1150	1125	100	1075	1050	1025	650	650	675		ß
	2	200	4900	7250	7650	7350	6750	6100	5350	4750	3450	4000	3000	1500	1750	1550	1550	1300	1250	1200	2100	1000	1850	9	1700	1650	1625	1550	5241	1475	1300	1250	1200	1100	1025	1050	1025	975	975	650	650	650		9
	7	2	850	2850	5205	5500	5100	4000	2500	1350	1250	1300	1300	1350	1400	1400	1350	1350	1250	1250	1800	100	1850	1750	1650	1675	1675	1625	250	1400	1275	1300	1225	1150	2	100	1050	1025	0001	675	675	675		55
	•		450	_	~	~	.,	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	_	1825	_				-	_	_	_					_		675			. 22
ı	-	100	250	850	_	~	~	_	-	_	_		-	_	_	_	_	_	_	_	_	_	_	_	_				-	-		_	_				_				675			
	اه	20	340			550													-							1450															675			2
	~			000									-	_	_		_		•																					725	675	675		2
	+	0	300	220	3	700	950	900	1200	1200	1200	1 500	1350	200	200	00	1350	1300	1200	1250	000	200	1700	1775	1775	1675	200	1630	1525	1500	1350	1300	1200	950	200	0601	1076			725	200	675	:	2
	-	0	300	9	100	820	1000	150	1200	1250	1250	1300	1500	1550	20	22	200	9	1150	9	200	450	0001	1325	25.	000		1300	1325	1175	1100	1125	1100	1025	713	200	200	200	2	725	200	675	:	2
	~	0	900	100	90	000	200	1300	1350	1450	400	1500	15%	1650	9	1700	1550	250	320	2	2 .		0671	6761	6761	3		1475	1500	1400	1300	1300	1225	211	2 :	3 5	1078	2		725	200	675	:	۽ ۽
	-	0	100	1050	2	1400	200	1550	3	3	1550	1750	1700	100	200	920	100	9	0061		200	200	0011		6761	1350	1360	1425	200	1300	1200	1225	1175	1160		3 5	1050	1075		725	100	675	•	^
-	alm.	•	2	2	9	9	3 1	7.	=	96	801	120	1 32	=	156	3	9	761	*07	917	977	200	767	*97	9 6	300	200	324	336	346	360	372	384	404	624		1	454		576	200	004	-01	:

*The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).
**Entered room to set up fan.
**Entered on.

TABLE IV-31 FUEL VAPOR CONCENTRATIONS IN PPM

Test 31 Conditions: Fuel - JP-4. Temperature - 89°F. R.H. - 28%. Sample Configuration No. 3. Four-gallon spill with floor fan operating part time to simulate draft under hanger door.

Time											Sample	le Po	Point Numbers	nbers										
(min.	-	~	-	+	~	•	-		6	의	=1	2]	=1	<u> </u>	15	2	17	=	6]	2	[2]	22	23	2
•	0	0	0	0	0	0	0	٥	0	٥	0	0	0	٥	0	c	c	•	•	•	•	•	•	•
12	100	S	3	100	75	8	200	9	200	200	001	20	400	2150	3500	9	8	376	9	300	2	9	9	9
54	200	901	100	200	3	175	125	150	450	325	175	100	150	4925	7175	9	000	176	300	677	2 2	200	6/2	2
36	225	125	100	200	150	150	150	150	275	522	125	250	000	3725	7400	8675	2450	350	16.3	275	200	577	275	2 3
9	200	<u>S</u>	001	150	125	125	125	125	350	300	150	125	200	2975	5055	7875	2250	275	325	225	222	28	250	3
3 :	200	125	2	20	150	8	125	125	350	200	125	125	300	2825	4325	6075	1800	300	300	275	200	175	225	
21	7	3	ie i	320	125	125	125	100	700	200	001	100	522	1775	3650	4725	2800	250	250	200	150	125	25	2
3 3	2	8	75	75	75	2	125	75	3	577	00	75	200	1425	3400	4900	1375	057	300	200	175	125	175	125
9	175	00 1	12	8	2	S	8	100	571	125	20	125	75	1275	3000	4300	1550	952	250	175	150	125	125	00
90	2 :	2 :	75	8	75	S	8	15	175	15	75	001	150	1050	2950	3925	1625	225	325	175	150	125	125	125
071	2 :	2	2	7.5	2	8	00	75	172	125	15	75	75	950	2500	3700	1650	175	275	175	125	8	100	9
26.1	571	2 :	15	15	20	3	20	20	125	00	75	75	75	775	2075	3175	1125	150	225	150	100	75	90	100
	571	2	001	125	2	8	20	8	15	001	52	52	2	200	2075	2750	1200	125	125	125	225	200	95	75
156	15	8	8	2	250	522	25	300	300	300	325	325	475	325	575	9	9	400	475	450	375	375	350	25
2	57	2	8	575	320	320	350	375	375	375	375	400	550	375	550	575	200	475	425	400	400	425	425	2
	577	175	150	325	275	320	320	350	350	300	250	225	522	200	150	1850	9	350	400	350	325	225	275	7.5
261	3 :	2 :	571	512	250	275	577	300	275	200	250	175	175	200	1025	2125	675	275	300	275	250	200	200	2
107	2	57	9	175	200	20	577	572	200	120	150	125	125	125	850	2375	850	200	350	200	175	150	175	7
917	061	001	00	125	8	8	200	175	5 00	522	125	125	001	175	675	2325	725	175	512	200	150	125	125	2
288	125	75	75	42	20	\$0	150	7.5	100	125	75	25	75	75	450	2325	575	125	275	150	100	75	001	75
432	200	175	175	1 50	150	150	150	150	150	051	150	150	150	125	000	1525	450	175	250	175	150	25	175	75
916	275	275	275	275	275	275	325	275	300	300	300	300	375	300	350	400	325	325	375	375	325	325	325	S
720	250	250	275	275	275	275	275	275	275	152	275	275	275	275	275	300	325	300	300	300	300	300	300	20
1104	150	175	175	175	175	178	175	175	175	175	175	175	175	175	175	175	175	175	175	175	175	175	175	٥

*The time shown corresponds to Sample Point No. 1. Each Sample Point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 2 is 60 sec).

**Fan on (156 min).

**Fan of (174 min).

Test 32 Conditions: Fuel - avgas. Temperature - 90°F, R. H. - 40%. Sample Configuration No. 3. Four-gallon drip test with floor fan operating partime to simulate draft under hangar door.

Time

1											SE SE	Semple Polat Num	Number											
min	-	~	-	+	~	اء	;-	-	2	의	=	2		=	2	=	11	9	61	20	21	22	23	1
•	7.	ř		;	;																			
• :		C ;	0	S	2	00	2	8	1 50	300	425	250	4575	7300	9450	10000	1350	000			136	76.7		
71	4/3	200	350	300	3	275	3.50	800	1025	1750	1000	1950	100001	+		10000		200		75.	671	674	3	3
54	2	650	675	525	\$25	550	1 125	1425	1500	3075	1450	2676	3				-			_	_	_	_	2,40
36	1225	950	975	300	£23	750	2425	2125	1250	4275	2675	4676				-			_		_	075		919
9	1750	1325	1425	1225	1150	1100	4075	20	1875	2426	3775	0033		•					7125 5	•	2925 1	_	775	111
9	1650	1300	1300	1 300	1200	1150	37.00	3750	6300	40.50		2000	_ ′				_		_				187	956
7.2	1850	200	1450	1500	300	300	200	200	0066	000	200	6300		0000	20000+			_	Ĭ	_		_		600
46	1 900	1550	200	9		2 2			001	2 2	47.50	6350		20000+ 2		+	•	_		4 0527	6500 2			000
ŧ	1900	9	40	1460	360	3	300	2000	0663	9	2400	0569		20000+ 2				_	•	_				900
-	8	9	200	000	0000	000	7	C.	5	7800	2750	5550			20000+ 2		200001 7		•	Ī				000
200	3	200	900	0000	30	1350	2200	4450	6800	6700	5500	9089			3 +0000:	20000+ 2		_	•					200
2	3	000	2	1450	1400	1400	5750	5550	6350	9579	9500	5750			* +0000				•			•		
761	3	0051	1450	3	140	1800	2400	200	6100	9190	5500	\$700			20000+ 2		70000+							3
*	900	1350	1200	1360	1400	303	5150	2400	5850	6150	4750	5550	18450 2	200004 2	20000+ 2	0000		200	001					8
156	28	1450	1350	3000	2750	3450	2:00	5100	5750	5200	5 300	2500					10000			-				8
108	906	1550	1+50	540	0017	47.00	5.00	100	2400	0	000	0000			200002	20000	_	_	Ī		•	_	_	000
180	2100	1700	1650	4600	54	47.60	0 4 3 5	000	200	0000	0000	0040	_		+00000			_	_	•	-			006
8	8	1760	200	200	2000	00.00	100	3	4420	2000	4500	4800	_		20000+ 2	_	6 00891		5700 5		_			9
2	3 5	2	000	00+	3800	4750	000+	3800	4800	2150	3650	4100	_		7 +0000	_	•		_					2
107	2400	2000	1850	4000	1250	4200	\$650	4200	4800	2000	4000	4300	13650 1	7500 2	20000+ 2	200004				2000		0000	064	220
216	2600	2250	2250	0000	3	4200	4450	3300	1600	4900	3750	4150			0000						•			8 20
977	2900	2600	2500	3400	3900	3900	1050	1160	4550	6003	2000	2000	•	•	-	_	•	_	_	-	•			800
240	3500	2900	2500	2500	2800	1700	2000	0000	000	2000	90	4500	13130	1 0534	•	Ξ	-	_	_	·	Ĭ	·		800
252	3500	3050	3000	0000	2007	00/5	2000	3400	4040	4550	3600	3900	12400 1	16330 1	18300	1 98 50 1	-		_					250
3,5	200	000	3	2010	2 400	3 300	25.50	7650	4200	4500	3700	4350	1:540 1	1 050+1	17350	00161	3800 4	1750						9 6
107	2015	2100	3	2000	0407	3100	300	2850	40 20	000	3150	3200	9100	12750	3800	15600	•	1850	3350 3		0000			3 5
9/7	2000	2000	3000	3000	2600	2800	2000	00t ~	2800	2400	2500	2700	5950	10450	1 400	12950	•	150		• •				000
288	2450	2700	2700	2400	2600	7500	2300	2050	2500	2350	2100	7350	6700	24.60	0.00	0001	٠,		000	•	•			220
											3	2	2	200	00+01	0081	7450 2	220	~	2 0062	2300	2 009		200
420	249	950	545	940	5_5	0.70	510	465	575	555	140	545	600	9	326			3						
** 432	475	585	535	550	900	650	054	675	448	034	36.7	207	2 6	0 0	613		001	65	635	929	605	260	0.30	135
+++	240	260	260	5.7	6.40	640	9	450	4.45	000			600	-	930	665	595	490	565	605	540	590	019	9
959 ***	525	540	240	4	404	9			610	200	000	040	69	, 20	802	155	410	425	575	585	555	580	51.5	75
10.0	465	475	000	000				600	200	200	3	290	635	675	730	635	290	400	400	490	510	405	015	4
007	2 4	17.5	9,4	026	666	533	555	555	530	230	545	535	585	619	645	909	450	365	445	495	014	475	084	3
492	375	395	385	4	64	44	460	413	410	465	475	465	515	5+5	555	545	435	415	435	435	405	435	425	3 3
				,	!	:	,	2	1	201	2	402	÷87	064	630	290	091	150	585	9	245	365	445	
916	145	165	155	160	150	170	180	185	091	091	140	4	501	183	665	245	36	011	105	105		145	9	35
720	4	37	ŕ		,	i	;												;	;	,	2	2	ĵ
<u> </u>	ò	C D	5	2	0	0	105	001	51	501	105	95	9	80	175	95	65	8	65	7.5	95	80	80	5
8001	75	2	9	98	92	89	88	Ç	\$6	96	88	8.5	88	96	155	8	20	85	75	89	8	88	88	5
1404	9	9	69	6.5	6.5	6.5	50	9	9	69	59	5.6	4	4	9	76	•	;	;		5			
		Į										;	3	;	3	2	?	0	Ç	ç	ç	65	9	12

oThe time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).

TABLE IV-33. FUEL VAPOR CONCENTRATIONS IN PPM

Test 33 Conditions: Fuel - JP-4. Temperature - 85 *F. R. H. - 48%. Sample Configuration No. 3. Four-gallon drip test with floor fan operating part time to simulate draft under hangar door,

Sample Polat Numbers 5 6 7 8 9 10 11 12 12 13	23 24									Ī												-			. •		•								375 200
3 4 5 6 7 R 9 10 11 12 12 12 12 12	22	9	200	007	000	1000	300	1300	1100	1100	1000	ŝ	1000	1950	2300	1950	1600	1600	1500	1500	1400	1200	1000	1000	850	750	200	650	009	575	9	575	575	525	200
3 4 5 6 7 R 9 10 11 12 12 14 16 15	7	900	3 6	2	200	900	3100	2500	9	1200	100	200	1100	2000	2275	2250	1800	1500	1700	1500	1100	1000	1000	900	750	200	200	550	9	550	525	525	9	200	400
3 4 5 6 7 8 9 10 11 12 14 15 15	27	900	200			2960	4300	3700	2200	2200	1200	1100	309	2000	2250	2250	1800	1850	1700	1400	1600	1100	1000	1000	90	150	850	625	625	725	625	550	525	200	450
3 4 5 6 7 8 9 10 11 12 12 14 15	6	9001	900	200	2000	4200	2500	2400	2600	5600	1800	1300	2100	2000	2250	2400	2100	2450	2400	2000	1800	1400	1200	1300	950	900	950	675	750	775	775	009	725	525	550
3 4 5 6 7 8 9 10 11 12 12 14 15	=	90	9			2100	390	4500	3300	2100	1500	1300	1700	2000	2275	2300	1900	1550	2400	1600	1300	1100	1000	9	750	150	100	0	725	900	9	625	650	575	550
3 4 5 6 7 8 9 10 11 12 13 14 15	=	1000	7400		200	14300	15400	16400	14600	12400	8200	8300	9300	2300	2450	4600	5850	5550	8300	6800	6700	5300	3600	4000	2500	3000	2600	2750	1800	2150	1925	2075	1750	1950	1525
3 4 5 6 7 R 9 10 11 12 13 14	9	4.800	0000	14000	000	000	19500	+00002	19000	17800	13000	12800	13000	2600	2450	6700	8350	0096	11000	10300	10400	8600	2000	6700	2100	4550	3900	3450	3475	3300	3075	2700	2500	2300	2125
3 4 5 6 7 A 9 10 11 12 13 13	2	4800	0008	2600	200	200	17400	+00007	17500	18400	11500	11500	12000	2800	2640	7300	7850	9350	10600	10000	0096	7400	6300	2000	3300	3800	3100	2425	2575	2475	1950	1700	1950	1625	1450
3 4 5 6 7 8 9 10	=	1800	7400	12000	200	200	10800	00071	00491	15300	9100	9700	1000	3000	5625	3000	5300	0569	8350	7400	1900	2000	3900	3200	006	1 700	1 20	1000	90	750	700	575	550	455	400
3 4 5 6 7 8 9 10	=	2600	2600	8700	9091		00061	00141	00471	200	2500	2800	1500	3000	2975	2950	0000	5200	6250	2500	5300	3300	2500	2000	1150	1000	. 100	220	525	200	200	475	425	400	375
3 4 5 6 7 8 9 10	2	00	009	1000	2200		2000	2000	0071	200	200	0002	007	2100	3000	2075	1550	1300	9	1000	900	900	800	900	009	000	200	450	475	450	450	450	425	375	375
3 4 5 6 7 8 9	=	300	1100	1300	9	3600	0000	200	200	200	0001		000	0061	3050	2150	1850	1400	1850	1 500	1500	1100	0001	006	00.	920	650	200	200	200	200	475	455	90	00
3 4 5 6 7 8	2	300	100	1800	2800	300	000	0000	200	20077	3 6	300	0071	006	2225	2455	1900	1450	1200	1100	90	1200	1000	9	9	3	2	525	220	ŝ	725	920	200	200	00
3 4 5 6 7	-	100	200	006	9	2100	3 5	200	200	200	901	200	0001	006	2200	5450	2100	9	1300	1200	100	0001	1000	006	000	200	000	575	220	9	200	200	475	450	400
3 4 5	•	100	400	100	1200	2000	20071	200	3	2 2		000	0071	2200	3075	2200	1900	1650	1250	000	00	000	0001	200	2 5	000	000	200	200	200	200	200	425	425	320
3 4 5	-	200	300	700	1300	2100	2	200	300	200			000	0002	2250	2150	1700	1450	1200	000	000	0	008	000	2 5	8 9	000	3	100	200	200	200	475	425	450
-	•	100	200	000	009	000	2			3		2 6	200	2007	2200	5777	1550	1250	00	006	0001	006	900	9	1 6	2 5	200	626	420	200	50	420	425	575	2
-		001	700	00	9	800	8	9	8	9	90			200	2300	0577	1 700	1450	0571	1100	0071	1200	0011	3	750	2 4	200	000	2	575	676	475	450	000	20
1		100	200	00	9	000	9	ç	Ş	900	000	2		200	5217	0077	009	1450	200	0001	9071	0011	200	200	5 5	94	2 5	000	000	2	04	475	96	674	3
7	1	100	200	200	100	900	900	90	00	9	900	200	2 6	2	5771	008	1350	0011	2	900	2 5	002	3 5	2 7	9	3	36	200	2 1	5	200	060	200	2 5	0
-	·	100	200	Ş	200	000	9	1000	006	9	00	200	2 6		200	10/3	1 550	1150	2	000		007	5 5	3 7	9	450	2 5	200		213	3	27.5	350	36.5	2
_	\cdot	100	300	9	000	1000	1300	1300	1300	1200	1100	000	200		200	2002	1550	200	200	0001	200	900	200	2	9	9	450	424		676	200	000	200	25.0	200
		0	~	\$ 2	36	7	3	2	4	*	108	120	? ?	761		007	2	2 3	261	407	917	977	24.		276	288	902	200	316	476	2.50	940	3 2	305	

of The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 is spaced 30 sec (e.g., Sample Point No. 2 is 60 sec, Sample Point No. 20 is 600 sec).

TABLE IV-14 FUEL VAPOR CONCENTRATIONS IN PPM

1/6/72.
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ļ								Condiguration No.	į		of a series		gallens of avgas in a optil in the center of the east wall. 6/6/72.	-		6/6/72.								
(min)	-	-	-	-		1	-	•	•	0	=			2	2	ام	41	=	4	8	F	2	12	*
•	•	•	•	•	•	•	•	•	•		c	•	•	•	•	•	•	•	•	•	•			3
-	18, 400	12,800	9, 250	\$.5	3, 700	2, 400	3,000	. 30	1, 800	1. 450	1, 150	1, 300	1,200	2. 400	2.350	951		900	90, 300	2 200			3 1	
2	17,600	10,600	15, 900	14. 900	3.5	12, 600	11,500	10, 500	. 800	8,750	8, 100	6, 700	7, 100	7. 808			T 2				_			
£	16, 900	16, 400	15. 700	14. 900	14, 806	13, 200	12, 200	. 38	10, 680	9. 600	. 800	7. B00		į	_			9 _			. 100		_	
11	 	16, 300	15,600	14, 700	14,100	13, 100	12, 490	11, 600	10,800	10,000	. 000	9, 200	7, 700	e 100	8, 800			160				700	208	
:	16.30	19.10	15. 488	14, 600	13,800	: :	12, 100	11, 360	10,500	4, 500	9. 600	7, 800	7, 300	7. 800	9.40		-	532	2, 100	_				
•	16, 100	3.	15, 200	14, 500	13, 700	12. 400	12, 100	11, 200	10, 300	• 100	•. 100	6, 700	. 400	7, 100	9. 200		- 12	_		54	_			
23	13.	15, 700	15,000	14, 300	13, 400	12, 700	11,78	900	10.00	. 800	7, 900	9, 600	7, 680	7. 906	. 980						_		3, 100	
*	15, 200	14, 780	13, 400	12, 500	11,500	10, 600	9. 780	. 400	4, 100	7, 000	6.400	000 '9	5, 400	9, 400	5. 900		7, 800	8, 300	_	_	 8			14,20
*	15.1	14, 900	13. 400	12, 500	Xe	10, 300	:	7, 900	6. 700		5, 800	4.500	4.600	4. 700	5, 800	5, 500	6, 600	8. 8	9,500	909 '0	_			14,24
5	15, 800	¥. 5	13, 500	12, 700	8	10, 800	. 600	8, 500	2, 100	9, 800	9, 300	4, 600	. 690	. 600	4. 700	5. 000	9. 400	6. 300	7, 600	9, 200	909 '61		12, 800	13,70
2 1	14, 800	14, 030	12, 800	: 8	10, 606	9, 400	9.100	6, 600	9. 700	4, 600	4, 200	3, 500	3,600	3, 600	3, 600	4, 000	4, 500	5, 700	7, 400	9,300	9,0		5.9	13, 70
133	14, 780	13, 400	12, 800	1. 400	10, 700	9, 500	6, 200	6, 500	9, 600	4, 600	4.300	3,600	3, 700	3, 800	3, 900	4, 200	4, 700	9, 100	6. 700	8, 400	_			13, 20
Ē			12, 200	11, 300	10, 000	6. 700	6. 800	5, 300	4.600	3, 700	3, 700	3, 500	3,600	3, 700	3, 700	3, 800	3, 600	4, 900	5, 200	6.500	_			12. %
157	14, 300	13, 200	11, 700	10, 400		6. 905	2,400	4, 400	4, 200	3, 400	3,400	3,000	3, 200	3, 200	3, 300	3, 200	3, 600	3, 600	4, 700	6.000	7.	10, 100		12, 50
601	14,000	12, 700	11, 200	. 800	7,500	\$. 400	4. 200	3, 200	1, 100	2,600	2, 700	2, 500	2, 800	2, 400	2, 800	2, 500	3, 000	2, 800	3, 100	3, 100	3, 900			3.
•			. 400	9. 700	4, 300	2, 900	3,000	2, 300	2, 500	2.100	2, 300	2, 000	2, 300	2, 180	2, 480	2, 200	2, 500	2, 100	2, 900	2,500	4. 10s	9, 500		
Ē	13,200	10, 700	• 100	. 600	3, 800	2, 600	2, 680	2,200	2, 300	2, 800	2, 100	1, 900	2,000	. 900	2,000	. 30	2, 290	1. 900	2, 400	2, 200	3, 100	4,100		8
507		10,000	006 .4	• 000	3, 36	2, 300	2, 300	1, 900	7,100	1. 900	2,000	1, 400	1. 900	1.800	1, 900	. 80	1. **	. 800	2, 200	2, 100	3,000	4, 200	11.5	
217			6, 300	3, 500	3, 100	2, 100	2,100	. 800	1.800	. 700	1, 700	1, 400	1,600	1.600	1, 400	1, 500	1,600	1.400	908.	1.800	2,600	3, 400		8
•77	12, 200	6, 700	5, 700	3, 300	2, 400	1, 900	2,000	1,600	1.790	1,500	1.500	1, 400	1.400	1, 400	1,500	1, 48s	1, 500	1.300	1. 800	1, 500	2, 400	3,000	5, 700	\$
₹			4, 450	7.800	2,500	1, 700	. 80	1. 400	1.400	1.400	1.300	1, 200	1.400	1, 200	1,400	1, 200	1. 400	1, 200	1, 700	1, 300	2,300	2, 600	5, 000	7.7
187			4, 700	2, 500	2, 200	. 48	3.	1, 200	1,300	1, 300	1.100	1, 200	1.000	1, 600	1.000	1.000	1, 300	1,000	1, 400	000.	1, 900	2,000	4, 500	, ·
502			4. 100	7, 300	2, 100	1, 300	1,400	1, 000	1, 100	400	3.000	00	8	00	900	2	1, 100	808	1, 300	1,000	2, 000	2,300	6. 500	9.
273			4,100	7, 300	2, 18	1.300	1.400	1,000	1,000	800	8	8	8	8	904	ŧ	1.000	•	1, 300	1, 000	2,000	2, 200	*, 400	, ě
582			3, 800		1, 900	1. 18	1,300	ş	1.000	9	9	004	90	9	8	8	000.1	100	1,300	906	2,000	2, 200	6, 500	6.50
ē						200	1, 366	ş	906	8	9	99	1	2	9	ğ	. 980	004	. 300		1, 700	96.	3, 900	5,76
Ē	10,400	5, 300	3, 500	1, 800	1, 700	1.100	1, 200	90	1.000	908	00	8	900	00:	8	Ş	00	0′9	000	2	1, 706	1,600	9,60	5.10
Æ	ie time she	The time shown corresponds to Sample Point No. 1. Each sample point hey	ande to San	uple Point	- 2	ch sample ;	point bayer	end No. 1 to	s spaced 30 sec	•													ž.	;

TABLE IV 35. FUEL VAPOR CONCENTRATIONS IN PPM

-											Managele Polisi Permisere	Table 7.0											
	~	-	-	1	-	-	-	•	01	=	21	=	=	=	2	=	=	2	8	7	77	52	×
8, 700	907.90	3, 36	3, 500	1.100	904	:	90	8	8	500	8	861	90	8	8	8	300	3	1,500	5,780	. 500	906.	10. 9
12, 200	901 '01 00	4.00	7,500	9, 300	2.600		90	8	90+	907	300	00+	300	9	90	. 400	3, 100	5, 400	7,200	8, 400	9,500	10, 300	
11.9	10,506	4.00		7, 900	. 78	4. 900	3,200	2, 300	1.300	1, 300	8	906	8	1, 500	1, 900	3, 500	5. 000	7, 100	8, 200		9.80	9. 480	
11. 70	10,600	10.00	4. 400	8, 600	7, 880	•	4.900	3, 700	2.2%	1. 900	1.000	1,200	1, 100	2,300	2, 400	4. 900	6. 500	7,700	4, 500	9,200	9, 400	10, 500	=
11,600	10,600	10,100	9, 500	9. 800	B. 100	7,200	5, 800	4, 200	2,600	2,200	1,300	1,500	1, 500	2, 706	3, 300	\$.600	6. 800	7, 900	8,600	9, 300	9.700	10, 400	
11.500	10,600	10,000	4. 500	9. 800	9,100	7,500	6,500	. 000	4,000	3,400	2,200	2,400	2,700	4.100	5, 300	6.800	7, 500	9,300	8, 700	9,200	9,800	10, 200	.7
2.5	10,400	*.	9, 500	900	9.400	7, 900	7,200	6.teo	9, 300	4.500	3, 190	3,600	3, 700	9.800	6.390	7, 100	7, 700	8,300	B. 800	9,300	4,800	10, 100	10, 60
	10,300	9.90	9.500	9, 000	9.600	8,200	7,600	7,100	6,200	5,500	3, 900	3, 900	4, 400	5. 400	6,700	7, 300	7,900	9,500	908 1	9,300	9.800	10,180	10,60
11,200	10, 300	4, 900	9, 500	4,000	8.000		7,600	6. 900	000	\$.100	3, 400	3, 400	3, 400	5, 300	6,200	7,000	7,700	. 100	B. 800	9,200	10,100	10,100	10.50
11,200	10,300	9,900	4.500	9,000	9. 600	8, 100	7,600	6, 900	\$. 900	9, 100	3.500	3, 500	3, 900	5,200	6.100	7, 800	7,600	9,100	8, 700	9,200	9, 700	10, 100	10, 500
10, 800	56 10,800 10,000 9,400 9,200 8,400 8,300 7,860 7	4, 400	9.200	B. 400	9, 300	7, 800	7, 300	008.4	. 000	5, 400	4,480	4, 300	4,700	9, 800	6,300	7, 000	7,500	9,000	8,300	8.800	9.200	000	10.200

TABLE IV 36. FUEL VAPOR CONCENTRATIONS IN PPM

Test 36 Conditions: Fuel - argue. Temperature - 68 F R H - 96% Sample Configuration No. 4. Four gallons of argas in a spill in the center of the east wall 6/13/72.

There											Sample	Sample Patest Numbers	2											
(WIE)	-	4	-	•	-	•	-	2	•	2	=	2	2	=	-	4	12		9	97	17	77	17	2
•	11, 400	9. e00	6, 900	3,400	7,400	900	900	909	90	400	900	00+	005	\$ 000	30.	969	900	8	2,500	4, 200	7, 300	. 700	11. 300	12, 500
•	13, 800	11.000	10,500	9.000	7,500	5,000	3, 700	2, 100	1,900	1, 100	1, 100	900	900	800	1,400	1.400	2, 300	4.500	7, 900	8, 300	9,400	10, 700	11,680	12,680
•	13, 300	17, 100	11,000	10.100	8.900	7, 400	6.800	6, 400	4.000	2, 400	2,400	1.500	1.800	1.600	000.7	3,700	5, 700	6, 900	7, 900	8.400	. 700	10.800	11,600	12, 400
2	13,000	12,000	11,000	10, 300	9, 300	8.600	7,800	7,000	٨, 300	9, 100	4.400	3, 36,	3,400	1, 900	6, 000	5, 400	6.900	7,600	. +00	9.200	9, 400	10, 800	11,430	12,200
2	12, 900	11, 900	11, 100	10,400	. 500	8.900	8,100	7, 400	6, 400	9, 200	4.500	3,200	3, 500	3, 700	\$,000	6.000	7, 100	7, 300	8,800	9, 500	. 180	9.400	10,500	11,000
07	11,500	10,700	10, 100	9.500	9.800	9,300	7,700	7, 000	6, 400	5.500	4.900	3,400	3,600	4, 000	6,200	\$. 400	6. 400	7, 400	8,000	#, 400	9,100	9. 400	10,300	10, 800
*	11,500	10, 700	10,000	9.500	8, 900	8, 300	7,800	7,200	6, 700	9. 100	5.400	4, 300	4, 100	4, 400	000 '	6,300	7,000	7,500	8,000	N, 600	4, 100	9, 700	10, 300	10, 700
2	11.000	10,000	9,500	9.000	9, 400	7,900	7,400	004 '9	6,500	9. :00	9,000	5. 800	5.800	5,800	6. 100	6.300	6, 800	7,200	7, 800	8,200	009.	4,300	9. 800	10,200
;	11,000	10,000	9, 500	9.100	001 '0	7,700	7, 100	0 × 100	6,300	904.	9, 100	5.800	\$, 900	5, 400	., 300	4.400	7, 000	7,400	7,900	8, 300	9, 800	901.6	9. BOD	10,200
•	10, 400	10,000	9,500	000.	8.400	B, 100	7,400	7, 100	6, 700	6.400	6,200	8,800	6.400	5, 900	.,200	004.4	906 .9	7,200	7,800	4,200	. 100	9, 200	4,600	9, 000
ŧ	time show	n correspo	nade to Sam	The time sheen corresponds to Sample Peint No. 1. Each sample point beyond	No. I. Es	ich sample	point beyt	and No. 1	No. 1 is spaced 10 sec.	0 sec.														

TABLE IV-37, FUEL VAPOR CONCENTRATIONS IN PPM

Test 37 Conditions: Fuel - avgas.

	:						*	9.00	. 30	10,786	8	. 500	11,300	86.	12.000	12.100		
	17		9	901	004	7.400	7,700	9.100	9, 990									
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	97		3	1.200	2,300	3,400	4, 300	9, 100	6. Boo	9.600	9, 000	. 700	9.100	6,500	9,700	9,500		
	2		ş	. 000	1.90	2.780	3, 400	4, 200	5, 500	B. 200	9,600	9, 300	6, 700	8, 400	9,000	9, 800	9,500	
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£	=	902	807	700	30	300	8	1.000	2, 100	3, 900	6,000	7, 000	6,800	9, 700	6,600	6,500	7,400	
Sample Polat Numbers	2	200	907	700	300	300	8	906	2, 900	3, 700	6, 000	7,000	6. 900	9,600	6,600	6.400	7,400	
Sample	=	200	8	700	300	200	8	1.200	3,300	4, 300	6.400	7,300	7, 100	9.600	7,000	008.9	7,600	
	9	200	200	200	300	200	8	1,200	3, 600	4, 500	6.700	7, 500	7, 400	9. 400	7, 200	6, 100	7, 400	
	•	907		300		1.000	1.600	2, 900	4,200	5.500	7,200	7, 906	1. 100	9, 100	7, 600	400	4. 300	opeced 10
	-	700	907	200	00+	1.000	1.800	2,400	. +00	6.100	7,700	9.300	9,100	7, 300	9. : 00	2, 400	008.9	4 No. 1 16
	-	200	82	200	9	. 800	2, 500	3, 300	6.000	7, 300	9.200	9. 800	8.000	1, 900	8.800	9.500	4, 300	otat beyon
	•	200	200	208	1, 100	2, 300	3, 000	3, 900	. 400	7, 800	8, 700	0,200	9.100	005.0	4.400	. 100	9, 800	h sample p
	-	200	200	1.000	2,000	3,200	4 . 100	9, 100	6.900	9.400	9,200	9,700	9, 600	. 100	10, 000	000 .	10.500	. 1. Eac
	-	700	\$	1.200	2,600		÷. 800	2. 400	7, 800	. 90	9.600	10, 000	10, 100	4, 700	10.400	10,600	10, 400	No Point N
	-	80+	8	2,500	3,700	8, 100	4.200	7,100	8,300	9,300	19, 000	10, 300	10,000	10, 100	10, 900	10.400	11.300	de to Samp
	-	9	2.00	4, 500	e. 00e	7,200	7, 800	9.100	. 40	. 900	10,500	10, 800	10, 400	10, 700	11,700	11.600	11, 400	The time shown corresponds to Sample Point No. 1. Each sample point beyond No. 1 as
	-	÷. 900	10.0	4. 800	10,100	10, 400	10, 700	10. 800	11.300	12,200	12,600	12, 600	3,000	75, 400	. 3, 800	.3. 400	13,800	I'me shown
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REFERENCES

- (1) Hansberry, Harvey, Personal Communication, April 1972.
- (2) Brenneman, J.J., "A Study of the Fuel Vapor Envelope at Aircraft Tank Fuel Vents during Fueling Operations," United Air Lines, December, 1963.
- (3) Katan, L. L., "The Fire Hazard of Fueling Aircraft in the Open," Fire Research Technical Paper, Joint Fire Research Organization, Boreham Woods, England, 1951.
- (4) Department of Trade and Industry, "The Fueling of Land Planes and Helicopters," CAP 74, HM Stationary Office, 1969.
- (5) Zabetakis, Michael G., "Flammability Characteristics of Combustible Gases and Vapors," Bulletin 627, U.S. Bureau of Mines, 1965.
- (6) Schiffauer, Earl J., Personal Communication, December 1971.
- (7) Schiffauer, Earl J., Personal Communication, March 1972.
- (8) Schon, G., "Expansion of Explosive Mixtures," Erdől und Kohle Erdgas Petrochemie, 20, No. 10, 714-720 (1967).
 NSTIC Translation No. 2010, DDC Document No. AD 697488.